Preliminary Classification:

Proposed Class:

Subclass:

NOTE: "All applicants are requested to include a preliminary classification on newly filed patent applications. The preliminary classification, preferably class and subclass designations, should be identified in the upper right-hand comer of the letter of transmittal accompanying the application papers, for example 'Proposed Class 2, subclass 129.' " M.P.E.P. § 601, 7th ed.

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

Box Patent Application Assistant Commissioner for Patents Washington, D.C. 20231

NEW APPLICATION TRANSMITTAL

Transmitted herewith for filing is the patent application of

Inventor(s):

John M. Krajnik, Keith R. Olesen, Gerald A. Vandezande

WARNING: 37 C.F.R. § 1.41(a)(1) points out:

"(a) A patent is applied for in the name or names of the actual inventor or inventors.

"(1) The inventorship of a nonprovisional application is that inventorship set forth in the oath or declaration as prescribed by § 1.63, except as provided for in § 1.53(d)(4) and § 1.63(d). If an oath or declaration as prescribed by § 1.63 is not filed during the pendency of a nonprovisional application, the inventorship is that inventorship set forth in the application papers filed pursuant to § 1.53(b), unless a petition under this paragraph accompanied by the fee set forth in § 1.17(i) is filed supplying or changing the name or names of the inventor or inventors."

For (title):

WATERBORNE COATING HAVING IMPROVED CHEMICAL RESISTANCE

CERTIFICATION UNDER 37 C.F.R. § 1.10*

(Express Mail label number is mandatory.) (Express Mail certification is optional.)

deposited with the United States Postal Service on this date _ in an envelope as "Express Mail Post Office to Addressee," mailing Label Number _EM481114117US dressed to the: Assistant Commissioner for Patents, Washington, D.C. 20231.

Laurie M. Feltes

(type or print name of person mailing paper)

WARNING: Certificate of mailing (first class) or facsimile transmission procedures of 37 C.F.R. § 1.8 cannot be used to obtain a date of mailing or transmission for this correspondence.

*WARNING: Each paper or fee filed by "Express Mail" must have the number of the "Express Mail" mailing label placed thereon prior to mailing. 37 C.F.R. § 1.10(b).

> "Since the filing of correspondence under § 1.10 without the Express Mail mailing label thereon is an oversight that can be avoided by the exercise of reasonable care, requests for waiver of this requirement will not be granted on petition." Notice of Oct. 24, 1996, 60 Fed. Reg. 56,439, at 56,442.

> > (New Application Transmittal [4-1]—page 1 of 11)



1. Type of Application

This new application is for a(n)

(check one applicable item below)

	X	Original (nonprovisional)
		Design
		☐ Plant
WARI	VING	Do not use this transmittal for a completion in the U.S. of an International Application under 35 U.S.C. § 371(c)(4), unless the International Application is being filed as a divisional, continuation or continuation-in-part application.
WAR	NING	: Do not use this transmittal for the filing of a provisional application.
NOTE	77	one of the following 3 items apply, then complete and attach ADDED PAGES FOR NEW APPLICATION RANSMITTAL WHERE BENEFIT OF A PRIOR U.S. APPLICATION CLAIMED and a NOTIFICATION PARENT APPLICATION OF THE FILING OF THIS CONTINUATION APPLICATION.
		Divisional.
		Continuation.
	□.	Continuation-in-part (C-I-P).

2. Benefit of Prior U.S. Application(s) (35 U.S.C. §§ 119(e), 120, or 121)

NOTE: A nonprovisional application may claim an invention disclosed in one or more prior filed copending nonprovisional applications or copending international applications designating the United States of America. In order for a nonprovisional application to claim the benefit of a prior filed copending nonprovisional application or copending international application designating the United States of America, each prior application must name as an inventor at least one inventor named in the later filed nonprovisional application and disclose the named inventor's invention claimed in at Teast one claim of the later filed nonprovisional application in the manner provided by the first paragraph of 35 U.S.C. § 112. Each prior application must also be:

- (f) An international application entitled to a filing date in accordance with PCT Article 11 and designating the United States of America; or
 - (ii) Complete as set forth in § 1.51(b); or
- (iii) Entitled to a filing date as set forth in § 1.53(b) or § 1.53(d) and include the basic filing fee set forth in § 1.16; or
- (iv) Entitled to a filing date as set forth in § 1.53(b) and have paid therein the processing and retention fee set forth in § 1.21(f) within the time period set forth in § 1.53(f).

37 C.F.R. § 1.78(a)(1).

NOTE: If the new application being transmitted is a divisional, continuation or a continuation-in-part of a parent case, or where the parent case is an International Application which designated the U.S., or benefit of a prior provisional application is claimed, then check the following item and complete and attach ADDED PAGES FOR NEW APPLICATION TRANSMITTAL WHERE BENEFIT OF PRIOR U.S. APPLICATION(S) CLAIMED.

WARNING: If an application claims the benefit of the filing date of an earlier filed application under 35 U.S.C. §§ 120, 121 or 365(c), the 20-year term of that application will be based upon the filing date of the earliest U.S. application that the application makes reference to under 35 U.S.C. §§ 120, 121 or 365(c). (35 U.S.C. § 154(a)(2) does not take into account, for the determination of the patent term, any application on which priority is claimed under 35 U.S.C. §§ 119, 365(a) or 365(b).) For a c-i-p application, applicant should review whether any claim in the patent that will issue is supported by an earlier application and, if not, the applicant should consider canceling the reference to the earlier filed application. The term of a patent is not based on a claim-by-claim approach. See Notice of April 14, 1995, 60 Fed. Reg. 20,195, at 20,205.

(New Application Transmittal [4-1]-page 2 of 11)

- WARNING: When the last day of pendency of a provisional application falls on a Saturday, Sunday, or Federal holiday within the District of Columbia, any nonprovisional application claiming benefit of the provisional application must be filed prior to the Saturday, Sunday, or Federal holiday within the District of Columbia. See 37 C.F.R. § 1.78(a)(3).
 - The new application being transmitted claims the benefit of prior U.S. application(s). Enclosed are ADDED PAGES FOR NEW APPLICATION TRANSMITTAL WHERE BENEFIT OF PRIOR U.S. APPLICATION(S) CLAIMED.

3.

В.		Fortened
	-	Enclosed
A.		uired for filing date under 37 C.F.R. § 1.53(b) (Regular) or 37 C.F.R. § 1.153 ign) Application
67	_ Pa	ges of specification
5	_ Pa	ges of claims
	_ Sh	eets of drawing
WAR		DO NOT submit original drawings. A high quality copy of the drawings should be supplied when filling a patent application. The drawings that are submitted to the Office must be on strong, white, amooth, and non-shiny paper and meet the standards according to § 1.84. If corrections to the drawings are necessary, they should be made to the original drawing and a high-quality copy of the corrected original drawing then submitted to the Office. Only one copy is required or desired. For comments on proposed then-new 37 C.F.R. § 1.84, see Notice of March 9, 1988 (1990 O.G. 57-62).
NOTE	inv the on	lentifying indicia, if provided, should include the application number or the title of the invention, tentor's name, docket number (if any), and the name and telephone number of a person to call if the Office is unable to match the drawings to the proper application. This information should be placed the back of each sheet of drawing a minimum distance of 1.5 cm. (5/8 inch) down from the top the page * 37 C.F.R. § 1.84(c)).
		(complete the following, if applicable)
		The enclosed drawing(s) are photograph(s), and there is also attached a "PETITION TO ACCEPT PHOTOGRAPH(S) AS DRAWING(S)." C7 C.F.R. § 1.84(b).
		formal ·
		informal
B.	Othe	er Papers Enclosed
	Pa	ages of declaration and power of attorney
	Pa	ages of abstract
	0	ther
l. A	dditi	onai papers enclosed
		Amendment to claims
		☐ Cancel in this applications claims before calculating the filing fee. (At least one original independent claim must be retained for filing purposes.)
		Add the claims shown on the attached amendment. (Claims added have been numbered consecutively following the highest numbered original claims.)
		Preliminary Amendment
	X	Information Disclosure Statement (37 C.F.R. § 1.98)
	X	Form PTO-1449 (PTO/SB/08A and 08B)
	X	Citations

L	Dec	aration of biological Deposit
	per	mission of "Sequence Listing," computer readable copy and/or amendment aining thereto for biotechnology invention containing nucleotide and/or acid sequence.
	Auti tive	orization of Attorney(s) to Accept and Follow Instructions from Representa-
	Spe	cial Comments
	Oth	er
5. Deci	aratio	n or oath (including power of attorney)
	the price by all capplica the sign by a stapeing to declarate person	executed declaration is not required in a continuation or divisional application provided that is nonprovisional application contained a declaration as required, the application being filed is fewer than all the inventors named in the prior application, there is no new matter in the on being filed, and a copy of the executed declaration filed in the prior application (showing attree or an indication thereon that it was signed) is submitted. The copy must be accompanied tement requesting deletion of the names of person(s) who are not inventors of the application led. If the declaration in the prior application was filed under § 1.47, then a copy of that ion must be filed accompanied by a copy of the decision granting § 1.47 status or, if a nonsigning under § 1.47 has subsequently joined in a prior application, then a copy of the subsequently declaration must be filed. See 37 C.F.R. §§ 1.63(d)(1)–(3).
	is direc abbrevi country	ration filed to complete an application must be executed, identify the specification to which it and it it is inventor by full name including family name and at least one given name, without ation together with any other given name or initial, and the residence, post office address and or citizenship of each inventor, and state whether the inventor is a sole or joint inventor. 37 is 1.63(a)(1)-(4).
NOTE:	as pres as pres is that i this pa	rentorship of a nonprovisional application is that inventorship set forth in the oath or declaration cribed by § 1.62, except as provided for in § 1.53(d)(4) and § 1.63(d). If an oath or declaration cribed by § 1.63 is not filed during the pendency of a nonprovisional application, the inventorship eventorship set forth in the application papers filed pursuant to § 1.53(b), unless a petition under agraph accompanied by the fee set forth in § 1.17(f) is filed supplying or changing the name set of the inventor or inventors." 37 C.F.R. § 1.41(a)(1).
X] End	losed
	Exe	cuted by
		(check all applicable boxes)
	\boxtimes	inventor(s).
		legal representative of inventor(s). 37 C.F.R. §§ 1.42 or 1.43.
		joint inventor or person showing a proprietary interest on behalf of inventor who refused to sign or cannot be reached.
		☐ This is the petition required by 37 C.F.R. § 1.47 and the statement required by 37 C.F.R. § 1.47 is also attached. See item 13 below for fee.
		Enclosed.
NOTE:	the U. may b	the filing is a completion in the U.S. of an International Application or where the completion of 6. application contains subject matter in addition to the International Application, the application a treated as a continuation or continuation-in-part, as the case may be, utilizing ADDED PAGE EW APPLICATION TRANSMITTAL WHERE BENEFIT OF PRIOR U.S. APPLICATION CLAIMED.
		Application is made by a person authorized under 37 C.F.R. § 1.41(c) on behalf of all the above named inventor(s).
		(New Application Transmittal [4-1]—page 4 of 11)

(The de	claration or oath, along with the surcharge required by 37 C.F.R. § 1.16(e) can be filed subsequently).
	Showing that the filing is authorized. (not required unless called into question. 37 C.F.R. § 1.41(d))
6. invent	orship Statement
WARNING:	If the named inventors are each not the inventors of all the claims an explanation, including the ownership of the various claims at the time the last claimed invention was made, should be submitted.
The inve	entorship for all the claims in this application are:
X	The same.
	or
	Not the same. An explanation, including the ownership of the various claims at the time the last claimed invention was made,
	☐ is submitted.
	will be submitted.
7. Langu	age
Ar rei	n application including a signed oath or declaration may be filed in a language other than English. In English translation of the non-English language application and the processing fee of \$130.00 quired by 37 C.F.R. § 1.17(k) is required to be filed with the application, or within such time as may be set by the Office. 37 C.F.R. § 1.52(d).
X	English
	Non-English
	☐ The attached translation includes a statement that the translation is accurate. 37 C.F.R. § 1.52(d).
8. Assign	
	An assignment of the invention toThe Sherwin-Williams Company
	☐ is attached. A separate ☐ "COVER SHEET FOR ASSIGNMENT (DOCUMENT) ACCOMPANYING NEW PATENT APPLICATION" or ☐ FORM PTO 1595 is also attached.
	will follow.
ar	f an assignment is submitted with a new application, send two separate letters-one for the application and one for the assignment." Notice of May 4, 1990 (1114 O.G. 77-78).
WARNING	A newly executed "CERTIFICATE UNDER 37 C.F.R. § 3.73(b)" must be filed when a continuation-in-part application is filed by an assignee. Notice of April 30, 1993, 1150 O.G. 62-64.
	(New Application Transmittal [4-1]—page 5 of 11)

9.	Cer	tifi	ed	Co	DV
•	-		-	~~	~,

Certified copy(ies) of application(s)

Country				
Country	Appin. N	No.		Filed
Country	Appin. i	Vo.		Filed
Country	Appin. N	lo.		Filed
rom which priority is claimed				
is (are) attached.				
will follow.				
NOTE: The foreign application form declaration. 37 C.F.R. § 1.5	ning the basis for the (5(a) and 1.63.	claim for	priority must l	pe referred to in the oath o
NOTE: This item is for any foreign U.S. application or Internation § 120 is itself entitled to price PAGES FOR NEW APPLICA CLAIMED. O. Fee Calculation (37 C.F. A. Regular application	nal Application from v ority from a prior foreig NTION TRANSMITTAL	vhich this In applica	application cla ation, then com	aims benefit under 35 U.S.C plete item 18 on the ADDEL
Togala approach	CLAIMS AS	FILED		,
Number filed	Number Ext	ra	Rate	Basic Fee 37 C.F.R. § 1.16(a)
				\$7 60.00
Claims (37 C.F.R.	20 = 0	×	\$ 18.00	0.00
Claims (37 C.F.R. § 1.16(c)) 14 - Independent Claims (37 C.F.R.	20 = 0 3 = 0	×	\$ 18.00 \$ 78.00	
Claims (37 C.F.R. § 1.16(c)) 14 - Independent Claims (37 C.F.R. § 1.16(b)) 2 -				0.00
Claims (37 C.F.R. 14 - 16(c)) 14 - 16(c) 14	3 = 0	× +	\$ 78.00 \$2 60.00	0.00
Claims (37 C.F.R. § 1.16(c)) Independent Claims (37 C.F.R. § 1.16(b)) Multiple dependent claim(s), if any (37 C.F.R. § 1.16(d))	3 = 0	+ is encid	\$ 78.00 \$260.00	0.00
ndependent Claims (37 C.F.R. § 1.16(b)) 2 - Multiple dependent claim(s), if any (37 C.F.R. § 1.16(d)) Amendment cancel	3 = 0 ling extra claims in a multiple-dependent	+ is enclo	\$ 78.00 \$260.00 osed.	0.00
Claims (37 C.F.R. § 1.16(c)) Independent Claims (37 C.F.R. § 1.16(b)) Quitiple dependent claim(s), if any (37 C.F.R. § 1.16(d)) Amendment cancel Amendment deletin Fee for extra claim NOTE: If the fees for extra claims as	3 = 0 ling extra claims ig multiple-depend s is not being paid re not paid on filling the the time period set for	+ is enclo dencies id at the	\$ 78.00 \$260.00 psed. is enclosed is time.	0.00 0.00 ins cancelled by amendmen
Claims (37 C.F.R. § 1.16(c)) Independent Claims (37 C.F.R. § 1.16(b)) Multiple dependent claim(s), if any (37 C.F.R. § 1.16(d)) Amendment cancel Amendment deletin Fee for extra claims and prior to the expiration of the notice of fee deficiency. 33	3 = 0 ling extra claims ig multiple-depend s is not being paid re not paid on filling the the time period set for	+ is enclo dencies id at the must be response	\$ 78.00 \$260.00 psed. is enclosed is time.	0.00 0.00
Claims (37 C.F.R. \$ 1.16(c)) Independent Claims (37 C.F.R. \$ 1.16(b)) Quiltiple dependent claim(s), if any (37 C.F.R. § 1.16(d)) Amendment cancel Amendment deletin Fee for extra claims au prior to the expiration of the notice of fee deficiency. 33	ling extra claims g multiple-depend s is not being paid e not paid on filing the te time period set for 7 C.F.R. § 1.16(d). Filing Fee Calcula	+ is enclo dencies id at the must be response	\$ 78.00 \$260.00 psed. is enclosed is time.	0.00 0.00 i. ims cancelled by amendmen and Trademark Office in a

(New Application Transmittal [4-1]—page 6 of 11)

C.		Plant application (\$480.00—37 C.F.R. § 1.16(g))	
		Filing fee calculation	\$
11.	Sma	all Entity Statement(s)	
		Statement(s) that this is a filing by a small entity us (are) attached.	under 37 C.F.R. § 1.9 and 1.27
WAI	RNING	G: "Status as a small entity must be specifically established the status is available and desired. Status as a small entity affect any other application or patent, including application directly dependent upon the application or patent in whice refiling of an application under § 1.53 as a continuation, diversity a continued prosecution application under § 1.53(d)), or the anew determination as to continued entitlement to small enapplication. A nonprovisional application claiming benefit usuapplication or in the patent if the nonprovisional application reference to the statement in the prior application or in statement in the prior application or in the patent and statement in the payment of the small entity basic statutory filing for purposes of this section." 37 C.F.R. § 1.28(a)(2).	in one application or patent does not tions or patents which are directly or in the status has been established. The ision, or continuation-in-part (including a filing of a reissue application requires notity status for the continuing or reissue under 35 U.S.C. § 119(e), 120, 121, or rely on a statement filed in the prior or the reissue application includes a the patent or includes a copy of the tus as a small entity is still proper and
WA	RNING	IG: "Small entity status must not be established when the perso can unequivocally make the required self-certification." M 1996 (emphasis added).	
		(complete the following, if applic	able)
		Status as a small entity was claimed in prior ap	pplication
		/, filed on	, from which benefit
		is being claimed for this application under: 35 U.S.C. § 119(e),	
		120,	
		☐ 121, ☐ 255(a)	
		☐ 365(c), and which status as a small entity is still prop	per and desired
		☐ A copy of the statement in the prior appli	
		Filing Fee Calculation (50% of A, B or C at	
		• • • • • • • • • • • • • • • • • • •	,010,
NO	6	Any excess of the full fee paid will be refunded if small entitity stare filed within 2 months of the date of timely payment of a extendable under § 1.136. 37 C.F.R. § 1.28(a).	
12.	Req	quest for International-Type Search (37 C.F.R. §	§ 1.104(d))
		(complete, if applicable)	
		Please prepare an international-type search repo when national examination on the merits takes	

13. Fee i	Payment Being Made at This Time	
. 0	Not Enclosed	
	No filing fee is to be paid at this time. (This and the surcharge required by 37 C.F.R. § subsequently.)	1.16(e) can be paid
X	Enclosed	
	☑ Filing fee	\$ 760.00
	Recording assignment (\$40.00; 37 C.F.R. § 1.21(h)) (See attached "COVER SHEET FOR ASSIGNMENT ACCOMPANYING NEW APPLICATION".)	\$ <u>120.00</u>
	Petition fee for filing by other than all the inventors or person on behalf of the inventor where inventor refused to sign or cannot be reached (\$130.00; 37 C.F.R. §§ 1.47 and 1.17(I))	\$
	☐ `For processing an application with a specification in a non-English language (\$130.00; 37 C.F.R. §§ 1.52(d) and 1.17(k))	\$
	☐ Processing and retention fee (\$130.00; 37 C.F.R. §§ 1.53(d) and 1.21(l))	\$
	☐ Fee for international-type search report (\$40.00; 37 C.F.R. § 1.21(e))	\$
3	37 C.F.R. § 1.21(I) establishes a fee for processing and retaining any applic failing to complete the application pursuant to 37 C.F.R. § 1.53(f) and this, 37 C.F.R. §§ 1.53 and 1.78(a)(1), indicate that in order to obtain the benefit either the basic filing fee must be paid, or the processing and retention fee within 1 year from notification under § 53(f).	, as well as the changes to of a prior U.S. application, e of § 1.21(f) must be paid,
	Total fees enclosed	\$ 880.00
14. Met	thod of Payment of Fees	
	Check in the amount of \$	
	8 880.00	in the amount of
	A duplicate of this transmittal is attached.	
	Fees should be itemized in such a manner that it is clear for which purpose & 1.22(h)	the fees are paid. 37 C.F.R

•

(New Application Transmittal [4-1]---page 8 of 11)

§ 1.136(a)(3).

Authorization to Charge Additional Fees WARNING: If no fees are to be paid on filing, the following items should not be completed. WARNING: Accurately count claims, especially multiple dependent claims, to avoid unexpected high charges, if extra claim charges are authorized. Market The Commissioner is hereby authorized to charge the following additional fees by this paper and during the entire pendency of this application to Account No. 37 C.F.R. § 1.16(b), (c) and (d) (presentation of extra claims) NOTE: Because additional fees for excess or multiple dependent claims not paid on filing or on later presentation must only be paid or these claims cancelled by amendment prior to the expiration of the time period set for response by the PTO in any notice of fee deficiency (37 C.F.R. § 1.16(d)), it might be best not to authorize the PTO to charge additional claim fees, except possibly when dealing with amendments after final action. 37 C.F.R. § 1.16(e) (surcharge for filing the basic filing fee and/or declaration on a date later than the filing date of the application) 37 C.F.R. § 1.17(a)(1)-(5) (extension fees pursuant to § 1.136(a)). 37 C.F.R. § 1.17 (application processing fees) NOTE: ". . . À written request may be submitted in an application that is an authorization to treat any concurrent or future reply, requiring a petition for an extension of time under this paragraph for its timely submission, as incorporating a petition for extension of time for the appropriate length of time. An authorization to charge all required fees, fees under § 1.17, or all required extension of time fees will be treated as a constructive petition for an extension of time in any concurrent or future reply requiring a petition for an extension of time under this paragraph for its timely submission. Submission of the fee set forth in § 1.17(a) will also be treated as a constructive petition for an extension of time in any concurrent reply

☐ 37 C.F.R. § 1.18 (issue fee at or before mailing of Notice of Allowance, pursuant to 37 C.F.R. § 1.311(b))

requiring a petition for an extension of time under this paragraph for its timely submission: 937 C.F.R.

NOTE: Where an authorization to charge the issue fee to a deposit account has been filed before the mailing of a Notice of Allowance, the issue fee will be automatically charged to the deposit account at the time of mailing the notice of allowance. 37 C.F.R. § 1.311(b).

NOTE: 37 C.F.R. § 1.28(b) requires "Notification of any change in status resulting in loss of entitlement to small entity status must be filed in the application . . . prior to paying, or at the time of paying, . . . the issue fee. . . " From the wording of 37 C.F.R. § 1.28(b), (a) notification of change of status must be made even if the fee is paid as "other than a small entity" and (b) no notification is required if the change is to another small entity.

(New Application Transmittal [4-1]—page 9 of 11)

	reasonable returned	time, nor by check	will the port if rec	eyer be no juested, by	tified of suc credit to a	h amounts	nd unless spe s; amounts ou account." 37	er twenty-fit	uested within ve dollars may 26(a).
X	Credit /	Account	No	19-202	25		_		
	Refund			•					
	**								
									∓
									•
									•

Reg. No. 34,296

Tel. No. (216) 566-3650

Customer No.

Heidi A. Boehlefeld

SIGNATURE OF PRACTITIONER //

(type or print name of attorney)

The Sherwin-Williams Company

P.O. Address

11 Midland Bldg. - Legal Dept. 101 Prospect Avenue, N.W. Cleveland, Ohio 44115

(New Application Transmittal [4-1]—page 10 of 11)

	pri sta the	neck the following item if the application in this transmittal claims the benefit of ior U.S. application(s) (including an international application entering the U.S. age as a continuation, divisional or C-I-P application) and complete and attach a ADDED PAGES FOR NEW APPLICATION TRANSMITTAL WHERE BENEFIT OF RIOR U.S. APPLICATION(S) CLAIMED)					
	X	Plus Added Pages for New Application Transmittal Where Benefit of Prior U.S. Application(s) Claimed					
		Number of pages added5					
		Plus Added Pages for Papers Referred to in Item 4 Above Number of pages added					
		Plus added pages deleting names of inventor(s) named in prior application(s) who is/are no longer inventor(s) of the subject matter claimed in this application. Number of pages added					
	X	Plus "Assignment Cover Letter Accompanying New Application" Number of pages added3					
	State	ment Where No Further Pages Added					
(if no further pages form a part of this Transmittal, then end this Transmittal wi this page and check the following item)							
		This transmittal ends with this page.					

ADDED PAGES FOR APPLICATION TRANSMITTAL WHERE BENEFIT OF PRIOR U.S. APPLICATION(S) CLAIMED

NOTE: See 37 C.F.R. § 1.78.

Practitioner's Docket No.

17. Relate Back

WARNING: If an application claims the benefit of the filing date of an earlier filed application under 35 U.S.C. §§ 120, 121 or 365(c), the 20-year term of that application will be based upon the filing date of the earliest U.S. application that the application makes reference to under 35 U.S.C. §§ 120, 121 or 365(c). (35 U.S.C. § 154(a)(2) does not take into account, for the determination of the patent term, any application on which priority is claimed under 35 U.S.C. §§ 119, 365(a) or 365(b).) For a c-i-p application, applicant should review whether any claim in the patent that will issue is supported by an earlier application and, if not, the applicant should consider canceling the reference to the earlier filed application. The term of a patent is not based on a claim-by-claim approach. See Notice of April 14, 1995, 60 Fed. Reg. 20,195, at 20,205.

(complete the following, if applicable)

Amend the specification by inserting, before the first line, the following sentence:

A. 35 U.S.C. § 119(e)

NOTE: "Any nonprovisional application claiming the benefit of one or more prior filed copending provisional applications must contain or be amended to contain in the first sentence of the specification following the title a reference to each such prior provisional application, identifying it as a provisional application, and including the provisional application number (consisting of series code and serial number)." 37 C.F.R. § 1.78(a)(4).

"This application claims the benefit of U.S. Provisional Application(s) No(s).:

APPLICATION NO(S).:	FILING DATE
60 / 138,086	06/08/99
/	
/	

(Added Pages for Application Transmittal Where Benefit of Prior U.S. Application(s) Claimed [4-1.1]—page 1 of 5)

NOTE:	"Except for a continued prosecution application filed under § 1.53(d), claiming the benefit of one or more prior filed copending nonprovision applications designating the United States of America must contain or first sentence of the specification following the title a reference to each suit by application number (consisting of the series code and serial number number and international filing date and indicating the relationship of references to other related applications may be made when appropria § 1.78(a)(2).	eal applications or international be amended to contain in the uch prior application, identifying per) or international application f the applications Cross-					
	This application is a						
	☐ continuation						
	☐ continuation-in-part						
	☐ divisional						
o	f copending application(s)						
С	application number 0 /	filed on"					
	and which designated the	ne U.S."					
NOTE:	The proper reference to a prior filed PCT application that entered the serial number and the filing date of the PCT application that designate	U.S. national phase is the U.S. ed the U.S.					
NOTE:	(1) Where the application being transmitted adds subject matter to the the filing can be as a continuation-in-part or (2) if it is desired to do so can be as a continuation.	International Application, then for other reasons then the filing					
NOTE:	The deadline for entering the national phase in the U.S. for an international application was clarified in the Notice of April 28, 1987 (1079 O.G. 32 to 46) as follows:						
	"The Patent and Trademark Office considers the International application month from the priority date if the United States has been designated a Preliminary Examination has been filed prior to the expiration of the 19 and until the 32nd month from the priority date if a Demand for International elected the United States of America has been filed prior to the from the priority date, provided that a copy of the international application to the Patent and Trademark Office within the 20 or 30 month period international application has not been communicated to the Patent at 20 or 30 month period respectively, the international application becomes States 20 or 30 months from the priority date respectively. These period as paragraph (h) of § 1.494 and paragraph (i) of § 1.495. A continuing application and 120 may be filed anytime during the pendency of the international	nd no Demand for International th month from the priority date ational Preliminary Examination e expiration of the 19th month ation has been communicated the respectively. If a copy of the nd Trademark Office within the res abandoned as to the United is have been placed in the rules plication under 35 U.S.C. 365(c)					
	m norm of the state of the stat						
-	, filed						
	U.S. Provisional Application(s) No(s).:						
APPLIC	ATION NO(S).:	FILING DATE					
	./	,					
	. /	· · · · · · · · · · · · · · · · · · ·					
C	Where more than one reference is made above, pleas into one sentence.	se combine all references					

B. 35 U.S.C. §§ 120, 121 and 365(c)

18. Relate Back—35 U.S.C. § 119 Priority Claim for Prior Application

The prior U.S. application(s), including any prior International Application designating the U.S., identified above in item 17B, in turn itself claim(s) foreign priority(ies) as follows:

	Country	Appln. no.	Filed on
The ce	rtified copy(ies) has	(have)	
		·	0 /, which was
	is (are) attached.		
	the International Bure application in the capplication communa U.S. serial number a stage is not entered prosecution of a condocuments from the to request transfer, reenter and make a rectine priority documents stage may not be re	nau may not be relied on without any continuing application. This is so be icated by the International Bureau in International Bureau in International Bureau in Internation, such certified copies matinuing application. An alternative wholders and transfer them to the continuine the folders, make suitable record of such copies in the Continuing into in folders of international application. Notice of April 28, 1987 (10)	· ·
19. Ma	intenance of Co	pendency of Prior Applic	cation
	The PTO finds it useful it esponse is filed with th November 5, 1985 (1060	e papers constituting the filing of	prior application extending the term for the continuation application. Notice of
A. 🗆	Extension of time	in prior application	•
(Thi		mpleted and the papers filed riod set in the prior applicati	
	A petition, fee and until	response extends the term	in the pending prior application
	☐ A copy of the	e petition filed in prior applic	ation is attached.
B. 🗆	Conditional Petition	on for Extension of Time in F	Prior Application
	(complete	this item, if previous item ne	ot applicable)
	A conditional peti application.	tion for extension of time is	being filed in the pending prior
	☐ A copy of the	conditional petition filed in	the prior application is attached.

20. Further Inventorship Statement Where Benefit of Prior Application(s) Claimed

(complete applicable item (a), (b) and/or (c) below)

(a)	Δ	application whose particulars are set out above and the inventor(s) in this application are			
			the same.		
			less than those named in the prior application. It is requested that the following inventor(s) identified for the prior application be deleted:		
			(type name(s) of inventor(s) to be deleted)		
(b)		☐ This application discloses and claims additional disclosure by a a new declaration or oath is being filed. With respect to the pre the inventor(s) in this application are			
			the same.		
			the following additional inventor(s) have been added:		
			(type name(s) of inventor(s) to be added)		
(c)		The	inventorship for all the claims in this application are		
		X	the same.		
			not the same. An explanation, including the ownership of the various claims at the time the last claimed invention was made		
			is submitted.		
			□ will be submitted.		

21.	Ab	andonment of Prior Application (if applicable)
		Please abandon the prior application at a time while the prior application is pending, or when the petition for extension of time or to revive in that application is granted, and when this application is granted a filing date, so as to make this application copending with said prior application.
NOTE	F	According to the Notice of May 13, 1983 (103, TMOG 6-7), the filing of a continuation or continuation-in- part application is a proper response with respect to a petition for extension of time or a petition to revive and should include the express abandonment of the prior application conditioned upon the granting of the petition and the granting of a filing date to the continuing application.
22.	Pe [*]	tition for Suspension of Prosecution for the Time Necessary to e an Amendment
		G: "The claims of a new application may be finally rejected in the first Office action in those situations where (A) the new application is a continuing application of, or a substitute for, an earlier application, and (B) all the claims of the new application (1) are drawn to the same invention claimed in the earlier application, and (2) would have been properly finally rejected on the grounds of art of record in the next Office action if they had been entered in the earlier application." M.P.E.P., § 706.07(b), 7th ed.
NOT		Where it is possible that the claims on file will give rise to a first action final for this continuation application and for some reason an amendment cannot be filed promptly (e.g., experimental data is being gathered) it may be desirable to file a petition for suspension of prosecution for the time necessary.
		(check the next item, if applicable)
		There is provided herewith a Petition To Suspend Prosecution for the Time Necessary to File An Amendment (New Application Filed Concurrently)
23.	Sn	nali Entity (37 C.F.R. § 1.28(a))
		Applicant has established small entity status by the filing of a statement in parent application / on
		☐ A copy of the statement previously filed is included.
WAF	RNIN	IG: See 37 C.F.R. § 1.28(a).
WAI	RNIN	IG: "Small entity status must not be established when the person or persons signing the statement can unequivocally make the required self-certification." M.P.E.P., § 509.03, 7th ed. (emphasis added).
24.	NC	OTIFICATION IN PARENT APPLICATION OF THIS FILING
		A notification of the filing of this (check one of the following)
		continuation
		☐ continuation-in-part
		☐ divisional
	_	filed in the parent application, from which this application claims priority under 35 120.

(Added Pages for Application Transmittal Where Benefit of Prior U.S. Application(s) Claimed [4-1.1]—page 5 of 5)

WATERBORNE COATING HAVING IMPROVED CHEMICAL RESISTANCE

BACKGROUND OF THE INVENTION

5

This invention relates to waterborne coatings having improved chemical resistance.

Conventional latex paints are widely used because they provide low volatile organic compound emission and because they allow easier clean up than solvent borne coatings. However, when compared to solvent borne coating systems, typical latex coatings lack the chemical resistance provided by such solvent borne coatings.

10

It has now been found that latex coating compositions having superior chemical resistance can be produced by formulating a chemical coating comprising a binder resin having post crosslinking groups, an associative thickener having post crosslinking groups and an associative dispersant having post crosslinking groups. The crosslinking groups present in the polymer of the dispersant and/or the thickener can be adjusted, depending on the particular binder resin used, to optimize the desired performance properties of the coating composition. Specifically, a coating composition can be tailor made to have increased chemical resistance, corrosion resistance, humidity resistance and/or adhesion to a particular substrate by altering the levels of crosslinking on the binder, thickener and dispersant. The coating composition of the present invention may be ambient cured, oven cured or radiation cured.

20

SUMMARY OF THE INVENTION

The present invention is directed to an aqueous coating composition in which the binder polymer, thickener polymer and/or dispersant polymer have functional groups that further react

5

some time after initial formation of the polymer. The aqueous coating composition contains (a) a binder polymer comprising at least one or more copolymerizable monoethylenically unsaturated monomers, wherein at least one of the monoethylenically unsaturated monomers contains latent crosslinking functionality; and (b) a second polymer comprising a monoethylenically unsaturated monomer containing latent crosslinking functionality. The second polymer may be an associative thickener or an associative dispersant.

The binder polymer, thickener and dispersant polymer may contain a macromonomer represented by the formula:

$$R^4$$

R¹-(OR²)₂-R³-C=CR⁵R⁶

wherein R¹ is a monovalent residue of a substituted or unsubstituted hydrophobe compound; each R² is the same or different and is a substituted or unsubstituted divalent hydrocarbon residue; R³ is a substituted or unsubstituted divalent hydrocarbon residue; R⁴, R⁵, R⁶ are the same or different and are hydrogen or a substituted or unsubstituted monovalent hydrocarbon residue; and z is a value of 0 to 150.

The binder polymer, thickener polymer and dispersant polymer may contain diacetone acrylamide as the monomer having latent crosslinking functionality.

The aqueous coating compositions of the present invention produce coatings having improved chemical resistance, as well as improved corrosion resistance.

DETAILED DESCRIPTION OF THE INVENTION

Binder

The latex polymers used as binders in accordance with the present invention (also

5

referred to herein as "binders") include those polymers polymerized from one or more suitable monomers. Typically, the binders are polymerized from one or more copolymerizable monoethylenically unsaturated monomers such as, for example, vinyl monomers and acrylic monomers.

The vinyl monomers suitable for use in accordance with the present invention include any compounds having vinyl functionality, i.e., ethylenic unsaturation, exclusive of compounds having acrylic functionality, e.g., acrylic acid, methacrylic acid, esters of such acids, acrylonitrile and acrylamides. Preferably, the vinyl monomers are selected from the group consisting of vinyl esters, vinyl aromatic hydrocarbons, vinyl aliphatic hydrocarbons, vinyl alkyl ethers and mixtures thereof.

Suitable vinyl monomers include vinyl esters, such as, for example, vinyl propionate, vinyl laurate, vinyl pivalate, vinyl nonanoate, vinyl decanoate, vinyl neodecanoate, vinyl butyrates, vinyl benzoates, vinyl isopropyl acetates and similar vinyl esters; vinyl aromatic hydrocarbons, such as, for example, styrene, methyl styrenes and similar lower alkyl styrenes, chlorostyrene, vinyl toluene, vinyl naphthalene and divinyl benzene; vinyl aliphatic hydrocarbon monomers, such as, for example, vinyl chloride and vinylidene chloride as well as alpha olefins such as, for example, ethylene, propylene, isobutylene, as well as conjugated dienes such as 1,3 butadiene, methyl-2-butadiene, 1,3-piperylene, 2,3-dimethyl butadiene, isoprene, cyclohexene, cyclopentadiene, and dicyclopentadiene; and vinyl alkyl ethers, such as, for example, methyl vinyl ether, isopropyl vinyl ether, n-butyl vinyl ether, and isobutyl vinyl ether.

The acrylic monomers suitable for use in accordance with the present invention comprise any compounds having acrylic functionality. Preferred acrylic monomers are selected from the

5

group consisting of alkyl acrylates, alkyl methacrylates, acrylate acids and methacrylate acids as well as aromatic derivatives of acrylic and methacrylic acid, acrylamides and acrylonitrile.

Typically, the alkyl acrylate and methacrylic monomers (also referred to herein as "alkyl esters of acrylic or methacrylic acid") will have an alkyl ester portion containing from 1 to about 12, preferably about 1 to 5, carbon atoms per molecule.

Suitable acrylic monomers include, for example, methyl acrylate and methacrylate, ethyl acrylate and methacrylate, butyl acrylate and methacrylate, propyl acrylate and methacrylate, 2-ethyl hexyl acrylate and methacrylate, cyclohexyl acrylate and methacrylate, decyl acrylate and methacrylate, isodecyl acrylate and methacrylate, benzyl acrylate and methacrylate, isobornyl acrylate and methacrylate, neopentyl acrylate and methacrylate, 1-adamatyl methacrylate and various reaction products such as butyl, phenyl, and cresyl glycidyl ethers reacted with acrylic and methacrylic acids, hydroxyl alkyl acrylates and methacrylates such as hydroxyethyl and hydroxypropyl acrylates and methacrylates, amino acrylates, methacrylates as well as acrylic acids such as acrylic and methacrylic acid, ethacrylic acid, alpha-chloroacrylic acid, alpha-cycanoacrylic acid, crotonic acid, beta-acryloxy propionic acid, and beta-styryl acrylic acid.

In addition to the specific monomers described above, those skilled in the art will recognize that other monomers such as, for example, allylic monomers, or monomers which impart wet adhesion, e.g., methacrylamidoethyl ethylene urea, can be used in place of, or in addition to, the specifically described monomers in the preparation of the binders (as well as the dispersants and thickeners hereinafter described). Further details concerning such other monomers suitable for copolymerization in accordance with the present invention are known to those skilled in the art. The amount of such other monomers is dependent on the particular

5

monomers and their intended function, which amount can be determined by those skilled in the art.

The binder polymer of the present invention has crosslinking functionality. At least one of the monomers used to polymerize the binder is a monoethylenically, unsaturated monomer containing "latent crosslinking" capabilities, which as used herein means a monomer which possesses the ability to further react some time after initial formation of the polymer. Activation can occur through the application of energy, e.g., through heat or radiation. Also, drying can activate the crosslinking polymer through changes in pH, oxygen content or other changes that causes a reaction to occur. The particular method of achieving crosslinking in the binder polymer is not critical to the present invention. A variety of chemistries are known in the art to produce crosslinking in latexes.

Examples of monomers which do not effect crosslinking until during film formation include carbonyl-containing monomers such as acrolein, methacrolein, diacetone acrylamide, diacetone methacrylamide and vinylaceto acetate. These monomers result in postcrosslinking, for example, when the aqueous polymer emulsion simultaneously contains an appropriate added amount of a polyamine compound. Particularly suitable compounds of this type are the dihydrazides and trihydrazides of aliphatic and aromatic dicarboxylic acids of 2 to 20 carbon atoms. Examples of these are oxalic dihydrazide, adipic dihydrazide and sebacic dihydrazide. Another monomer which produces postcrosslinking is, for example, 2-acetoacetoxyethyl methacrylate (alone or in combination with polyamines or polyaldehydes, such as glyoxal).

Other polymer building blocks which are suitable for postcrosslinking are those which contain hydrolyzable organosilicon bonds. Examples are the copolymerizable monomers

5

methacryloyloxypropyltrimethoxysilane and vinyltrimethoxysilane. Further suitable polymer building blocks of a corresponding type are described in DE-A4341260. If the disperse polymer particles have carboxyl groups, postcrosslinking can also be effected by adding metal salts having polyvalent cations (for example Mg, Ca, Zn or Zr salts).

Epoxy-, hydroxyl- and/or N-alkylol-containing monomers, for example, glycidyl acrylate, N-methylolacrylamide and -methacrylamide and monoesters of dihydric alcohols with α,β -monoethylenically unsaturated carboxylic acids of 3 to 6 carbon atoms, such as hydroxyethyl, hydroxy-n-propyl or hydroxy-n-butyl acrylate and methacrylate are also suitable for postcrosslinking.

U.S. Patent No. 4,144,212 describes an air-curing copolymer latex prepared by emulsion copolymerization in the presence of free radical polymerization catalysts such as inorganic or organic peroxide polymerization catalysts, with a blend (in % by weight based on the total weight of all monomers used) of (a) about 1% to about 20% of dicyclopentadienyl acrylate or dicyclopentadienyl methacrylate, (b) about 99% to about 20% of an alkyl acrylate or methacrylate, including mixtures of such monomers, and preferably a lower alkyl acrylate or methacrylate in which the alkyl groups contain from 1 to 4 carbon atoms, (c) 0% to about 5% of acrylic acid or methacrylic acid, and (d) 0% to about 85% of other monoethylenically unsaturated copolymerizable monomers, e.g., higher alkyl acrylates and methacrylates in which the alkyl groups contain from 5 to about 18 carbon atoms, acrylamide, methacrylamide, acrylonitrile or methacrylonitrile; also vinyl esters (e.g. vinyl acetate, vinyl propionate of vinyl chloride), styrene and alkyl vinyl ethers.

The binder resin of the present invention contains about 0.5 to 10% by weight, based on

5

the total weight of the polymer, of at least one monomer having latent crosslinking functionality, and preferably 1 to 6% by weight, based on the total weight of the polymer, of at least one monomer having latent crosslinking functionality.

Typically, the particle size of the binders is from about 0.1 to 1.0 microns, preferably from about 0.2 to 0.4 microns and more preferably from about 0.25 to 0.3 microns. The Tg of the binders of the present invention is typically from about -60 to 100°C preferably from about -30 to 70°C and more preferably from about -15 to 60°C. As used herein, the term "Tg" means polymer glass transition temperature. Techniques for measuring the glass transition temperature of polymers are known to those skilled in the art. One such technique is, for example, differential scanning calorimetry. A particularly useful means of estimating the glass transition temperature of a polymer is that given by Fox,

$$1/Tg_{(polymer)} = x_1/Tg_1 + x_2/Tg_2 + x_3/Tg_3 + ... + x_n/Tg_n$$
 (1)

where x_1 is the weight fraction of component i in the copolymer and Tg_1 is the homopolymer glass transition of component i. The homopolymer glass transition temperatures can be found in any publicly available source such as the Polymer Handbook. For example, the homopolymer glass transition temperatures for typical monomers are: vinyl acetate = -32°C, butyl acrylate = -54°C, and vinyl neodecanoate = -3°C and 2-ethylhexyl acrylate = -65°C.

Typically, the viscosity of the binders of the present invention is from about 20 to 3000 and preferably from about 50 to 1500 centipoise ("cP") measured with a 40 to 60 weight percent solids composition using a Brookfield Viscometer with a number 2 spindle at 60 revolutions per

5

minute. The molecular weight of the binders of the present invention is typically from about 10⁴ to 10⁷, preferably from about 200,000 to 1,000,000 grams per gram mole. As used herein, the term "molecular weight" means weight average molecular weight. Techniques for altering molecular weight are well known and include, for example, utilizing multi functional monomers and chain transfer agents. Techniques for measuring the weight average molecular weight of latex polymers is known to those skilled in the art. One such technique is, for example, gel permeation chromatography.

The binder polymer of the present invention may contain hydrophobic groups. The monoethylenically unsaturated monomers described above can be polymerized with one or more macromonomers which are polymerizable. Such macromonomers comprise a hydrophobic portion and an alkoxylated portion which is polymerizable with the other monomers. U.S. Patent No. 4,703,080, incorporated herein by reference, describes hydrophobic binder resins. Preferred macromonomers are urethane monomers which comprise the reaction product of a monohydric surfactant and a monoethylenically unsaturated isocyanate. These macromonomers are described in detail below with respect to the dispersant.

In one aspect of the present invention, the binder polymer comprises an acid functional latex. Specific acid functional monomers suitable for use in accordance with the present invention include, for example, acrylic acid, methacrylic acid, and maleic acid.

Preparation of latex compositions is well known in the paint and coatings art. Any of the well known free-radical emulsion polymerization techniques used to formulate latex polymers can be used in the present invention. Such procedures include, for example, single feed, coreshell, and inverted core-shell procedures which produce homogeneous or structures particles.

5

A preferred vinyl acrylate binder resin comprises 40-60% by weight of a fatty acid vinyl ester, 30-50% by weight of methylmethacrylate, 0.5 to 10% by weight of diacetone acrylamide and 0.5-5% by weight methacrylic acid, based on the total weight of the polymer.

A preferred acrylic binder resin comprises 20-35% by weight butyl acrylate, 40-65% by weight methyl methacrylate, 0.5-10% by weight diacetone acrylamide, 0.5-5% by weight methacrylic acid and 5-10% by weight acrylonitrile, based on the total weight of the polymer.

Dispersants

The dispersants suitable for use in accordance with the present invention comprise the reaction product of an unsaturated carboxylic acid monomer, a monoethylenically unsaturated monomer different from the carboxylic acid monomer, a macromonomer comprising a hydrophobic portion and an alkoxylated portion which is polymerizable with the other monomers, and a monomer having latent crosslinking functionality.

The unsaturated carboxylic acid monomers suitable for use in accordance with the present invention are typically α,β -monethylenically unsaturated carboxylic acids. Preferred carboxylic acid monomers are selected from the group consisting of acrylic acid, methacrylic acid, crotonic acid, itaconic acid, maleic acid, and mixtures thereof. Methacrylic acid is especially preferred. The concentration of the carboxylic acid monomer is typically from about 20 to 70 weight percent, preferably from about 20 to 50 weight percent and more preferably from about 35 to 45 weight percent based on the total weight of the polymer. The amount of the carboxylic acid monomer is preferably sufficient to provide a polymeric structure which will solubilize and provide viscosity enhancement when reacted with an alkali such as for example, sodium hydroxide.

5

In accordance with the present invention, the monoethylenically unsaturated monomer different from the carboxylic acid monomer preferably comprises a methyl group. More preferably, this monomer is an acrylate. Most preferably, this monomer is ethyl acrylate. Typically, the amount of the monoethylenically unsaturated monomer different from carboxylic acid is from about 5 to 70 weight percent, preferably from about 10 to 50 weight percent based on the total weight of the polymer.

The macromonomers suitable for manufacturing the dispersant in accordance with the present invention comprise a hydrophobic portion and an alkoxylated portion which is polymerizable with other monomer(s). As used herein, the term "macromonomer" means a polymerizable monomer which comprises the reaction product of two or more compounds. Such macromonomers include, for example, any alkoxylated, e.g., ethoxylated or propoxylated, monomers having ethylenic unsaturation and which are terminated by a hydrophobic fatty chain. Examples of unsaturated, polymerizable moieties include those selected from the group consisting of vinyl group containing moieties, methacryloyl, maleoyl, itaconoyl, crotonyl, an unsaturated urethane moiety, hemiester maleoyl, hemiester itaconoyl, CH₂=CHCH₂-O-, methacrylamido and substituted methacrylamido. Examples of hydrophobic moieties include those selected from the group consisting of alkyl, alkaryl, i.e., alkylaryl or aralkyl, or aryl, linear or branched, saturated or unsaturated, and having at least 6 carbon atoms, preferably from about 6 to 30 carbon atoms per molecule.

Preferred macromonomers are urethane monomers which comprise the reaction product of a monohydric surfactant and a monoethylenically unsaturated isocyanate. Preferably, the urethane monomer is a nonionic, urethane monomer which is the urethane reaction product of a

5

monohydric, nonionic surfactant with a monoethylenically unsaturated monoisocyanate, preferably one lacking ester groups, e.g., alpha, alpha-dimethyl-m-isopropenyl benzyl isocyanate. The monohydric nonionic surfactants are themselves well known and are usually alkoxylated, e.g., ethoxylated, hydrophobes containing adducted ethylene oxide to provide the hydrophilic portion of the molecule. The hydrophobes are usually aliphatic alcohols or alkyl phenols in which a carbon chain containing at least 6 carbon atoms, preferably about 6 to 30 carbon atoms, provides the hydrophobic portion of the surfactant. These surfactants are illustrated by ethylene oxide adducts of dodecyl alcohol or octyl or nonyl phenol which are available in commerce and which contain about 5 to about 150, preferably 25 to 60 moles of ethylene oxide per mole of hydrophobe. Other hydrophobic substituents, such as complex hydrophobes, disclosed for example in U.S. Patent 5,488,180 issued January 30, 1996, are suitable for use in accordance with the present invention.

The monoethylenically unsaturated isocyanates suitable for use in preparing the urethane monomers can be any isocyanates effective to form the desired urethane linkage. Preferably, the isocyanate is a monoethylenically unsaturated monoisocyanate. Any copolymerizable unsaturation may be employed, such as acrylate and methacrylate unsaturation. One may also use allylic unsaturation, as provided by allyl alcohol. These, preferably in the form of a hydroxy-functional derivative, as is obtained by reacting a C2-C4 monoepoxide, like ethylene oxide, propylene oxide or butylene oxide, with acrylic or methacrylic acid to form an hydroxy ester, are preferably reacted in equimolar proportions with an organic diisocyanate, such as toluene diisocyanate or isophorone diisocyanate. The preferred monoethylenic monoisocyanate is styryl, as in alpha, alpha-dimethyl-m-isopropenyl benzyl isocyanate, and this unsaturated

5

monoisocyanate lacks the ester group so it forms urethanes which lack this group. The amount of the monoethylenically unsaturated isocyanate relative to the monohydric surfactant used in making the macromonomer, (on a mole ratio basis) is typically from about 0.1-2.0 to 1, preferably about 1.0 to 1.0.

Suitable macromonomers useful in this invention can also be represented by the formula:

$$R^{1}$$
- $(OR^{2})_{z}$ - R^{3} - C = $CR^{5}R^{6}$

wherein:

 R^1 is a monovalent residue of a substituted or unsubstituted hydrophobe compound; each R^2 is the same or different and is a substituted or unsubstituted divalent hydrocarbon residue;

R³ is a substituted or unsubstituted divalent hydrocarbon residue;

R⁴, R⁵, R⁶ are the same or different and are hydrogen or a substituted or unsubstituted monovalent hydrocarbon residue;

and z is a value of 0 to 150.

Illustrative R¹ substituents include, for example, simple or complex hydrophobe containing from 1 to 30 carbon atoms such as alkyl, aryl, aralkyl, alkaryl and cycloakyl groups.

Illustrative R³ substituents include, for example, the organic residue of ethers, esters, urethanes, amides, ureas, anhydrides and the like including mixtures thereof. The R³ substituent can be generally described as a "linkage" between the hydrophobe bearing surfactant or alcohol and the unsaturated portion of the macromonomer compound.

The oxyalkylene moieties included in the macromonomer compounds may be

5

homopolymers or block or random copolymers of straight or branched alkylene oxides. Mixtures of alkylene oxides such as ethylene oxide and propylene oxides may also be employed.

Further details concerning the preparation of such macromonomers are known to those skilled in the art and are disclosed, for example, in U.S. Patent Nos. 4,514,552, 4,801,671, 5,292,828, 5,292,843 and 5,294,693, incorporated herein by reference.

Typically, the amount of the macromonomer is from about 0.5 to 60 weight percent, preferably from about 5 to 50 weight percent and more preferably from about 35 to 45 weight percent based on the total weight of the dispersant polymer. Typically, the molecular weight of the macromonomer ranges from about 400 to 8000 grams per gram mole.

Typically the viscosity of the dispersants of the present invention is from about 5 to 1500 cP in the un-neutralized form measured at 20°C with a 20 to 50 weight percent solids composition using a Brookfield Viscometer with a number 2 spindle at 60 revolutions per minute. The molecular weight of the dispersants of the present invention is typically from about 10³ to 106, preferably from about 5,000 to 10,000 grams per gram mole. Typically, the particle size of the dispersant is from about 0.05 to 1.0 microns, preferably from about 0.1 to 0.4 microns and more preferably from about 0.1 to 0.3 microns. The Tg of the dispersants of the present invention is typically from about 0 to 90°C preferably from about 5 to 60°C and more preferably from about 15 to 35°C.

The dispersants useful in the present invention contain 0.5 to 50% by weight, preferably 20 to 35% by weight, based on the total weight of the dispersant polymer, of at least one monomer having latent crosslinking functionality.

5

Thickeners

Any suitable alkali soluble thickeners may be utilized in accordance with the present invention. Such alkali soluble thickeners are disclosed, for example, in U.S. Patent Nos. 4,514,552, 4,722,962, 5,292,828 and 5,292,843, which are incorporated herein by reference. The alkali soluble thickeners typically comprise the aqueous emulsion reaction product of an unsaturated carboxylic acid monomer, e.g., methacrylic acid; a monoethylenically unsaturated monomer different from the carboxylic acid monomer, e.g. ethyl acrylate; a macromonomer comprising a hydrophobic portion and an alkoxylated portion which is polymerizable with the other monomers; and a monomer having latent crosslinking functionality. The unsaturated carboxylic acid monomer, monoethylenically unsaturated monomer different from the carboxylic acid monomer, macromonomer and latent crosslinking monomer used to polymerize the thickener can include those such as described above with reference to the binder polymer and dispersant. Often, the macromonomer is a urethane monomer which is the urethane reaction product of a monohydric surfactant and a monoethylenically unsaturated monoisocyanate. Typically, the monohydric surfactant comprises an ethyloxated or propoxylated aliphatic alcohol or alkyl phenol.

In a preferred aspect of the present invention, the thickeners are prepared in accordance using monomers such as those described above with respect to the preferred dispersants.

Typically, the amount of the macromonomer is from about 1 to 20 weight percent, perferably from about 5 to 15 weight percent based on the total weight of the polymer.

Typically, the viscosity of the thickeners of the present invention is from about 5 to 1500 cP in the un-neutralized form measured at 20°C with a 20 to 50 weight percent solids

5

composition using a Brookfield Viscometer with a number 2 spindle at 60 revolutions per minute. The molecular weight of the thickeners of the present invention is typically from about 10^4 to 10^7 , preferably from about 20,000 to 200,000 grams per gram mole. Typically, the particle size of the thickeners is from about 0.05 to 1.0 microns, preferably from about 0.1 to 0.4 microns and more preferably from about 0.1 to 0.3 microns. The Tg of the thickeners of the present invention is typically from about 0 to 90°C, preferably from about 5 to 60°C, and more preferably from about 15 to 55°C.

The thickeners useful in the present invention contain 0.5 to 35% by weight, preferably 1 to 5% by weight, based on the total weight of the thickener polymer, of at least one monomer having latent crosslinking functionality.

The binders, dispersants and thickeners of the present invention are typically in colloidal form, i.e., aqueous dispersions, or in solution and can be prepared by emulsion polymerization in the presence of a chain transfer agent and an initiator. Specific details concerning procedures and conditions for emulsion polymerization are known to those skilled in the art. Typically, however, the polymerization is carried out in an aqueous medium at a temperature of from about 35 to 90°C. The pressure is not critical and is dependent upon the nature of the monomers employed as can be determined by one skilled in the art.

A chain transfer agent is preferably present during the polymerization reaction at a concentration of from about 0.01 to 5 weight percent, preferably from about 0.1 to 2 weight percent based on the total monomer content. Both water-insoluble and water-soluble chain transfer agents can be employed. Illustrative of substantially water-soluble chain transfer agents are alkyl and aryl mercaptans such as butyl mercaptan, mercaptoacetic acid, mercaptoethanol,

3-mercaptol-1,2-propanediol and 2-methyl-2-propanethiol. Illustrative of the substantially water-insoluble chain transfer agents include, for example, t-dodecyl mercaptan, phenyl mercaptan, pentaerythritol tetramercaptopropionate, octyldecyl mercaptan, tetradecyl mercaptan and 2-ethylhexyl-3-mercaptopropionate.

5

In carrying out the emulsion polymerization, an initiator (also referred to in the art as a catalyst) is preferably used at a concentration sufficient to catalyze the polymerization reaction. This will typically vary from about 0.01 to 3 weight percent based on the weight of monomers charged. However, the concentration of initiator is preferably from about 0.05 to 2 weight percent and, most preferably, from about 0.1 to 1 weight percent of the monomers charged. The particular concentration used in any instance will depend upon the specific monomer mixture undergoing reaction and the specific initiator employed, which details are known to those skilled in the art. Illustrative of suitable initiators include hydrogen peroxide, peracetic acid, t-butyl hydroperoxide, di-t-butyl hydroperoxide, dibenzoyl peroxide, benzoyl hydroperoxide, 2,4-dicholorbenzoyl peroxide, 2,5-dimethyl-2,5-bis(hydroperoxy) hexane, perbenzoic acid, t-butyl peroxypivalate, t-butyl peracetate, dilauroyl peroxide, dicapryloyl peroxide, distearoyl peroxide, dibenzovl peroxide, diisopropyl peroxydicarbonate, didecyl peroxydicarbonate, dicicosyl peroxydicarbonate, di-t-butyl perbenzoate, 2,2'-azobis-2,4-dimethylvaleronitrile, ammonium persulfate, potassium persulfate, sodium persulfate, sodium perphosphate, azobisisobutyronitrile, as well as any of the other known initiators. Also useful are the redox catalyst systems such as sodium persulfate-sodium formaldehyde sulfoxylate, cumene hydroperoxide-sodium metabisulfite, hydrogen peroxide-ascorbic acid, and other known redox systems. Moreover, as known by those skilled in the art, traces of metal ions can be added as

5

activators to improve the rate of polymerization, if desired.

The particular surfactant useful for conducting the polymerization reaction is not critical to the present invention. Typical surfactants include anionic surfactants such as sodium lauryl sulfate, sodium tridecylether sulfate, diester sulfosuccinates and sodium salts of alkyl aryl polyether sulfonates; and nonionic surfactants such as alkyl aryl polyether alcohols and ethylene oxide condensates of propylene oxide, propylene glycol adducts.

The reaction products of the polymerizations comprising the binders, dispersants or thickeners of the present invention typically have a solids, i.e., polymer, content of from about 15 to 65 weight percent, preferably from about 20 to 65 weight percent and more preferably from about 25 to 60 weight percent based on the weight of the latex and water.

EXAMPLES

The following examples are provided for illustrative purposes and are not intended to limit the scope of the claims which follow.

Example M1

Preparation of Macromonomer with Small Hydrophobe

To a one-liter glass reactor fitted with a thermometer, heating mantle, thermoregulator, stirrer, nitrogen sparge, and condenser including a Dean-Stark trap was charged 930 grams of a 40 mole ethoxylate of nonyl phenol, i.e., a small hydrophobe. The reactor contents were heated, with nitrogen sparging, to 110°C and held for two hours while trace moisture was removed and collected in the Dean-Stark Trap (typically less than 1g). The reactor contents were then cooled to 80°C, the Dean Stark trap was replaced with a condenser, and the nitrogen sparge was switched to an air sparge for 15 minutes. With continued air sparging, 0.02 g methoxy-

5

hydroquinone inhibitor, 0.50 g dibutyl tin dilaurate catalyst, and 99.7 g of alpha, alpha-dimethyl-m-isopropenyl benzyl isocyanate (m-TMI, a product of CYTEC, Stamford, CT) were charged in order to the reactor. After a rapid initial exotherm which increased the reaction temperature about 8°C, the contents were maintained at 80°C for an additional two hours. The product was then cooled to room temperature. The final product was a white wax in appearance with residual isocyanate content of 0.5% and with 98% of the original ethylenic unsaturation retained.

Example M2

Preparation of Macromonomer with Large Hydrophobe

A macromonomer was prepared substantially in accordance with Example M1, except that a 20 mole ethoxylate of bis-nonylphenoxy ethanol (large hydrophobe) was used in place of the nonylphenol (small hydrophobe) and the amounts of the reacts used were adjusted to maintain a molar ration of 1:1.

Example A

Acrylic Latex Binder Preparation

A monomer mixture was prepared by charging 460 g of butyl acrylate, 520 g of methyl methacrylate, 9.8 g diacetone acrylamide (DAAM), 5.4 g of methacrylic acid, 40 g of Rhodacal DS-4 (a dodecyl benzene sulfonate surfactant available from CYTEC) and 365 g of water to a two liter monomer feed cylinder. A two liter jacketed resin flask equipped with a four-bladed stainless steel mechanical stirrer, Claisen connecting tube, Friedrichs water condenser, nitrogen sparge and bubble trap, thermometer, and monomer addition inlets were used to charge 560 f of water. An initial oxidizer solution, prepared by dissolving 4 g of ammonium persulfate in 20 g of water, was prepared in a separate container. Under nitrogen purge, the reactor was heated to

5

80°C by circulating temperature controlled water through the reactor jacket. After the temperature of the reactor charge had reached 80°C, the initial oxidizer solution was added to the reactor. Two minutes later, the monomer feed was conveyed to the reaction vessel over a 3 hour period by FMI (Fluid Metering Inc.) pumps using 1/8 inch Teflon tubing with continuous stirring while the reaction temperature was held between 79° and 81°C. The reaction was allowed to proceed at 80°C for an additional hour after completion of the monomer feed. To the product was added 15% ammonium hydroxide solution to a pH of 9. To the cooled product was added 36.8 g of a 10% solution of adipic dihydrazide.

Example B

Styrene Acrylic Latex Binder Preparation

A first monomer mixture was prepared by charging 365 grams of butyl acrylate (BA), 470 grams of methyl methacrylate (MMA), 130 grams of styrene, 5.4 grams of methacrylic acid (MAA), 40 grams of diacetone acrylamide (DAAM), 40 grams of TRITON GR-9M (a disodium ethoxylated lauryl alcohol half ester of sulfosuccinic acid surfactant available from Union Carbide Corporation, Danbury, CT) and 450 grams of water to a 2-liter monomer feed cylinder. A two liter jacketed resin flask equipped with a four-blade stainless steel mechanical stirrer, Claisen connecting tube, Friedrichs water condenser, nitrogen sparge and bubble trap, thermometer, and monomer addition inlets was used as the reactor. To the reactor was charged 600 grams of water. An initial oxidizer solution, prepared by dissolving 4 grams of ammonium persulfate in 20 grams of water, was prepared in a separate container. Under nitrogen purge, the reactor was heated to 80°C by circulating temperature controlled water through the reactor jacket. After the temperature of the reactor charge had reached 80°C, the initial oxidizer solution

5

was added to the reactor. Two minutes later, the monomer feed was conveyed to the reaction vessel over a 3 hour period by FMI (Fluid Metering Inc.) pumps using 1/8 inch Teflon tubing with continuous stirring while the reaction temperature was held between 79° and 81°C. The reaction was allowed to proceed at 80°C for an additional hour after completion of the monomer feed.

A second monomer mixture was prepared by charging 36 grams of methacrylic acid (MAA), 72 grams of methyl methacrylate, 120 grams of styrene, 12.5 grams diacetone acrylamide, 1.2 grams of ethylhexyl-3-mercaptopropionate as a chain transfer agent (CTA), 12.5 grams of the macromonomer of Example M1 and 12.5 grams of the macromonomer alpha, alphadimethyl-m-isopropenylbenzylisocyanate adduct with Bis-nonylphenoxy-propylpoly(ethyleneoxy) ethanol (large hydrophobe macromonomer of Example M2), 4 grams of Rhodacal DS-4 and 245 grams of water to a one 2-liter monomer feed cylinder. An additional 4 grams of ammonium persulfate in 20 grams of water, was prepared in a separate container and added to the reactor. The monomer feed was conveyed to the reaction vessel over a 3 hour period with continuous stirring while the reaction temperature was held between 79° and 81°C. The reaction was allowed to proceed at 80°C for an additional hour after completion of the monomer feed.

To the product was added 15% ammonium hydroxide solution to a pH of 9. To the cooled product was added 0.75 molar amounts of adipic dihydrazide.

Table 1 below sets forth a variety of latexes made with the monomers as listed in accordance with the procedure of Example B. Ingredients are listed in grams.

TABLE 1

		1st Stage	2nd Stage	2nd Stage	2nd Stage	2nd Stage	
	<u>Example</u>	DAAM	<u>M1</u>	<u>M2</u>	DAAM	MAA	<u>CTA</u>
	B1	40	0	0	12.5	30	0
5	B2	15	0	12.5	5	36	1.2
	B3	40	12.5	0	12.5	36	0
	B4	15	12.5	12.5	5	36	0
	B5	15	12.5	12.5	5	30	1.2
	B6	15	12.5	0	5	36	1.2
10	В7	40	0	0	12.5	36	1.2
	B8	40	12.5	0	12.5	30	1.2
	В9	15	12.5	0	5	30	0
	B10	40	12.5	12.5	12.5	30	0
	B11	15	0	12.5	5	30	0
15	B12	15	0	0	5 5	36	0
	B13	15	0	0		30	1.2
a , sroom	B14	40	0	12.5	12.5	30	1.2
	B15	40	12.5	12.5	12.5	36	1.2
i,LI	B16	40	0	12.5	12.5	36	0
20	B17	100	0	0	25	48	1.2
1, <u>1</u>	B18	50	0	5 5	12.5	48	1.2
[]	B19	100	0		25	36	1.2
1.2	B20	50	0	0	12.5	36	1.2
	B21	50	0	5	12.5	36	1.2
25	B22	100	0	0	25	36	1.2
	B23	100	0	5	25	48	1.2
[::0]; 2::0];	B24	50	0	0	12.5	48	1.2
tal Fi	B25 ¹	50	0	0	12.5	15	1.2
1 12	B26 ¹	50	0	0	12.5	15	1.2
	$B27^{2}$	50	0	0	12.5	15	1.2
	B28 ² *	50	0	0	12.5	15	1.2
	B29 ³ *	50	0	0	12.5	15	1.2

¹ Methylmethacrylate substituted for styrene monomer in stage1 and stage 2.

² VeoVa10 substituted for BA and styrene in stage 1 and stage2.

³ MMA substituted for styrene and acrylonitrile substituted for 10% by weight of MMA in stage 1 and stage 2.

* Surfactant used was Rhodafac RE-610

10

5

Example C

Latex Binder Preparation

A monomer mixture was prepared by charging 615 grams of VeoVa 10 (a vinyl versatate ester having 10 carbon atoms in the acid portion, commercially available from Shell Chemical), 368 grams of methyl methacrylate (MMA), 9.8 grams diacetone acrylamide (DAAM), 11 grams of methacrylic acid (MAA), 40 grams of Rhodafac 610 (a nonylphenol ethoxylated phosphate ester surfactant available from Rhodia) and 365 grams of water to a 2-liter monomer feed cylinder. A two liter jacketed resin flask equipped with a four-bladed stainless steel mechanical stirrer. Claisen connecting tube, Freidrichs water condenser, nitrogen sparge and bubble trap, thermometer, and monomer addition inlets was used as the reactor. To the reactor was charged 560 grams of water. An initial oxidizer solution, prepared by dissolving 4 grams of ammonium persulfate in 20 grams of water, was prepared in a separate container. Under nitrogen purge, the reactor was heated to 80°C by circulating temperature controlled water through the reactor jacket. After the temperature of the reactor charge had reached 80°C, the initial oxidizer solution was added to the reactor. Two minutes later, the monomer feed was conveyed to the reaction vessel over a 3 hour period by FMI pumps using 1/8" Teflon tubing with continuous stirring while the reaction temperature was held between 79° and 81°C. The reaction was allowed to proceed at 80°C for an additional hour after completion of the monomer feed. To the product was added 15% ammonium hydroxide solution to a pH of 9. To the cooled product was added 0.75 molar amounts of adipic dihydrazide.

Table 2 below sets forth other latexes made with monomers as listed in accordance with the procedure of Example C. Ingredients are listed in grams.

5

10

TABLE 2

<u>Example</u>	<u>VeoVa10</u>	\underline{MMA}	\underline{MAA}	<u>Surfactant</u>
C1	615	368	11	Rhodafac RE-610
C2	487	497	11	Rhodafac RE-610

Example D

Acrylic Latex Binder Preparation

A monomer mixture was prepared by charging 530 grams ("g") of butyl acrylate, 600 g of methyl methacrylate, 23 g diacetone acrylamide (DAAM), 5.4 g of methacrylic acid (MAA), 40 g of Rhodacal DS-4 (a surfactant available from Rhone-Poulenc) and 450 g of water to a one 2-liter monomer feed cylinder. A two liter jacketed resin flask equipped with a four-bladed stainless steel mechanical stirrer, Claisen connecting tube, Friedrichs water condenser, nitrogen sparge and bubble trap, thermometer, and monomer addition inlets were used to charge 800 g of water. An initial oxidizer solution, prepared by dissolving 4 g of ammonium persulfate in 20 g of water, was prepared in a separate container. Under nitrogen purge, the reactor was heated to 80°C by circulating temperature controlled water through the reactor jacket. After the temperature of the reactor charge had reached 80°C, the initial oxidizer solution was added to the reactor. Two minutes later, the monomer feed was conveyed to the reaction vessel over a 3 hour period by FMI (Fluid Metering Inc.) pumps using 1/8" Teflon tubing with continuous stirring while the reaction temperature was held between 79 and 81°C. The reaction was allowed to proceed at 80°C for an additional hour after completion of the monomer feed.

A second monomer mixture was prepared by charging 7.35 grams of methacrylic acid (MAA), 21 grams of butyl acrylate, 7.5 grams diacetone acrylamide (DAAM), 7.35 grams of the

macromonomer M1, 4 grams of Rhodacal DS-4 and 10 grams of ammonium persulfate in 20 grams of water, was prepared in a separate container and added to the reactor. The monomer feed was conveyed to the reaction vessel over a 3 hour period with continuous stirring while the reaction temperature was held between 79 and 81 °C. The reaction was allowed to proceed at 80 °C for an additional hour after completion of the monomer feed.

To the product was added 15% ammonium hydroxide solution to a pH of 9. To the cooled product was added 0.75 molar amounts of adipic dihydrazide.

Table 3 sets forth a variety of latexes made with the monomers as listed in accordance with the procedure of Example D. Ingredients are listed in grams.

10
1.2
<u> </u>
4.1 5
į. <u>.</u>
E
<u> </u>
l=
<u></u>
-
20

25

5

TABLE 3

1st Stage	2nd Stage	2nd Stage	2nd Stage
DAAM	<u>M1</u>	$\overline{\mathrm{DAAM}}$	MAA
23	7.35	7.3	7.5
58	1.8	1.8	15
58	7.35	1.8	15
23	1.8	7.3	7.5
23	7.35	7.3	15
58	1.8	1.8	7.5
23	1.8	7.3	15
58	7.35	1.8	7.5
	DAAM 23 58 58 23 23 58 23	DAAM M1 23 7.35 58 1.8 58 7.35 23 1.8 23 7.35 58 1.8 23 1.8 23 1.8	DAAM M1 DAAM 23 7.35 7.3 58 1.8 1.8 58 7.35 1.8 23 1.8 7.3 23 7.35 7.3 58 1.8 1.8 23 1.8 7.3

Example E

Preparation of Crosslinkable Thickener

A monomer mixture (300 grams) was prepared by charging ethyl acrylate, methacrylic acid, diacetone acrylamide, macromonomer M1, 13 grams of a 75% solution of Aerosol® OT surfactant (American Cyanamid) and 3 grams of distilled deionized water to a bottle, and dispersing the contents with vigorous shaking. The ethyl acrylate, methacrylic acid, diacetone

5

acrylamide and macromonomer M1 were added in amounts identified in Table 4 below. A catalyst feed mixture comprised of 0.53 grams of sodium persulfate and 52.47 grams of water was prepared in another container. To a 2 liter resin flask that had been immersed in a thermostated water bath and equipped with a 4-bladed stainless steel mechanical stirrer, Claisen connecting tube, water condenser, nitrogen sparge and bubble trap, thermometer and monomer and catalyst addition inlets, 1.20 grams of the sodium salt of vinyl sulfonic acid and 658.5 grams of water were charged. The monomer mixture was charged to a 1-liter graduated monomer feed cylinder, and the catalyst solution was charged to a 125 milliliter graduated catalyst feed cylinder. Under nitrogen purge, the reactor was heated to 70°C, whereupon 33 milliliters of the monomer mixture and 3 milliliters of the catalyst feed mixture were charged to the reaction vessel. The reaction vessel was subsequently heated to 80°C. After allowing the monomers to react for 20 minutes to form a seed product, the monomer and catalyst feed mixtures were conveyed to the reaction vessel by FMI pumps via 1/8 inch teflon tubing at a rate of 1.94 and 0.27 milliters/minute, respectively, under continuous stirring at a reaction temperature held between 76° and 82°C. The reaction was allowed to proceed for another hour, after which the product was cooled and filtered with a 200 mesh nylon cloth. The coagulum was collected from the reaction vessel and filter cloth. The product is a low viscosity latex of solids content of about 40% and pH of about 2.5.

Table 4 sets forth a variety of thickeners made with the monomers as listed, in accordance with the procedure of Example E. Ingredients are listed in percentages by weight based on the total weight of the polymer.

15

TABLE 4

	Example	<u>M1</u>	<u>M2</u>	\underline{MAA}	$\underline{\mathrm{EA}}$	<u>DAAM</u>	Surfactant
	E1	15		40	35	10	Rhodafac RE-610
5	E2	5		40	45	10	Rhodafac RE-610
	E3	15		40	40	5	Rhodafac RE-610
	E4	5		40	50	5	Triton GR-9M
	E5		5	40	50	5	Triton GR-9M
	E6		5	40	45	10	Triton GR-9M
10	E7	15		40	35	10	Triton GR-9M
	E8	15		40	40	5	Triton GR-9M

Example F

Preparation of Crosslinkable Dispersant

A monomer mixture (300 grams) was prepared by charging ethyl acrylate, methacrylic acid, diacetone acrylamide, macromonomer M1, 13 grams of a 75% solution of Aerosol® OT surfactant (American Cyanamid) and 3 grams of distilled deionized water to a bottle, and dispersing the contents with vigorous shaking. The ethyl acrylate, methacrylic acid, diacetone acrylamide and macromonomer M1 were added in amounts identified in Table 5 below. A catalyst feed mixture comprised of 0.53 grams of sodium persulfate and 52.47 grams of water was prepared in another container. To a 2 liter resin flask that had been immersed in a thermostated water bath and equipped with a 4-beaded stainless steel mechanical stirrer, Claisen connecting tube, water condenser, nitrogen sparge and bubble trap, thermometer and monomer and catalyst addition inlets, 1.20 grams of the sodium salt of vinyl sulfonic acid and 658.5 grams of water were charged. The monomer mixture was charged to a 1-liter graduated monomer feed cylinder, and the catalyst solution was charged to a 125 milliliter graduated catalyst feed cylinder. Under nitrogen purge, the reactor was heated to 70°C, whereupon 33 milliliters of the monomer

mixture and 3 milliliters of the catalyst feed mixture were charged to the reaction vessel. The reaction vessel was subsequently heated to 80°C. After allowing the monomers to react for 20 minutes to form a seed product, the monomer and catalyst feed mixtures were conveyed to the reaction vessel by FMI pumps via 1/8 inch teflon tubing at a rate of 1.94 and 0.27 milliters/minute, respectively, under continuous stirring at a reaction temperature held between 76° and 82°C. The reaction was allowed to proceed for another hour, after which the product was cooled and filtered with a 200 mesh nylon cloth. The coagulum was collected from the reaction vessel and filter cloth. The product is a low viscosity latex of solids content of about 25%. The product was subsequently neutralized to a pH of about 9.0.

Table 5 sets forth a variety of dispersants made with the monomers as listed, in accordance with the procedure of Example F. Ingredients are listed in percentages by weight based on the total weight of the polymer.

TABLE 5

	Example F1 F2 F3	<u>M1</u> 30	<u>M2</u> 30	MAA 17.5 17.5 17.5	EA 32.5 47.5 17.5	DAAM 20 5 35	Surfactant Rhodafac RE-610 Triton GR-9M Triton GR-9M
	F4 F5	30 37.5		17.5 17.5	32.5 25	20 20	Triton GR-9M Rhodafac RE-610
20	F6	37.5		17.5	10	35	Triton GR-9M
	F7 F8	45	37.5	17.5 17.5	32.5 40	5 5	Triton GR-9M Triton GR-9M
	F9		37.5	17.5	25	20	Triton GR-9M Triton GR-9M
25	F10 F11		45 45	17.5 17.7	17.5 2.5	20 35	Triton GR-9M Triton GR-9M
	F12	30		25 25	35 25	10 20	Triton GR-9M Triton GR-9M
	F13 F14	30 30		25 40	20	10	Triton GR-9M
20	F15	30		25 17.5	40 25	5 5	Triton GR-9M Triton GR-9M
30	F16	30		11.3	23	5	1111011 010 7111

The binders, thickeners and dispersants described above were used in the formulation of paints as described below. The paint formulations may, in addition to the polymers described herein, contain conventional additives, such as pigments, fillers, wetting agents, coalescants, biocides and anti-foaming agents and the like.

Example G

Preparation of Latex Paint

10

5

A pigment grind is prepared by adding the following ingredients in sequence: 54.96 grams of water, 5.92 grams of a 28% aqueous ammonia solution and 2.76 grams of Dispersant F9 to a HSD-type grinding apparatus with low agitation. Slowly added are 200.8 grams of TiPure R-706 titanium dioxide pigment (DuPont) while the agitation is increased. The mixture is ground for approximately 1 hour, or until a fineness of grind of 8 Hegman is obtained. The agitation is reduced and 25.6 grams of ethylene glycol and 1.8 grams of BYK 035 defoamer is added.

A thickener premix is prepared by adding 10.32 grams of water to a mix tank and under agitation, adding 0.25 grams of Thickener E5 and 0.05 grams of 28% aqueous ammonia solution to the tank.

20

The paint is prepared by adding 568.72 grams of Binder resin C2 to the grind mixture under agitation. After this mixture is agitated for about 30 minutes, the following ingredients are added in order: 21.64 grams of Exxate 1000 (Exxon), 5.44 grams of Arcosolve DPNB (dipropylene glycol n-butyl ether from Arco Chemicals) and 11.64 grams of Exxate 900 (oxononyl acetate from Exxon). The thickener premix is then added under agitation. Flash X-

5

150 flash rust inhibitor (Halox) in an amount of 2.6 grams is then added, followed by 1.48 grams of Surfynol 104BC defoamer (Air Products) and 1.48 grams of Byk 307 (wetting agent from BYK-Chemie). Dispersant F9 is then added in an amount of 2.76 grams. The paint is mixed until it is homogeneous and then reduced with 54.57 grams of water to the desired application viscosity.

Example H

Preparation of Paint

A pigment grind is prepared by adding the following ingredients in sequence: 54.96 grams of water, 5.92 grams of a 28% aqueous ammonia solution and 2.55 grams of Dispersant F5 to a HSD-type grinding apparatus with low agitation. Slowly added are 200.8 grams of TiPure R-706 titanium dioxide pigment (DuPont) while the agitation is increased. The mixture is ground for approximately 1 hour, or until a fineness of grind of 8 Hegman is obtained. The agitation is reduced and 25.6 grams of ethylene glycol and 1.8 grams of BYK 035 defoamer is added.

A thickener premix is prepared by adding 10.32 grams of water to a mix tank and under agitation, adding 0.25 grams of Thickener E5 and 0.05 grams of 28% aqueous ammonia solution to the tank.

The paint is prepared by adding 581.48 grams of Binder resin B29 to the grind mixture under agitation. After this mixture is agitated for about 30 minutes, the following ingredients are added in order: 21.64 grams of Texanol (Eastman Chemicals), 5.44 grams of Arcosolve DPNB (dipropylene glycol n-butyl ether from Arco Chemicals) and 12.73 grams of Exxate 900 (oxononyl acetate from Exxon). The thickener premix is then added under agitation. Flash X-

150 flash rust inhibitor in an amount of 2.6 grams is then added, followed by 1.48 grams of Surfynol 104BC defoamer (Air Products) and 1.48 grams of Byk 307 (wetting agent from BYK-Chemie). Dispersant F9 is then added in an amount of 2.76 grams. The paint is mixed until it is homogeneous and then reduced with 45.5 grams of water to the desired application viscosity.

5

Examples 1-88 were prepared substantially in accordance with the procedure of Example G. The following criteria were used to evaluate the quality of the coatings 1-88. For evaluation of the coatings for ambient cure chemical coating applications, each coating was applied to Bonderite 100 substrates. Adhesion was evaluated by applying the coatings to treated aluminum, Lexan, ABS, Noryl and Styron substrates. QUV evaluations were conducted on coatings applied to aluminum substrates. Table 7 shows the results of the evaluations of the coatings for ambient cure chemical coating applications. These coatings were compared to commercially available polyurethane coatings, Polane® 700T, a one-component waterborne polyurethane and Polane®HS Plus, a two-component solvent borne polyurethane.

For the evaluation of the coatings for industrial maintenance applications, the coatings were applied to cold rolled steel substrates. Adhesion was evaluated by applying the coatings to weathered aluminum and weathered galvanized steel substrates. Corrosion, humidity, salt spray and 24 hour water soak were evaluated by applying the coatings on blased steel panels. QUV evaluations were conducted on coatings applied to aluminum substrates. Table 8 shows the results of the evaluations of the coatings for industrial maintenance applications. These coatings were compared to commercially available coatings, Polylon® 1900, a two-component solvent borne polyurethane coating, CenturionTM, a two-component waterborne polyurethane coating, and Sher-crylTM, an acrylic enamal coating.

For the evaluation of the coatings for oven bake applications, the coatings were applied to Bonderite 1000 substrates. Adhesion was evaluated by applying the coatings to weathered aluminum and weathered galvanized steel substrates. QUV evaluations were conducted on coatings applied to aluminum substrates. Table 9 shows the results of the evaluations of the coatings for oven bake applications. These coatings were compared to commercially available coatings Kem Aqua® 1700T and Kem Aqua® 1400, both water reducible enamel coatings.

AMBIENT CURE

Property	Test Method	Measurement
Chemical Resistance	ASTM D3912-80 24 hr. exposure Key Chemicals: 1. Formula 409 2. isopropanol 3. MEK 4. Toluene 5. 10% NaOH 6. 10% sulfuric acid 7. Deep Woods Off Spray 8. Coppertone 30	rating 1. Total Failure 2. severe Failure 3. slight failure 4. minimal failure 5. no effect
Pencil Hardness	ASTM D3363	Use film breakthrough
Salt Spray	ASTM B117	200 hours
MEK Rubs		Until substrate shows
Gloss		60°, 20°
Reverse Impact Test	ASTM D2794	Until film breakage
Impact Resistance	ASTM D2794	Until film breakage
QUV	ASTM D4587-91 Method B	1000 hours
Storage Stability	4 weeks at 120°F	4 weeks, check viscosity as settling
Adhesion	ASTM D3359 Key substrates: 1. Treated Aluminum 2. Lexan 3. ABS 4. Noryl 5. Styron	Tape adhesion
48 hr. Water Immersion		Blister, Rust, Tape adhesion

OVEN BAKE

Property	Test Method	Measurement
Chemical Resistance	ASTM D3912-80 24 hr. exposure	rating 1. Total Failure 2. severe Failure 3. slight failure 4. minimal failure 5. no effect
QUV	ASTM D4587-91 Method B	1000 hours
Pencil Hardness	ASTM D3363	Use film breakthrough
Gloss		60°, 20°
Corrosion-Weathering	ASTM D5894-96	6 cycles
Salt Spray	ASTM B117	500 hrs.
Reverse Impact Test	ASTM D2794	Until film breakage
Impact Resistance	ASTM D2794	Until film breakage
Storage Stability	for 4 weeks at 140°F	Check Viscosity and Settling
Early Blister Resistance	2,4, and 6 hrs after application	Blister and Rust
Adhesion	ASTM D3359 Key Substrates: 1. Weathered Aluminum 2. Weathered Hotdipped Galvanized	Tape Adhesion

	T	T	Т	T	Τ	Γ	Т	T	Т	П	Т	П	Т	<u> </u>	Т	Г		Π	T	ſ	Т	Т	Т	Г	Г	П		Г	Г	Ι	r —	_			Į		т-	Т	٦	
043	042	041	040	039	038	037	036	035	034	033	032	031	023	022	021	020	019	018	017	016	015	014	013	012	011	010	009	008	007	006	005	004	003	002	901	Formula				
3	3	2	2	2	2	2	2	2	2	2	2	2	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	3	ω	ω	з	3	з	Resin			T	
1	-	7	7	2	===	æ	ω	_	1	4	3	2	3	11	3	11	7	2	1	5		11	8	3	10	10	3	ۍ.	_	3	11	2	7	8	2	Dispersant			1	
2	2	-		-	-	-	_			2	2	2	-	-1	_	-	-		-		1	2	2	2	2	2	2	2	2		1	1	1	-	1	Dispersant amount				
1	4	6	8	8	2	4	4	5	7	8	6	-	7	2	6	4		4	æ	ω	2	8	7	7	2	2	ω	5	7	7	7	6	5	5	3	Thickener				
1.52	1.78	2.16	1.72	1.86	1.98	2 06	2.09	1.91	1.88	1.99	1.82	1.98	2.06	1.78	1.8	1.76	1.73	1.69	1.84	1.56	1.8	2.01	1.89	1.74	1.78	2.04	1.82	1.77	2 03	1.71	1.95	2.24	2.01	1.95	1.76	Film build			4	
19.6 54.2	23.5	23.6	27.2	24.2	34.5	15.4	16.1	15.6	25.2	13.0	37.4	22.4	39.1	30.0	33.1	31.4	13.4	33 5	21.4	37.9	30.7	28.1	11.7	20.8	7.1	13.3	31.5	33.4	34.3	16.5	26.4	4.3	30.3	23 5	5.9	20 gloss			AMBLEINT	'Tak
54.2	59.2	58.7	62.3	58.7	67.1	48.5	50.2	48.9	59.9	44.8	67.9	56.7	69.1	65.2	67.4	66.0	46.3	66.9	57.8	68.7	64.8	64.5	43.0	56.6	35.5	48.0	65.0	67.9	67.8	51.3	61.9	24.8	64.6	58.6	29.4	60 gloss			VI CUKE	
4	4	4	4.5	4	4	4	4	4	5	4.5	4.5	5	5	5	5	4	5	4.5	4.5	5	4.5	4	4	4	4	5	5	4.5	5	5	5	4	51	3	1	Coppertone				
2 .	2	2	2	2	2	1	2	2	2	2	2	2	3.5	3	3	3	3	3	3.5	3	3.5	3.5	3	3	3.5	3	3	3	4	2	2	သ	ω	ω	3	Toluene				
3	2	3	2	ဒ	2	အ	ű	3	ω	2.5	အ	သ	თ	თ	4	သ	4	გ	5	5	წ	4	თ	4.5	ڻ.	5	4	5	5	3	2	3	3	2	3	IPA	₽			
2	2	2	2	2	2	1	2	2	2	2	2	2	3	5	4	3	3.5	5	3.5	3	3	3.5	3	3	4	3	4	5	თ	3	2	ω	ა	2	3	MEK	Chemical Resistance			
2	2	2	2	2	2	2	2	2	2	2	2	2	2	2	2	2	2	2	2	2	2	2	2	2	3.5	2.5	3.75	3.5	3.75	2	2	2.5	2.5	2	2	DWO	sistance	***************************************		
5	2	5	5	3	5	4.5	4	5	4.5	3	4	4	4	5	თ		ۍ.	5	Çī.	4	5	ပ ၢ	۲'n	υı	Մո	5	ა ი	5	ST.	4.5	4	5	4	3	51	10% Sulf				
2	2	2	2	2	2	2	2.5	2.5	2	2	2	ω	Ch	4	3.5	3.5	4.5	3	ω	ω	3.5	ω	4	4	4	4	3	4	4	3	2	з	ယ	3	3	NaOH				
5	4	4.5	4	4.5	ယ	4	5	4.5	4.5	O1	3	4	G	5	Cī	Cħ.	5	5	տ	5	4	5	ა	51	տ	4	3.5	5	6	5	5	5	5	ъ.	5	F409				

Table 7 (Cont.)
AMBIENT CURE

HS+	700T	1									T				Γ	Γ														_ 						Fo		T
	Ŀ	088	18/	086	085	182	083	082	081	080	079	078	077	976	075	074	073	972	071	070	069	890	067	055	054	053	052	051	ن50	049	048	047	046	045	044	Formula		
		2	2	2	2	_	-	-	_			_	_	-		_	_	-	-	_	-	_	-	3	2 .	3	3	3	3	3	3	3	3	3	ပ	Resin		
		8	5	5	-	3	9	10	7	3	2	9	9	6	5	2	7	11	3	ы	8		ហ	8	8	9	9	5	3	8	11	7	8	5		Dispersant		
		2	2	2	2	_	-	_	1	_	1			_	_	2	2	2	2	2	2	2	2	2	-1	1	-		2	2	2	2	2	2	2	amount		
		4	7	7	သ	6	51	1	သ	8	-	4	თ		2	5	O	Ç1	N	2	2	6	သ	4	4	2	1	4	5	6	ယ		3	8	7	Thickener		
1.96	2.08	1.90	1.67	1.38	1.70	2 06	1.56	1.82	1.88	1.93	1.89	1.62	2.00	2.03	2.10	1.76	1.58	1.48	1.64	1.68	1.61	1.60	1.64	1.77	3.53	2.34	2.18	2.30	1.75	1.64	1.70	1.74	1.45	1.50	1.72	Film build		1
89.8	2.5	17.8	33.8	240	30.9	35 4	34.6	27.8	32.4	32.4	28.4	28.0	30.8	21.9	30.6	33.0	32.7	36.4	32.2	34.7	37.8	36.5	27.7	8.6	150	22.6	25.2	29.1	15.5	26.8	25.6	28.0	7.2	26.3	9 1	20 gloss		
90.1	29.5	53 6	66.5	60.2	64.6	69 0	68.8	62.5	67.0	67.7	62.9	65.8	66.5	59.2	67.1	67.8	69 3	69.8	67.5	69 8	71.3	70.8	65.0	35.8	48.9	57.9	59.4	63.6	49.9	63.6	61.0	62.5	32.5	62.0	38.4	60 gloss		
4	2.5	4	4	S1	5	5	4.5	4.5	4	51	4	4.5	4.5	ڻ.	O1	4.5	5	4.5	4	4.5	4	3	5	4	5	4	5	4	4	4.5	4	4	4.5	4	4	Coppertone		
D.	· 2	2	N	2	2	3	3	2	3.5	3.5	3.5	3	3.5	သ	ω	4	4	5	4	3.5	4	3	5	ယ	သ	2	2	2	2	2	2	2	2	3	2	Toluene		
7	ω	ω	3	2	3	4.5	4	5	4.5	3	4	4.5	4	55	ა	5	5	5	5	5	5	4	5	ω	ω	3	2.5	5	2	3	3	ω (۱ د	١,	3	IPA	0	
ת	4.5	2	2	2	2	ω	з	2	ယ	3	4	3	သ	ω	ς,	ω	5	5	3	3.5	ω	4	5	ωı	2	3	2	2 1	2	2	3	2	٠ ر ۱	٥,	3	MIL X	hemical R	
	-	2	2	2	2.5	2	2.5	2.5	2	2	2	2	2	2	2	2	2	2.5	N	ω	3.5	2.5	2.5	-	25	١,	3 !	2	3	2	2 !	y !	J ,	3 1	3	DWO	Chemical Resistance	
n	3.5	4	Сī	5	3.5	ω	ω	4	4	3	ယ	3	3	3	ω	2	ω	3	3	2	ω	,	ω,	5 0	ט ת	7 .	4	י ת	n (ω .	4	י ע	7 (3 ,	, 0,0	10% Sulf		
,	2.5	2	2	2	2	2	2	2	2	2	-	2	2	2	2	ω	2	2	2	2	2	<u>،</u> ا	٥١	n (ه ا د	ماد	ه ،	2	٠,	2 1	2	3	3 N	ء اد	2	N0%		
	2	ω	ω	2	4	5	ω	5	5	5	5	5	4.5	4.5	5	ا 4	54	5	ω	5	5n .	۰ م	، د	מ	, c	ח כ	n c	л	,	л с	, ,	- c	ن	, j	4.5	F409		

Table 7 (Cont.)
AMBIENT CURE

Г	Γ	Т	T	Т	Т	Т	T	Т	T	Т	 	_	T	Т	1	т-	Т	T	_	Τ-	_	т-	т	T	Т	Т	γ	_	ı						_	·			
043	042	041	040	039	038	037	036	035	034	033	032	81	023	022	021	020	019	018	017	016	015	014	013	012	011	010	009	900	007	ბ06	005	004	003	902	<i>υ</i> 01	Formula			
4	4	4	5	4	4	4	5	4	4	5	4	4	4	4	4	5	4	4	6	5	4	თ	4	5	5	51	5	6	4	3	4	4	5	4	4	Hardness		Pencil	
8	8	8	8	8	6	8	8	8	6	8	.80	8	•	6	6	6	8	8	8	4	6	6	8	6	8	8	6	4	8	6	8	8	8	œ	œ	Blister size			
4	4	3	3	2	2	ű	з	4	4	3	2	2	4	-	_	_			-	2	-		1	1		1	1			4	4	4	2	3	4	density	Blister		
8	9	7	ζħ	8	7	o	6	5	စ	5	6	5	8	မ	8	8	7	&	6	7	8	7	7	6	6	6	6	6	۲٦.	7	7	10	4	6	8	Rust	Tulling	13	
no	yes	yes	yes	по	no	yes	yes	yes	yes	yes	yes	yes	yes	yes	yes	yes	yes	yes	yes	yes	yes	yes	yes	yes	yes	yes	yes	yes	yes	no	οn	9	yes	yes	on	or N	Flash rust-Y	200	
46.2	51.4	47.3	49	39.5	49.6	38.4	42.6	43.5	49.9	38	61.5	42.4	23.2	17.3	19.1	16	17.5	27	29.4	18.9	17.8	16.1	21.3	15.2	11.7	16.7	15.4	16.8	16	42.3	54.4	24.4	42.7	46.2	23.8	Gloss			
-14.76%	-13.18%	-19.42%	-21.35%	-32.71%	-26.08%	-20.82%	-15.14%	-11.04%	-16.69%	-15.18%	-9.43%	-25.22%	-66.43%	-73.47%	-71.66%	-75.76%	-62.20%	-59.64%	-49.13%	-72.49%	-72.53%	-75.04%	-50.47%	-73.14%	-67.04%	-65.21%	-76.31%	-75.26%	-76.40%	-17.54%	-12.12%	-1.61%	-33.90%	-21.16%	-19.05%	gloss	% Change		
2	2	2	2	2	2	2	2	2	2	2	2	2	2	4	4	4	4	4	4	4	2	2	2	2	2	2	2	2	2	2	2	2	2	2	2	size	Blieber	T	
-		-	2	2	2	_			1	1	1		ω	4	ω	ω	ω	4	ω	3	ω	ы	4	ω	4	з	3	3	2	2	2	2	2		2	density	Salt Spray-		
6	6	7	7	8	6	4	6	ე	7	7	6	6	9	9	7	7	7	9	8	7	8	8	9	7	9	8	7	8	7	6	5	7	5	5	6	Rust	Spray-100 Hours		
9	9	9	9	9	9	9	9	9	9	9	9	9	7	6	6	7	6	7	6	6	7	6	6	6	4	9	6	ט פ	9	9	٥	9	9	9	9	Scribe			
2	2	2	2	2	2	2	2	2	2	2	2	2	2	4	4	4	4	4	4	4	2	2	2	2	2	2		١,	٥	2	2	2	2	2	2	size	1		
<u>-</u> -	- -	0	2	2	2	-	-		_	-	_	-	3	4	ω	3	3	4	ω	ω	3	2	4	ω.	4	ω	,	2	١	2	3	١	2	-	2	density	Salt Spray-200 hours		
o (s .	7	7	8	o .	4	6	5	7	7	6	6	8	9	7	7	7	9	8	7	8	8	9	7	9	8	ļ	a -	7 6	D (η -	7	ית	5	6	Rust	200 hours		
، او	٥	٥	، او	، و	٥	، ام	٥	9	9	9	9	9	7	6	o .	7	s .	7	6	6	7	5	5	5	4	او		n 0	٥	ه ا ه	٥	٥	،	ام	9	Scribe			

Table 7 (Cont.)

AMBIENT CURE

+SH	700T					<u> </u>			_	Γ			Γ	Γ							Γ															Ţ	Т	Τ
	T	088	087	086	085	084	083	082	081	080	079	078	077	076	075	074	073	072	071	070	069	068	067	055	054	053	052	251	050	049	948	947	, 046	045	044	Formula		
6	6	ω	З	4	4	2	3	4	w	s	4	4	2	2	4	4	4	4	4	2	2	u	2	4	4	4	4	4	5	4	5	5	2	4	5	Hardness	Pencil	
none	none	8	8	6	6	6	8	8	8	8	æ	8	8	8	8	8	8	8	8	8	8	8	8	8	8	8	8	8	8	8	8	8	8	8	8	Blister size		
none	none	2	2	3	3	3	3	2	4	3	4	3	3	2	2	3	2	3	3	s	4	3	2	4	4	4	3	3	4	4	4	2	3	4	4	density	Blister	
none	none	თ	7	ა	თ	6	7	8	8	6	7	7	8	6	6	7	5	4	4	4	6	5	51	6	7	8	9	9	9	9	8	9	7	7	9	Rust	Humid	
no	no	yes	yes	yes	yes	yes	yes	yes	yes	yes	yes	yes	yes	yes	yes	no	yes	20	yes	yes	yes	yes	no	yes	yes	no	ПO	yes	OO	or N	Flash rust-Y							
68.5	36.6	44	49.7	47.6	50.8	16.8	25.1	24.2	37.1	18.6	20.9	28.3	28.4	27.5	25	33.8	29.4	30	28.3	26.8	22.1	29.7	27.8	31.3	41.1	51.1	44.8	44.4	39.5	48.4	40.1	43.7	25.7	45.6	35.2	Gloss		
-23.97%	24.07%	-17.91%	-25.26%	-20.93%	-21.36%	-75.65%	-63.52%	-61.28%	-44.63%	-72.53%	-66.77%	-56.99%	-57.29%	-53.55%	-62.74%	-50.15%	-57.58%	-57.02%	-58.07%	-61.60%	-69.00%	-58.05%	-57.23%	-12.57%	-15.95%	-11.74%	-24.58%	-30.19%	-20.84%	-20.66%	-35.84%	#REF!	-20.92%	-26.45%	-8.33%	gioss	% change	
10	6	2	2	2	2	4	4	2	6	4	6	4	4	4	4	4	4	6	4	4	6	4	6	4	2	4	2	2	2	4	4	4	2	2	2	size	Blister	
5	3	-	_	_	-	2	1	2	2	2	2	1	2	2	_	2	2	_		2	1	2	1	_	_	သ	2	2	2	2	-	2	-			density	Blister	
10	7	6	6	6	2	7	7	8	8	7	8	8	7	6	6	7	7	8	3	з	2	2	2	2	6	-1	6	8	6	6	6	6	6	6	6	Rust	Blister Hours	
9	6	9	9	9	9	9	7	7	9	9	8	7	9	9	9	9	9	9	9	9	9	9	9	9	9	9	7	9	9	9	9	9	9	7	9	Scribe		
10	6	2	2	2	2	4	4	2	6	4	6	4	4	4	4	4	4	6	4	4	6	4	6	4	2	4	2	2	2	4	4	4	2	2	2	size	Blister	
5	ω	-	-1	1	-	2	1	2	2	2	2	-1	2	2		2	2		-1	2	-	2		-	-	з	2	2	2	2	_	2	-1	_	_	density	Blister Blister	
10	7	6	6	2	2	7	7	8	8	7	8	8	7	6	6	7	7	8	3	ω	2	2	2	2	6	8	6	8	6	6	6	6	6	6	6	Rust	200 nours	
9	6	9	ဖ	9	9	9	7	7	9	9	8	7	9	9	9	9	မ	g	9	9	8	9	9	9	8	9	7	8	9	9	9	9	9	7	9	Scribe		

Table 7 (Cont.)
AMBIENT CURE

					1,147,177,11,11,1	COME					ı
	lm	Impact				Adhesion				48 Hr	tr Water Soak
Formula	Forward	Reverse	MEK rubs	Treated aluminum	Noryl	ABS	Lexan	Styron	Blister size	Blister	
001	36	4	132	з	0	0	-	٥	10	5	
002	40	4	50	4	0	0	2	-	6	4	
003	44	8	100	3	-	0		-	8	3	\perp
004	40	4	50	ယ	0	3	3	2	70	5	\bot
005	40	8	50	3	۵	0	0	-1	10	5	
006	40	8	150	သ	-	-	0	0	10	5	
007	> 168	> 168	150	3	÷	0	0	-	4	З	\rightarrow
008	> 168	> 168	750	3	-	0	0	-1	6	2	
009	140	> 168	400	4	-	0	0	<u>-</u>	6	-	
010	> 168	> 168	46	4	<u>.</u>	0	0	-	6	4	
011	> 168		49	4	<u>-</u> .	0	0	<u>.</u>	10	5	
012	> 168	> 168	1000	2	0	0	0	0	8		
013	> 168	> 168	40	5	-1	0	0	<u>.</u>	6	5	
014	> 168	> 168	46	5	-1	0	0	-	8	2	
015	> 168	> 168	45	4	-1	-1	0	0	8	-	
016	> 168	> 168	50	2	0	0	0	ᅩ	8	-	
017	> 168	> 168	187	3	.	0	0	<u>.</u>	8	ω	
018	> 168	> 168	45	3	-	0	0		8	2	
019	> 168	> 168	47	ဒ	-1	0	0	.	8	2	
020	> 168	> 168	500	4	-1	0	0	∸	8	_	
021	> 168	> 168	750	u	<u>-</u>	0	0	÷	8	>	
022	> 168	> 168	150	ω	<u>.</u>	0	0	<u>.</u> .	8	2	
023	> 168	> 168	150	3	÷	2	0	÷	8	-	
031	36	^4	200	ω	-1	0	3	2	8	_	
032	36	<.4	50	3	0	0	2	0	6	2	
033	32	< 4	400	4	0	0	0	ပ	8	-	
034	32	4	29	သ	-	0	1		6	2	
035	36	^4	130	4		3		3	8	-	
036	32	< 4	100	3	<u>.</u>	0	0	ω	6	ω	
037	32	^4	46	4	÷	0	0	0	6	4	
038	36	8	300	4	<u></u>	-1	0	0	ō	2	
039	8	4	650	3	0	0	0	0	6	3	
040	32	^4	42	3	-1	0	0	2	&	_	
241	32	^4	38	4	0	0	2	0	8	_	
042	56	8	75	4	<u></u>	0	0	. 0	6		
043	40	4	45	4	-	0	0	0	10	5	

Table 7 (Cont.)
AMBIENT CURE

	lmı	Impact				Adhesion				48 Hr W	Water Soak	
Formula	Forward	Reverse	MEK rubs	Treated aluminum	Noryi	ABS	Lexan	Styron	Blister size	Blister	Rist	Adhesion
044	40	4	150	4	0	0	-	۵	8	4	10	4
045	40	8	48	4		0	0	<u>-</u>	8	3	5 6	١
046	28	< 4	50	3	0	0	0	<u>-</u>	8	_ ,	10 0	ω (
347	40	8	39	3	<u>ن</u>	0	0	-	8	ω	10	ا د
048	44	8	146	3	0	0	0	2	8	3	10	ی ر
049	92	40	100	4	0	0	သ	0	8	_	10 0	0
050	76	12	300	သ	0	0	2	0	8	_	10	2
051	56	6	48	ω	0	0	0	0	6	ω	10	ا د
052	36	8	42	IJ	۵	÷	0	اد	6	ω	10	، د
053	36	4	200	3	-	0	0	0	10	5	10	3
054	44	4	200	3		0	2	-	8	2	9	ω
055	36	4	150	3	0	0	ω	-	8	2	5	3
067	56	12	800	3	0	0	0	သ	10	5	10	4
068	64	20	100	3	2	0	0	2	10	5	10	4
069	84	20	800	3	4	-	2	3	10	5	70	5
070	56	12	200	ω	N	0	2	2	10	5	10	ω
071	68	16	100	3	o,	0	0	4	10	5	10	3
072	52	8	1000	w	4	0	÷	4	10	51	10	3
073	60	&	250	3	2	0	0	ယ	10	5	6	4
074	2	4	300	3	з	0	0	-	10	5	10	4
075	56	8	43	3	0	٥	0	-	10	5	10	4
076	56	4	50	3	0	0	ω	4	10	5	10	4
077	56	8	700	ω	0	0	0	3	10	Մո	6	3
078	60	12	18 8	.3	0	0	2	4	10	ڻ د	10	3
079	52	æ	100	3	0	0	-	ω	10	5	10	3
080	56	4	1000	3	з	0	0	ဃ	10	5	10	3
081	52	8	350	3	0	0	0	2	10	5	10	4
082	60	8	300	3	4	0	0	4	10	ហ	6	4
083	56	4	1000	3	0	0	۵	3	10	5	10	3
084	60	12	350	3	0	0	0	4	10	5	10	4
085	36	^4	37	4	0	0	0	0	6	2	ω	-
086	36	4	250	4	0	0	_	2	6	2	-	-
087	32	4	246	3	<u>.</u>	0	0	٥	6	_		٠.
088	32	44	100	3	0	0	-		4	ω	6	0
700T	> 168	> 168	150	ω	-	5	5	-1	8	4	10	4
HS+	68	8	1000	3	<u>.</u>	თ	თ	ა	5	5	10	4

Table 7 (Cont.)

AMBIENT CURE

	_												_	_	_	,	_			_	_								-									-
042	041	040	039	038	037	036	035	034	033	032	031	023	022	021	020	019	018	017	016	015	014	013	012	011	010	009	800	007	906	005	004	003	ა02	001	Formula			
55.20	60.50	63.20	60.00	66.80	51.80	53.00	52.50	60.90	47.10	68.70	57.70	71.80	67.80	70.70	68.70	49.20	69.00	59.30	70.70	66.10	69.10	46.80	59.30	40.60	52.00	68.30	70.30	69.40	51.00	61.00	49.60	65.70	56.50	32.60	Initial	Glos		
36.20	43.40	47.60	48.30	57.30	41.70	40.00	36.00	44.40	29.00	47.10	37.50	22.10	21.70	22.00	21.10	12.90	19.00	14.50	19.70	18.20	19.60	15.00	16.50	10.40	13.80	21.90	30.50	33.30	35.80	47.00	29.80	50.70	40.10	21.10	at 500 hrs	Gloss (60 degree)		
-33.28	-28.26	-24.68	-19.50	-14.22	-19.50	-24.53	-31.43	-27.09	-38.43	-31.44	-35.01	-69.22	-67.99	-68.88	-69.29	-73.78	-72.46	-75.55	-72.14	-72.47	-71.64	-67.95	-72.18	-74.38	-73.46	-67.94	-56.61	-52.02	-29.80	-22.95	-39.92	-22.83	-29.03	-35.28	%schang	ree)		
1.36	1.63	1.49	1.86	1.40	1.78	1.29	1.42	1.88	1.38	1.61	1.65	1.31	1.31	1.57	1.37	0.45	0.92	0.61	1.39	1.00	1.10	1.31	0.73	0.26	1.05	1.06	1.17	1.81	1.34	2.05	1.17	1.81	2.69	0.94	Initial			***************************************
2.38	1.49	1.37	1.61	1.36	2.45	1.18	0.73	1.79	2.19	0.77	1.38	1.87	2.79	2.34	2.09	2.25	2.01	1.80	1.88	2.01	2.45	2.83	1.95	3.03	3.14	1.98	1.41	2,49	3.16	3.44	2.66	2.72	5.10	3.23	at 500 hrs	Delta E	QUV-500 hours	
1.02	0.14	0.12	0.25	0.04	0.67	0.11	0.69	0.09	0.81	0.84	0.27	0.56	1.48	0.77	0.72	1.80	1.09	1.19	0.49	1.01	1.35	1.52	1.22	2.77	2.09	0.92	0.24	0.68	1.82	1.39	1.49	0.91	2.41	2.29	change		CLS	***************************************
-0.88	-0.83	-1.05	-0.80	-0.81	-0.82	-0.86	-1.18	-0.61	-0.89	-1.33	-0.98	0.06	0,08	-0.10	-0.29	-0.30	-0.26	-0.46	-0.44	-0.29	-0.32	0.05	-0.45	-0.13	0.01	-0.31	-0.32	0.04	-0.46	-0.36	-1.00	0.79	0.41	-0.85	Initial			
1.20	0.81	0.71	0.82	69.0	1.40	0.59	0.21	0.86	1.24	0.15	0.65	0.95	1.63	1.24	1.17	1.16	1.10	0.86	0.94	1.03	1.38	1.60	26.0	1.75	1.83	1.06	0.83	1.43	1.76	1.92	1.36	1.42	2.79	1.55	at 500 hrs	Delta b		
2.08	1.64	1.76	1.62	1.46	2.22	1.45	1.39	1.47	2.13	1.48	1.63	0.89	1.57	1.34	1.46	1.46	1.36	1.32	1.38	1.32	1.70	1.55	1.40	1.88	1.82	1.37	1.15	1.39	2.22	2.28	2.36	0.63	2.38	2.40	change			
31.80	44.80	49.40	50 70	58.70	43 60	39.20	36.70	47.80	26.10	54.90	35.90	23.20	16.00	14.90	16.40	10.40	15.90	12.30	18.10	15.50	15.90	12.30	12.70	7.50	9.80	15.20	21.20	21.90	32 80	45 60	26.50	48 20	37.10	17 90	1000 hour	Gloss (60		
-34.10 -42.39	-25.95	-21.84	-15.50	-12.13	-15.83	-26.04	-30.10	-21.51	-44.59	-20.09	-37.78	-67.69	-76.40	-78.93	-76.13	-78.86	-76.96	-79.26	-74.40	-76.55	-76,99	-73.72	-78.58	-81.53	-81.15	-77.75	-69 84	-68.44	-35.69	-25.25	-46.57	-26.64	-34.34	-45.09	% change	(60 degree)		
2.67	2.12	1.54	1.89	1.81	2 30	1.63	1.33	2.51	1.93	0.75	1.42	2.59	3.51	2.87	2.72	2.54	2.58	2.40	2.36	2.29	3 01	3.40	275	3.85	4 00	2 44	2 58	4.09	3 62	4 04	2 66	3 02	5 70	2 88	Delta E	Delta E	QUV1000 hrs	
1.31	0.49	0.05	0 03	0.41	0.52	0.34	0.09	0.63	0 55	0.86	0.23	1.28	2.20	1.30	1.35	2.09	1.66	1.79	0.97	1 29	191	2 09	2 02	3.59	2.95	1.38	141	2 28	2 28	1.99	1 49	1 21	3 01	1.94	_change	a E	00 hrs.	
1.34	1.19	0.76	0 92	0.90	1.08	0 82	0.41	1.24	1.06	0.02	0.60	1.22	1.82	1.44	1.32	1.20	1.24	0.96	1.12	1.12	1.56	1.79	1 17	1 97	2.07	1.09	1 22	2.22	1.70	1.84	0 93	1 25	2 95	1 13	Delta b	Delta		
2.22	2.02	1.81	1.72	1.71	1.90	1.68	1.59	1.85	1.95	1.35	1.58	1.16	1 76	1.54	1.61	1.50	1.50	1.42	1.56	1 41	1 88	1.74	1.62	2.10	2.06	1.40	1.54	2.18	2.16	2.20	1.93	0 46	2.54	1 98	change	a b		

HS+	7001	088	087	086	085	084	083	082	081	080	079	078	077	076	075	074	073	072	071	070	069	068	067	055	054	053	052	051	050	049	048	047	046	045	044	Formula			
86.50	31.80	54.40	66.60	62.20	64.90	72.40	72.10	64.90	69.70	69.70	66,50	69.20	70.00	59.40	69.70	71.80	70.90	72.00	70.40	73.10	73.70	72.60	67.80	37.50	48.10	58.00	58.00	61.70	51.80	64.60	61.10	63.00	38.40	63.20	41.70	loitial	Glo		
69.80	13.30	35.50	40.40	37.30	40.30	33.10	32.40	30.20	33.80	33.20	33.60	33.30	34.60	37.50	35.30	35.70	33.40	39.80	34.40	40.50	43.70	42.90	39.00	27.00	30.60	40.40	42.40	44.90	30.10	45.00	42.50	48.80	25.60	46.90	23.80	at 500 hrs	Gloss (60 degree)		
-19.31	-58.18	-34.74	-39.34	-40.03	-37.90	-54.28	-55.06	-53.47	-51.51	-52.37	-49.47	-51.88	-50.57	-36.87	-49.35	-50.28	-52.89	-44.72	-51.14	-44.60	-40.71	-40.91	-42.48	-28.00	-36.38	-30.34	-26.90	-27.23	-41.89	-30.34	-30.44	-22.54	-33.33	-25.79	-42.93	%chang	ree)		
3.04	0.14	1.54	1.51	1.55	1.61	1.57	1.33	1.43	1.48	1.42	1.61	1.46	1.37	1.38	1.06	1.43	1.23	1.43	1.18	1.15	1.61	1.38	1.21	0.98	1.28	1.20	1.44	1.41	1.37	1.43	1.13	1.52	1.14	1.48	1.17	Initial			
4.02	0.45	0.87	0.66	1.08	0.92	2.02	1.67	1.81	1.46	1.64	1,48	1.70	1.76	1.56	1.00	1.16	0.95	0.86	1.22	1.23	1.33	1.78	86.0	3.18	2.50	2.79	2.83	2.00	2.28	2.24	2.28	1.85	2.33	1.87	2.51	at 500 hrs	Delta E	UV-500 ho	
0.98	0.31	0.67	0.85	0.47	0.69	0.45	0.34	0.38	0.02	0.22	0.13	0.24	0.39	0.18	0.06	0.27	0.28	0.57	0.04	0.08	0.28	0.40	0.23	2.20	1.22	1.59	1.39	0.59	0.91	0.81	1.15	0.33	1.19	0.39	1.34	change		ES.	<i>Ž</i> 2.T,
3.89	0.11	-1.12	-1.26	-1.24	-1.11	-0.70	-0.77	-0.95	-0.90	-0.82	-0.68	-0.82	-0.77	-0.82	-0.86	-0.83	-1.10	-1.04	-0.89	-0.81	-0.92	-0.56	-1.08	-0.75	-1.11	-0.87	-0.72	-1.09	-1.14	-1.25	-1.04	-1.15	-1.03	-1.15	-1.00	Initial			MBIENT
2.53	-0.41	0.36	0.19	0.43	0.34	1.00	0.90	0.92	0.78	0.76	0.99	0.90	0.93	0.94	0.57	0.67	0.35	0.39	0.65	0.71	0.63	0.98	0.45	1.58	1.05	1.35	1.35	0.85	0.80	0.72	1.02	0.81	1.04	0.80	1.21	at 500 hrs	Delta b		AMBIENT CURE
-1.36	-0.52	1.48	1.45	1.67	1.45	1.70	1.67	1.87	1.68	1.58	1.67	1.72	1.70	1.76	1.43	1.50	1.45	1.43	1.54	1.52	1.55	1.54	1.53	2.33	2.16	2.22	2.07	1.94	1.94	1.97	2.06	1.96	2.07	1.95	2.21	change			
82.90	11.20	36.50	40.70	37.10	45.30	32.70	26.20	29.10	32.10	32.00	31.60	30.10	30.80	43.50	36.80	29.40	34.30	33.50	32.40	30.10	42.70	36.10	26.40	25.70	29.10	39.40	43.50	45.00	28.70	42 00	40.80	49.30	25.20	43.40	20.10	1000 hour	Gloss (60		
-4.16	-64.78	-32.90	-38.89	-40.35	-30.20	-54.83	-63.66	-55.16	-53.95	-54.09	-52.48	-56.50	-56.00	-26.77	-47.20	-59.05	-51.62	-53.47	-53.98	-58.82	-42.06	-50.28	-61.06	-31.47	-39.50	-32.07	-25.00	-27.07	-44.59	-34.98	-33.22	-21.75	-34.38	-31.33	-51.80	% change	(60 degree)		
4.11	0.52	1 21	0.83	0.99	0.86	2.26	1.86	2.34	1.97	1.66	2.07	2.03	2.18	2.26	1.61	1.98	1.71	1.62	2.03	2.28	2.00	2.75	1.92	3.08	2.18	2.69	2.64	1.69	2 18	1.81	2.13	1.47	2 27	1 79	3 09	Delta E	Delt	QUV1000 hrs.	
1.07	0.38	0.33	0 68	0.56	0 75	0 69	0.53	0.91	0.49	0.24	0.46	0.57	0.81	0.88	0 55	0.55	0.48	0.19	0.85	1.13	0 39	1.37	0.71	2.10	0.90	1 49	1 20	0 28	0.81	0 38	1 00	0 05	1 13	0 31	1 92	change	аE	00 hrs.	
2.59	-0.10	-0.46	0.21	0.28	0.32	1.20	0 92	1.27	1.02	0.80	1.07	1.19	1.02	1.09	0 67	0.94	0.62	0.75	1.00	1.16	1 00	1.46	0.73	1.49	0.76	1.17	1.16	0.54	0.67	041	0 77	0.49	0 89	074	1 33	Delta b	Delta		
-1.30	-0.21	0 66	1 47	1.52	1.43	1 90	1.69	2.22	1.92	1.62	1.75	2.01	1.79	1.91	1.53	1.77	1.72	1.79	1.89	1.97	1 92	2.02	1.81	2.24	1 87	2.04	1.88	1 63	1.81	1.66	1 81	1.64	1 92	1 89	2 33	change	a b		

Table 7 (Cont.)
AMBIENT CURE

1	n/a	n/a		n/a	9.5		gelled	0.7		gelled	8	043
	n/a	n/a		n/a ·	9.44		gelled	0.86		gelled	85	042
	n/a	n/a		n/a	9.39		no sampi	1.79		no sampi	92	041
	n/a	n/a		n/a	9.4		gelled	0.54		gelled	86	040
	n/a	n/a		n/a	9.56		gelled	0.77		gelled	101	039
	n/a	n/a		n/a	9.55		gelled	1.38		gelled	86	038
	n/a	n/a		n/a	9.23		gelled	0.85		gelled	92	037
	n/a	n/a		n/a	9.33		no sampl	1.17		no sampi	88	036
	med	40	-5.72	8.9	9.44	-14.31	1.67	1.95	26.51	105	83	035
	n/a	n/a		n/a	9.44		gelled	1.13		gelled	90	034
	soft	10	-7.77	8.31	9.01	49.56	0.45	0.9	-17.44	71	86	033
	n/a	n/a		n/a	9.24		gelled	1.5	,	gelled	72	332
	n/a	n/a		n/a	9.57		geiled	1.37		gelled	93	031
	n/a	n/a		n/a	9.48		gelled	0.88		gelled	70	023
	n/a	n/a		n/a	9.65		gelled	0.78		gelled	80	022
	n/a	n/a		n/a	9.53		gelled	1.19		gelled	69	021
	n/a	n/a		n/a	9.64		gelled	2.34		gelled	78	020
	n/a	n/a		n/a	9.47		no sampi	1.28		no sampl	63	019
	n/a	n/a		n/a	1.697		gelled	0.68		gelled	58	018
	n/a	n/a		n/a	9.52		gelled	1.63		gelled	61	017
	n/a	n/a		n/a	9.38		gelled	1.12		gelled	68	016
	n/a	n/a		n/a	9.52		gelled	1.17		gelled	61	015
	n/a	e/u		n/a	9.56		no sampl	0.56		no sampi	88	014
	n/a	a/a		n/a	9.32		gelled	0.77		gelled	74	013
	n/a	n/a		n/a	9.45		gelled	0.66		gelled	69	012
ď	med-hard	20		n/a	9.14	-94.87	0.48	9.42	2.41	85	83	011
ď	med-hard	30	-7.26	8.43	9.09	-20.33	0.39	0.492	15.29	98	85	010
	n/a	n/a		n/a	9.42		gelled	1.11		gelled	68	900
	n/a	n/a		n/a	9.32		gelled	1.88		geiled	95	800
	n/a	n/a		n/a	9.48		gelled	1.88		gelled	91	007
	n/a	n/a		n/a	8.8		gelled	1.83		gelled	108	006
	n/a	n/a		n/a	9.61		no sampl	0.69		no sampl	136	ე05
	n/a	n/a		e/u	9.65		gelled	1.88		gelled	79	004
	n/a	n/a		n/a	9.43		gelled	1.16		gelled	94	003
		n/a		n/a	9.59		gelled	1.18		gelled	140	002
		n/a	,	n/a	9.58		gelled	1.6		gelled	96	001
	settling type	settling amount	% change	final pH	initial pH	% change	final ICI	initial ICI	% change	final KU	initial KU	Formula
			ð	eks at 120	Viscosity, settling, and pH Stability (4 weeks at 120F)	d pH Stab	ettling, ar	scosity, s	<u>≤</u>			
_											+	

Table 7 (Cont.)
AMBIENT CURE

												HS+
			alling away	% settling is the relative ht on stirring stick that adheres w/o easily falling away	at adheres	ring stick th	e ht on stir	the relativ	% settling i:			700T
	n/a	n/a		n/a	9.18		gelled	0.95		gelled	90	088
	soft	80	-7.38	8.66	9.35	116.41	1.69	0.78	27.71	106	83	087
	medium	20	-7.50	8.63	9.33	3.62	1.09	1.05	22.22	88	72	086
	n/a	n/a		n/a	9.01		gelled	0.84		gelled	87	085
	soft	90	-5.62	9.23	9.78	-4.32	0.71	0.74	26.51	105	83	084
	medium	90	-6.01	9.23	9.82	-40.55	0.65	1.1	21.98	111	91	083
	soft	10	-4 .55 .	9.23	9.67	14.51	0.81	0.71	3.61	86	83	082
	medium	35	-4.59	9.35	9.8	-13.49	0.92	1.06	46.81	138	94	081
	soft	40	-5.52	9.24	9.78	2.89	1.00	0.97	3.53	88	85	080
	n/a	none	-4.44	9.48	9.92	-33.36	0.73	1.1	36.36	105	77	079
	soft	80	-5.15	9.39	9.9	21.11	0.76	0.63	20.21	113	94	078
-	med-hard		-5.25	9.38	9.9	60.00	1.10	0.69	18.75	114	96	077
	n/a	none	-5.79	9.11	9.67	-60.36	0.33	0.84	-9.52	76	84	076
	soft	80	-6.17	9,13	9.73	-11.50	0.71	8.0	18.89	107	90	075
	soft	80	-5.75	9.34	9.91	-15.18	0.72	0.85	46.67	132	90	074
	medium	80	-3.91	9.35	9.73	53.41	0.63	0.41	18.89	107	90	073
	soft	slight	-5.61	9.25	9.8	5.77	0.55	0.52	-3.13	93	96	072
	soft	30	-5.64	9.21	9.76	-44.06	0.87	1.55	-4.71	81	85	071
	medium	60	-6.05	9.16	9.75	83.84	1.34	0.73	15.58	89	77	070
	medium	90	-3.91	9.33	9.71	85.49	0.95	0.51	21.43	119	98	069
	medium	70	-5.88	9.13	9.7	62.55	0.83	0.51	11.49	97	87	068
	medium	80	-5.71	9.25	9.81	-10.82	0.76	0.85	37.08	122	89	067
	n/a	n/a		n/a	9.32		gelled	1.74		gelled	87	055
	n/a	n/a		n/a	9.72		gelied	1.48		gelled	58	054
	n/a	n/a		n/a	9.65		gelled	1.34		gelled	78	ე53
	n/a	n/a		n/a	9.65		gelled	1.62		gelled	138	052
	n/a	n/a		n/a	9.43		gelled	2.88		gelled	64	051
	n/a	a/u		n/a	9.4		gelled	0.63		gelled	68	050
	n/a	e/u		n/a	9.07		gelled	1.66		gelled	86	049
	n/a	n/a		n/a	9.53		gelled	1.34		gelled	80	048
	n/a	n/a		n/a	9.37		no sampi	0.7		no sampi	84	047
	n/a	n/a		n/a	9.22		gelled	1.11		gelled	73	.046
	n/a	n/a		n/a	9.3	, ·	gelled	1.16	•	gelled	75	045
	n/a	n/a		n/a	9.49		gelled	1.35	ì	gelled	85	044
	settling type	settling	% change	final pH	initiai pH	% change	final ICI	initial ICI	% change	final KU	initial KU	Formula
			Ť	Viscosity, settling, and pH Stability (4 weeks at 120F)	tility (4 we	nd pH Stat	ettling, ar	scosity, s	≤			
			-									

Table 8 INDUSTRIAL MAINTENANCE

	•			1	_	_																																					
047	046	045	044	043	042	041	040	ACO	038	236	037	036	035	034	033	032	031	023	022	120	020	610	018	017	016	015	014	013	012	011	010	900	800	007	006	005	004	003	002	001	Eormula		
3	ω	u	з	ω	3	2	2		, ~	,	٦ ،	٥	2	2	2	2	2	4	4	4	4	4		4	4	*	4	4	4	4	4	4	4	4	3	3	3	သ	3	3	Resin		-
7	8	5	1	1	-	7	7	2	11	0		. اد	1	-	4	အ	2	ü	11	3	11	7	2	-	5	_	11	8	3	ō	10	3	5	1	.3	11	2	7	8	2	Dispersant		
2	2	2	2	2	2	-	-1	_	-		-		.	-	Ŋ	2	2	1	-	-	-	-		1	-1		2	2	N	N	2	2	2	2	1	. 1	- -			-	Amount	-	
1	3	8	7	1 1	4.	6	8	8	2	4	4		, ,	. 7 1	8	. 6	1, 1	7 . !	2	6	4	1	4	8	3	2	8	7	7	2	2 !	. 3	О Т	7	7	7	. 6	- 5	Ċ,	3'	Thickener		-
1.94	2.09	2.36	2.34	2.34	3.01	2.49	2.32	2.81	2.43	2.54	2.51	14.7	2 47	249	2.09	1.93	2.38	2.51	2.60	2.71	2.65	2.70	2.51	2.63	2.76	2.55	2.49	2.58	2.43	2.30	2.28	2.34	2.80	2.72	2.60	2.36	2.75	2.37	2.69	2.61	Ellm. Thickness		
25.0	6.9	26.6	9.7	18.9	25.7	23.8	27.4	21.7	33.0	15.1	16.6	13.4	15.7	25.4	12.5	31.0	21.5	36.9	30.8	34.2	33.5	14.3	33.7	21.2	36.0	28.9	29.6	11.7	20.1	8.0	13.9	30.8	35.9	34.7	17.2	25.6	4.6	28.8	23.6	6.6	20 Gloss		
61.4	31.5	62.4	39.9	54.4	61.0	59.4	62.5	58.5	67.3	49.1	51.2	49.5	20.2	80.5	44.7	66.9	56.1	68.1	66.3	69.0	67.2	48.0	66.8	57.2	67.5	63.7	65.4	44.4	57.9	37.9	49.8	65.5	68.3	67.9	52.7	61.6	25.7	63.8	8.65	31.2	60 Gloss		
1.5	1.5	-	-1	-	-	1.5	1.5	1.5	1.5	-	1.5	ō		7, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1,	15	1.5	1.5	3	ω	3	- 4	1.5	1,5	1.5	3	1:5	*		1.5	4	3	3	4	1,5	-	-	-	á	-	 -	Toluene	-	
ယ	ω	3	ω	3	3	3	3	3	3,	2	्र अ	4	4	· # .	3.5	3.5	4	1.5	4	3	. S	. 4	် ယ •	15. 4.5 .	3	4.5	ü	3	4.5	4	ယ	4	A	4.5	3	3	4	ω	ပ	3	Ethanol		
1.5	1.5		1.5	-	1.5	1.6	_	1.6	1.5	-		1.5	1.0		7	5	1.5	3	2	1.5	1.5	-	1.5	2	N	N	1.5	•	1.5	1.5	1.5	-3	1.5	1.5	1.5	1.5	1.5	1.5		1	MEK	Chemical Resistance	
5	S1	4	5	5	5	5	5	0	6	4	5	0		7	,	5	5	5	5	4.5	4.5	4	4.5	51	3	8	61	4	4.5	51	3	3	4	57	4.5	5	61	5	0	O.	10% Sulf	Resistar	
2	з	2	2	2	2	2	2	2	2	2	2 .	3	3	3 4	4		u	u	ω	4	4	u	2	4.5	3	1.5	3	3	4	4	3	ω	ω i	2	S	2	3	2	2	3	10% Sulf 10% NaOH	C	
2.5	5	4.5	5	2	5	2	2	2	2.5	5	2	2	2	,	,	3	ת	3	3	3	ω	3	3	3	3	3	3	3	3	5	3	3	3	3	4.5	3	5	4	4	_	Di. Water		
-	-		1	1	0	0	0	0	0	0	0	0	o				٥	0	0	0	0	0	0	0	0	0	0	0	0	-	-	0	0 0	0	-	<u>.</u>	_		0	-	Pencil. hardness		

		Sher-cryl	Centurion	Polylon 1900	088	087	086	085	084	083	082	081	080	079	078	077	076	075	074	073	072	071	070	069	890	067	055	054	053	052	051	050	049	048	Eormula		
					2	2	. 2	2	-3	_	_		-	-	_	1	1	1	1	1	1	. 1	1	1.	1	- 1	သ	2	3	3	. 3	3	3	3	Resin		
				4 "	8	(J)	5	1	3	9	10	7.7	3	2	9	8	6	5	. 2	. 7	11.	3	3	8	: 1	5	8	. 8	8	9	5	3	8	11	Dispersant		
		Control #3	Control #2	Control #1	2	2	2	2	1	. 1	1	1	1	1	1	1	. 1	1	2	2	2	2	2	2	. 2	2	2	. 1	-	1	1	2	2	2	Dispersant Amount	-	
-				N N	4 1	7	7 1	3 4	} 6∦§	5	1 11 .	3	8	1	. 4	51	1 1	2,	5.	6	5	2	2	2	6	·	4	٨	2		. 4	5	6	3	Thickener		
		1.97	3.66	3.30	2.43	2.52	2.34	1.95	3.24	2.88	2.95	2.94	2.55	2.87	2.25	2.40	2.49	2.44	2.57	2.19	2.09	2.24	2.38	2.38	2.28	2.40	2.79	2.47	2.47	2.54	2.56	2.20	2.02	2.15	Elim. Thickness		
		46.3	72.8	83.3	17.5	30.9	24.7	27.0	38.0	36.2	28.8	34.5	33.8	28.2	30.4	31.9	24.3	32.2	33.7	32.2	35.9	32.0	36.1	38.6	37.0	29.1	8.9	14.9	21.7	22.6	26.3	15.4	24.9	23.6	20 Gloss		
		78.0	88.8	94.4	52.7	65.5	60.4	63.5	69.7	69.4	61.7	66.6	67.5	63.9	66.7	67.4	59.7	67.7	68.2	67.4	69.2	. 67.3	69.4	71.5	70.9	65.5	37.3	49.1	57.3	57.7	63.0	50.3	63.6	59.8	60 Gloss		
		1	1.5	1.5	1.5	1.5		1.5	1.5	1,5	1.5	1.5	2	1.5	1.5	1.5	1.5	1.5	1.6	1.5	1.5	1.5	1,5	1,5	1.5	1.5	1		_	٨	-1		1.5	-	Toluene		
		3	1.5	71.5	9'k	3.5	3	3	2	4	O)	idi.	3	4	4	4	4	Cti	S.	3.5	9 ∰ N ,	2 O 1	သ	. 3	4	4	3	3	ပ	1	3.5	3	4	3	Ethanol		
		1.5	1.5	1.5	1,5	1.5	, j. 1	1.5		1.5	1.5	 N	-	1.5	1,5	1.5	1.6	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	1.5	- -		-	-	_	1.6	1.5	1.5	MEK 2	Chemical Resistance	
	ŀ	5	6	4	, ; ;	4.5	6	G	3	ເນ	1.4	3	4	4	4.5	4	4	4.5	4	ω	.4	ယ	* 4	. 3	4	3	4.5	4.5	O.	5	5	5	5	5	10% Suff	Resistar	- ,
		3	5	· 4.5	N	2	2	· · · 2	2	2	 4	3	. 2	2	2	2	2	3	2	2	3	2	2	2	ω	2	ω	2.5	2	2	2	2	4	2	10% Sulf 10% NaOH	100	
		4	5	4.5	5	2	2	2	2	2	5	4	2	3	•	4.5	4	4	3	4	3	2	4	3	3	3	4.5	2	2	2	3	4.5	4	3	Di. Water		
		0	4	5	0	0	0	0	0	0	0	0	0	0	٥	0	0	0	0	0	0	0	0	0	0	0	_	-1	_		0		2		Pencil. hardness		

	<u>''</u>	Π	Π	~			Т	Т	T	Т	Τ	Т	Т	Τ	Τ	Т	Т	Т	Τ	Г	Γ	Т	Τ	Т	Τ	Π		Г	Г	Г	Г				Г	Г	Г		Γ		Т	Т
047	046	045	044	043	042	2	040	039	038	037	036	035	034	933	032	 2	023	022	021	020	019	018	017	016	015	014	013	012	011	010	900	800	007	006	205	204	003	002	261	Eormula		
8	6	8	. 6	6	4	6	4	4	4		4		4	6	6	4	2	4	4	4	2	4	4	4	4	4	2	6	4	8	6	6	6	8	&	4	8	6	4	Blister size		
2	2	2	2	2	2	2	. 2	. 2	3	3	2	2	2	2	3	1	1	1	2	2	1	1	1	2	1	1	2	2	3	1	2	2	2	. 3	3	2	2	ဒ	2	density	Blictor	
8	9	6	10	9	8	7	9	7	9	8	7	O	4	S	9	5	8	N	4	8	8	8	. 9	6	8	-	10	4	5	-	6	9	. 1	9	8	7 *	9	10	9	Rust	Humidity	
43.3	22.5	40.1	28.0	32.1	37.0	33.0	25.2	28.3	36.4	23.8	30.3	24.0	33.5	31.0	43.5	31.0	8.4	20,7	23.9	16,8	.7.8	10.5	10,0	36,3	18,2	9.0	11.7	25.6	16.9	19.6	26.0	20.5	26.5	41.6	, 47.9	15.4	46,3	40.2	19.9	Gloss	-	
-29.48%	-28.57%	-35.74%	-29.82%	-40.99%	-39.34%	-44.44%	-59.68%	-51.62%	45.91%	-51.53%	40.82%	-51.32%	-44.35%	-30.65%	-34.98%	-44.74%	-87.67%	-68.78%	-65.36%	-75.00%	-83.75%	-84.28%	-82.52%	-46.22%	-71.43%	-86.24%	-73.65%	-55.79%	-55.41%	-60.64%	-60.31%	-69.99%	-60.97%	-21.06%	-22.24%	-40.08%	-27.43%	-32.78%	-36.22%	gloss	8 2	
2	2	2	2	2	N	2	2	2	2	2	2	2	2	2	2	2	6	6	6	6	6	6	6	6	2	6	8	6	6	6	6	6	6	2	2	2	2	2	2	Size		
2	2	2	2	2	2	2	2	2	_	2	2	2	2	2	2	2	4	4	4	4	4	4	4	4	4	3	4	4	4	4	4	4	S	3	2	2	2	2	2	density	75	
8	9	9	8	9	8	8	7	10	7	8	7	6	8	8	6	8	9	9	8	8	8	8	8	8	9	7	٥	8	8	8	ö	5	8	8	8	9	6	9	ō	Rust	(200 hours)	
8	8	8	ė	8	8	8	8	8	8	8	မ	9	9	9	9	8	8	8	8	8	8	8	ھ	8	7	7	8	8	8	8	®	8	۵	8	8	8	8	8	8	Scribe	urs)	
2	2	2	2	2	2	2	2	2	2	2	2	2	2	2 ·	2	2	6	6	4	4	4	2	4	4	4	4	4	2	4	4	6	4	2	2	2	2	2	2	2	Size	60	
-		-	_	_		4	1	-1	. 1	2	1	1	1		_	2	ω	2	3	သ	3	3	3	3	3	ω	3	3	3	3	3	3	3	2	-	1	1	-	-3	density	alt Spray	
7	7	8	8	8	7	7	S.	.7	6	7	6	. 4	7	O1	6	7	9	9	7	8	9	8	8	8	9	8	6	8	8	8	9	9	7	8	8	8	7	8	. 9	Bust	(375 hours)	
7	7	7	6	6	7	7	7	7 .	7	7	. 6	8	8	7	7	7	7	7	7	7	6	7	6	8	7	7	5	7	6	7	8	8	8	8	7	7	7	7	7	Scribe	s	
36	36	6	36	40	96	24	28	40	28	24	28	24	28	28	36	24		× 168	> 168	× 168		> 168	× 168	> 168	> 168			> 168	> 168		> 168	> 168	> 168	6	44	6	36	44	40	Impact		
4	4	8	4	4	5	^^	4	4	4	^4	^4	44	4	^4	4		> 168			> 168	> 168			> 168	> 168				> 168				> 168	4	8	4	4	4	4	Reverse		

Table 8 (Cont.)

_		1		_					,	,	_	_	_		,		,		,	_	_		_	_	_	_		_	_	_			_					
		Sher-cryl	Centurion	Polylon 1900	088	087	086	085	084	083	382	081	080	079	078	077	076	075	074	073	072	071	070	069	068	067	055	054	053	052	051	050	049	048	Formula			
		8	4	2	6	6	4	4	4		4	4	•	4	4	4	6	4	4	6	6	6	8	4	· 6	. 6	4	. 8	. 8	8	8	8	8	8	Blister size	ang ng Later Mehalin	1.00	
		2	. 2	. 3	2	2	2	2	2	Ν	N	. 2	, 2	2	, 2	2	. 2	2	. 2	1	1 2	2	1	2	2	2	3	3	1 3	3	3	. 3	. 2	1 3		Blister	a,	
		9	10	10	9	. 9	9	9	10	10	9	10	9	9	9	10	10	.10	9	. 9	9	9	9	9	10	. 9	9	10	10	8	9	10	9	9	Rust		, Humidity	14
*	- 1	30.2	31.2	90.5	26.3	22.6	23.0	17.9	16,5	22.1	26,4	22,4	19,9	22/8	22 7	13.6	30.9	19.6	29,7	20.6	26.8	27.8	32.6	18.7	28.8	21.2	28.5	35.3	46.3	46.5	· 48.2	32.6	33.2	42.2	Gloss	The same of the same	1 1 1	-
		-61.28%	-64.86%	-4.13%	-50.09%	-65.50%	-61.92%	-71.81%	-76.33%	-68.16%	-57.21%	-66.37%	-70.52%	-64.32%	-65.97%	-79.82%	-48.24%	-71.05%	-56,45%	-69.44%	-61.27%	-58.69%	-53.03%	-73.85%	-59.38%	-67.63%	-23.59%	-28.11%	-19.20%	-19.41%	-23.49%	-35.19%	-47.80%	-29.43%	gloss	% Change	1 8 1	
		10	10	10	2	2	2	2	2	2	2	2	2	2	2	2	10	2	2	2	2	2	2	2	2	2	2	2	2	2	2	2	2	2	size	Blister	Sa	
		თ	Ŋ	5	2	2	2	1	2	2	3	3	3	3	3	4	5	2	2	1	3	2	ပ	3	3	3	2	သ	2	2	2	2	2	2	density	Blister	Salt Spray	
		9	9	10	6	6	8	8	9	8	9	9	9	9	10	10	10	9	9	10	9	10.	9	9	ō	9	7	7	5	7	9	6	5	7	Rust		(200 hours	
		8	8	9	8	8	9	9	8	8	8 .	8	8	8	8	8	7	8	8	8	7	8	8	8	8	8	8	8	8	æ	8	හ	8	8	Scribe	1	urs)	
		10	10	10	2	2	2	. 2 .	2	2	2.	2	N	2	4		2	2	·	2	2	2	4	2	2	•	2	2	2	2	2	2	. 2.	2	Sizo	Blister	S	,
		ij.	5	6	1	1	2	. 2	2	2		3	Ċ,	2	3	7. : 2	. lun 4	2	. 2	2,	, 2	2	2	2	ω	2	-	: 3	. 2		2	-	-		density		Salt Spray (-
-		7	9	10	6	6	7	8	9	9	. 8	8	80	8	8	9	9	8	8	9	8	9	8	8	8	8	7	9	8	7	8	6	ڻ ن	5	Rust		(375 hours	
		7	8	သ	7	. 7	9	9	8	9	8	7	8	7	7	8	8	8	&	8	æ	æ	8	æ	8	7	7	7	8	8	6	7	7	7	Scribe		8)	
		> 168	> 168	36	40	28	32	28	2	52	8	4	56	36	56	52	44	2	44	2	48	40	52	56	44	44	28	32	36	32	48	48	60	40	Impact	Forward		
		> 168	> 168	4	4	^4	4	â	24	8	8	4	6	8	8	8	4	6	4	12	4	12	12	8	4	8	4	4	4	4	4	4	16	4	Impact	Reverse		

SSAG		90	4	30	-	در:		··	-	2	Ş
PASS	4	9	4	6	0	4	7	10	9	5	40
PASS	ယ	9	3	4	0	c	۵	ē	1 0		266
PASS	4	ī	3	0		3	•	5 6	2 0	10	240
PASS		9	2			,	8	5	5	10	044
1			3	B	0	4	8	6	5	10	043
PASS	4	9	3	4	0	4	8	10	C)	10	042
PASS	ယ	9	2	6	0	4	5	10	5	10	241
PASS	ယ	9	3	6	0	ഗ	8	10	o		Ç
PASS	4	· 10	1	4	0	4	α	ē	0	3	
PASS	သ	6	2	6	1	U	٥	ā			030
PASS	ŭ	5	0	0			0	5 3	, , , , , , , , , ,	10	038
77.00	,	5 6	3		4	3	9	10	5	10	037
PAS	4	6	3	1	2	ა	6	10	5	10	036
PASS	3	10		0		ΟI	8	10	On .	10	035
PASS	4	10	2	4, ,4	သ	S ₁	9	10	5	10	034
PASS	သ	8	2	Ø	3	ഗ	9	10	o	5	033
PASS	4	9	2	0	Ą	5	,	5		5	
PASS	3	10	•	60	4	5	,	10	, 0	3 6	23
PASS	1	10	O	10	2	Ü				5	034
PASS	c	5	0	5	,				ת	5	023
FASS	•	5	n	5	. اد	٦.	7	10	S)	ő	022
DAG		0	ام	20	4	4	7	10	ຍາ	- 6	021
PASS	2	9	O1	10	ယ	5	7		ဟ	10	020
PASS	2	ő	3	8	3	5	œ	10	5	ð	910
PASS	5	9	4	О	3	5	9	10	O	10	018
PASS	5	10	•		ω	5	ø	10	0	10	017
PASS		10	•	œ	. 2	O n	9	9	0	5	0
PASS	ري ن	10	ఆ	8	u	5	æ	100	0	3 5	
PASS	5	10	2	œ	2	Ö	0		n	5 6	016
PASS	2	5	0	5				5 6	7	10	014
PASS			n	50	٠ .	7	9	6	5	10	013
0000	, ,	0	3	20 (-	5	8	6	6	10	012
DAG		10	A	6	0	5	9	10	S	.10	011
PASS	רכ	9	3	6	2	5	8	9	4 '	6	010
PASS	1	8	5		ယ	5	8	10	5	10	009
PASS		9	6	10	3	5	7	10	5	10	008
PASS	51	10	Oi .	10	3	5	8	10	5	10	007
PASS	4	10	Ot.	10	-1	4	9	10	5	10	006
PASS	4	9			0	3	6	10	5	10	005
PASS	.51	10	5	10	2	Сh	8	10	o	10	Ş
PASS	4	9	10.00	CO 11.55	3	4	8	10	o	10	903
PASS	4		17. 18. 18. 18. 18. 18. 18. 18. 18. 18. 18	(3°% 6 % %)	4	4	8	10	5	10	3 8
\dashv	4	. 10	O	题 10 A	3	4	8	10	5	10	8
n Mandrel bend	Adhesion	Rust	Blister density	Blister	galvanized	aluminum	Scribe	1.	Alistran larging	DISTO SIZE	Comming
	·	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	, j	17 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	Weathered HD.	Weathered				1 -	
		Ir Soak	24 Hr. Water Soak		ion	Monagion	Cide	Take Rivers			
			A			7 1700	200	rharing (4 cv	Corrosion Weathering (4 cycles)		

Table 8 (Cont.)

	Sher-cryl	Centurion	Polylon 1900	088	087	086	085	084	083	082	081	080	979	078	077	076	075	074	073	072	071	070	069	068	067	055	054	053	052	051	050	049	048	Eormula		
	8	ō	10	10	10	ō	ō	ő	10	10	10	ō	10	10	10	10	10	10	1 '	10	10	10	10	10	10	10	10	10	10	10	10	10 %	10	Blister size		1
	4	5	۲)	σ,	5	5	5	ch	5	5	6	5	- О	O.	Ċħ.	O .	5		o,	On .	5	5	5	.* Or	·	6 3 3 3	5	, 5	5	5	СÒ	6°; 6 # 15;	5	Blister density	orrosion	
,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	9	10	ő	10	ō	10	10	10	10	10	10	10	10	10	10	10	10	10	10:4:4	. 10	10	10	10.	9	10	8	10	10	10	10	10	10	10	Rust	mering (4 cyc	
	6	7	5	9	g	εó	7	8	. 8	8	8	8	8	of 7	8	8	8	. 8		8	7	8 .	9	. 8	. 8	· 7	. 7	9	9	8	7	. 8	6	Scribe	*	
	4	ა		5	5	4	4	4	4	4	4	4	4	4	သ	4	4	4	4	4	4	4	4	4	4	4	-	4		4	2	4	4	aluminum	Adhesion	
	2	0	2	သ	3	3	4	, 3	2	3	သ	2	3	-	0	0	2	_	N	1	2 .	2	2	_	-	4	3	0	0	0	0	-1	1	galvanized	ion	
	. 10	10		Charles & Land	18 18 4 s	्रम् (क्रिकेस्टर्ड 🍂 ्राष्ट्री 💽	a, bit and the	后身横城 600 G 70 1	0	6, 6, 6, i	10 Per 10	85 10 800 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1		•					Sup. Car. 6 25 12 2	The state of the s	43 1 € 1 6	6	6 (d. 6)	1	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	10	4	*** 8	ا مارسیال	0	•	1,71,82 M OD	.10	Blister size	The state of the s	
	5	ტ	Ö	2	1	.2	Conflict Transfer	3		-1	ν.	N	2	3	N		3		- 1	<u>_</u> -	W.	3	2	2	3	5	4	4	. 5	ů.	•	***	Ö	Blister density	24 Hr. Wa	
	9	10	10	10	10	10	10	10	. 8	6	8	9	9	10	1	- 1		9	6	10	10	- 1	10	10		9	10	10	10	8	10	8	9	Zwat	er Soak	
	0	2	0	ω	2	ယ	ယ	3	0	0	0	0	ω	4	2	4	0	٥	2	0	ω	ယ	ω	6	ယ	4	•	5	4	4	ယ	ຜ	4	Adhesion		
	FAIL	PASS	FAIL	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	PASS	Mandrel bend		

047	046	045	044	043	042	2.	040	039	038	03/	3 8	036	235	033	032	8 2	023	022	021	020	019	018	017	016	015	014	013	012	011	010	009	800	007	006	005	004	003	002	8	Formula		
				L	L	L	L	╀	╀	+	1	+	╀	╀	-	╀	-	ŀ	_	-	H	\vdash	H	\vdash	┞	-		-			Н										<u> </u>	
63.00	38.40	63.20	41.70	55.20	60.70	60.50	63.20	80.00	8.80	3 2		23.00	200	27.10	68.70	57.70	71.80	67.80	70.70	68.70	49.20	69.00	59.30	70.70	8.16 16	69.10	46.80	59.30 ·	40.60	52.00	68.30	70.30	69.40	51.00	61,00	49.60	65.70	56.50	32.60	litia		
48.80	25.60	46.90	23.80	36.20	40.50	43.40	47.60	48.30	57.30	41.70	20.50	3 8	3 2	29.00	47.10	37.50	22.10	21.70	22.00	21.10	12.90	19.00	14.50	19.70	18.20	19.60	15.00	16.50	10.40	13.80	21,90	30.50	33.30	35:80	47.00	29.80	50,70	40.10	21.10	at 500 hrs	Gioss (60 degree	
-22.54	-33.33	-25.79	-42.93	-34.42	-33.28	-28.26	-24.68	-19.50	-14.22	-19.50	CC.+2.	31.43	60:72	-38.43	-31.44	-35.01	-69.22	-67.99	-88.88	-69.29	-73.78	-72.46	-75.55 ·	-72 14	-72.47	-71.64	-67.95	-72.18	-74.38	-73.46	-67.94	-56.61	-52.02	-29.80	-22,85	-39.92	-22.83	-29.03	-35.28	%change	100	
1.52	1.14	1.48	1.17	1.36	1.29	1.63	1.49	1.86	1.48	1.78	87.1	1.42	1.88	1.38	1,61	1,65	1.31	1.31	1.57	1.37	0,45	0.82	0,61	1.39	1.00	1.10	1.31	0,73	0.26	1.05	1.06	1,17	1,81	1.34	2.05	1.17	1.81	2.69	0.94	niti a	-	
1.85	2.33	1.87	2.51	2.38	1.82	1.49	1.37	1.61	1.36	2.45	1.10	0.73	1.79	2.19	0.77	1.38	1.87	2.79	2.34	2.09	2.25	2.01	1.80	1.88	2.01	2.45	2.83	1.95	3.03	3.14	1.98	1.41	2.49	3.16	3.44	2.66	2.72	5.10	3.23	at 500 hrs	Delta E	QUV-500 hours
0.33	1.19	0.39	1.34	1.02	0.53	0.14	0.12	0.25	0.04	0.67	0.11	0.89	0.09	0.81	0.84	0.27	0.56	1.48	0.77	0.72	1.80	1.09	1.19	0.49	1.01	1.35	1.52	1.22	2.77	2.09	0.92	0.24	0.88	1.82	1.39	1.49	0.91	2.41	2.29	change		BIN
1 15	1.03	-1.15	1.00	-0,88	-0.95	-0.83	-1.05	-0,80	-0.81	-0.82	-0.88	-1.18	-0.61	-0.89	-1.33	-0.98	90.0	. 90.0	-0.10	-0.29	-0.30	-0.26	-0,46	-0,44	-0.29	-0.32	0.05	-0.45	-013	0.01	-0.31	-0.32	0 2	-b.46	-0.36	-1.00	0.79	0.41	-0.85			
0.81	1.04	0.80	1.21	1.20	0,89	0.81	0.71	0.82	0.65	1.40	66.0	0,21	0.86	1.24	0.15	0.65	0.95	1.63	1.24	1.17	1.16	1,10	0.86	0.94	1.03	1.38	1.60	0.95	1.76	1.83	1.86	0.83	1.43	1.76	1.92	1.36	1.42	2.79	1.55	at 500 hrs.	Delta b	
8	2.07	1.95	2.21	2.08	1.84	1.64	1.76	1.62	1.46	2.22	1.45	1.39	1.47	2.13	1.48	1,63	0.89	1.57	1.34	1.46	1,46	1.36	1.32	. 7			1.55	1.40	1.88	1.82	1.37	1.16	1 39	222	2.28	2.36	0.63	2.38	2.40	change		
4930	25.20	43.40	20.10	31.80	40.00	44.80	49.40	50.70	58.70	43.60	39.20	36.70	47.80	26.10	54.90	35.90	23.20	16.00	14.90	16.40	10.40	15.90	12.30	18.10	15.50	15.90	12.30	12.70	7.50	9.80	15.20	21.20	21.90	32.80	45.60	26.50	48.20	37.10	17.90	1000 hour	Gloss (60 degree)	
31 75	34 38	-31.33	-51.80	-42.39	34.10	-25.95	-21.84	-15.50	-12.13	-15.83	-26.04	-30.10	-21.51	-44.59	-20.09	-37.78	-67.69	-76.40	-78.93	-76.13	-78.86	-76.96	-79.26	-74.40	-76.55	-76.99	-73.72	-78.58	-81.53	-81.15	-77.75	69.84	-68 44	-35.69	-25.25	46.57	-26.64	-34.34	-45.09	%_change	degree)	
1 47	227	1.79	3.09	2.67	2.09	2.12	1.54	1.89	1.81	2.30	1.63	1.33	2.51	1.93	0.75	1.42	2.59	3.51	2.87	2.72	2.54	2.58	2.40	2.36	2.29	3.01	3.40	2.75	3.85	4.00	2.44	2 58	4 09	3 62	4.04	2.66	3.02	5.70	2.88	Delta E	Delta E	QUV-1
200	1 13	0.31	1.92	1.31	0.80	0.49	0.05	0.03	0.41	0.52	0.34	0.09	0.63	0.55	0.86	0.23	1.28	2.20	1.30	1.35	2.09	1.66	1.79	0.97	1.29	1.91	2.09	202	3.59	2.95	1 38	141	228	228	1.99	1.49	1.21	3.01	1.94	change	E	QUV-1000 hrs.
0 0	0 80	0.74	1.33	1.34	0.90	1.19	0.76	0.92	0.90	1.08	0.82	0.41	1.24	1.06	0.02	0.60	1.22	1.82	1.44	1.32	1.20	1.24	0.96	1.12	1.12	1.56	1.79	117	1.97	2.07	120	1 23	2 22	1 70	1.84	0.93	1.25	2.95	1.13	Delta b	Delta	
1 24	3 8	1 80	2.33	222	1.85	2.02	1.8	1.72	1.71	1.90	1.68	1.59	1.85	1.95	1.35	1.58	1.16	1.76	- 54	1.61	1.50	1.50	1.42	1.56	1.41	1.88	1.74	183	210	208	1 40	1 5 6	2 10	2 16	2 20	1 93	0.46	2 54	1.98	change	ਸ਼ 5	

HS+	700T	Sher-cryl	Centurion	Polylon 1900	088	087	086	085	084	083	082	081	080	079	078	077	076	075	074	073	072	071	070	900	890	067	055	054	053	052	051	.050	,049	048	Formula			
86.50	31.80	80.60	56.20	94.50	54.40	66.60	62.20	64.90	72.40	72.10	64.90	69.70	69.70	, 66.50	69.20	70.00	59.40	69.70	71.80	70.90	72.00	70.40	73.10	73.70	72.60	67.80	37.50	48.10	58.00	58.00	61.70	51.80	64.60	61.10	Initial	1000年	· · · · · · · · · · · · · · · · · · ·	Ţ
69.80	13.30	72.30	17.70	94.50	35.50	40.40	37.30	40.30	33.10	32.40	30.20	33.80	33.20	33.60	33.30	34.60	37.50	35.30	35.70	33.40	39.80	34,40	40.50	43.70	42.90	39.00	27.00	30.60	40:40	42,40	44.90	30.10	45.00	42.50	at 500 hrs		ss (60 degree)	
-19.31	-58.18	-10.30	-68.51	0.00	-34.74	-39.34	-40.03	-37,90	-54.28	-55,06	-53.47	-51.51	-52.37	-49,47	-51.88	-50.57	-36.67	49.35	-50.28	-52.89	44.72	-51,14	-44,60	-40.71	-40.91	-42.48	-28.00	-36.38	-30.34	-26.90	-27.23	-41.89	-30.34	-30.44	%change	三元を変え	Tee	-
3.04	0.14	5.76	10.09	4.40	1.54	1.51	1.55	1.61	1.57	1.33	1.43	1,48	1.42	1.61	1.46	1,37	1.38	1,06	1.43	1.23	1:43	1,18.	1.15	1.61	1.38		. 86'0	1.28	1.20	1.44	1.41	1.37	1.43	1.13	initial	· · · · · · · · · · · · · · · · · · ·	70.7	0
4.02	0.45	6.25	11.42	4.80	0.87	0.66	1.08	0.92	2.02	1.67	1.81	1.46	1,64	1.48	1.70	1.76	1.56	1.00	1.16	0.85	0.86	1.22	1.23	1.33	1.78	0.98	3.18	2.60	2.79	2.83	2.00	2.28	2.24	2.28	at 500 hrs	B. On March	Delta E	QUV-500 hours
0.98	0.31	0.49	1.33	0.40	0.67	0.85	0.47	0.69	0.45	0.34	0.38	0.02	0.22	0.13	0.24	0.39	0,18	0.06	0.27	0.28	0.57	0.04	0.08	0.28	0.40	0.23	2.20	1,22	1.59	1.39	0.59	0.91	0.81	1.15	_change	ele in the control of		- 1
3.89	0.11	2.43	0.81	0.14	-1.12	-1.26	. 4.24	-1.11	-0,70	0.77	-0.95	-0.80	-0.82	-0.68	-0.82	-0.77	-0.82	-0.86	-0.83	1.10	1.04	0.89	-0.81	-0.92	-0.56	-1.08	-0.75	1.11	-0.87	-0.72	-1.09	-1.14	-1.25	-1.04	' Initial			
2,53	-0.41	1.53	3,56	0,73	0.36	0.19	0,43	0.34	1.00	0.90	0.92	0.78	0.76	66.0	0.90	. 68.0	+6.0	0.57			660	0.65	0.71	0.63	. 86.0	0.45	: 1.58 :	. : 50,1	1,35.1	1.35	0.85	0.80	0.72	1.02	at 500 hrs	新月四周衛	Delta b	
-1.36	-0.52	-0.90	2.76	0.59	1.48	1.45	1.67	1.45	1,70, 🔝	1.67	1.87	1.68	1.58	1.67	1.72	1,70	1.76	1.43	1.50	1.45	13.43	1.54	1.52	1.55	1.54	1.53	2.33	2.16	2.22	2.07	1.94	1.94	1.97	2.06	change	2 mg/s - 2 m	The state of the s	¥ .
82.90	11.20	51.90	12.30	91.60	36.50	40.70	37.10	45.30	32.70	26.20	29.10	32.10	32.00	31.60	30.10	.30.80	43.50	36.80	29.40	34.30	33.50	32.40	30.10	42.70	36.10	26.40	25.70	29.10	39.40	43.50	45.00	28.70	42.00	40.80	1000 hour		Gloss (60	
4,16	-64.78	-35.61	-78.11	-3.07	-32.90	-38.89	-40.35	-30.20	-54.83	-63.66	-55.16	-53.95	-54.09	-52.48	-56.50	-56.00	-26.77	-47.20	-59.05	-51.62	-53.47	-53.98	-58.82	-42.06	-50.28	-61.06	-31.47	-39.50	-32.07	-25.00	-27.07	-44.59	-34.98	-33.22	% change		oss (60 degree)	
4.11	0.52	6.34	11.92	4.96	1.21	0.83	0.99	0.86	2.26	1.86	2.34	1.97	1.66	2.07	2.03	2.18	2.28	1.61	1.98	1.71	1.62	2.03	2.28	2.00	2.75	1.92	3.08	2.18	2.69	2.64	1.69	2.18	1.81	2.13	Delta E		Delta E	QUV1
1.07	0.38	0.58	1.83	0.56	0.33	0.68	0.56	0.75	0.69	0.53	0.91	0.49	0.24	0.46	0.57	0.81	0.88	0.55	0.55	0.48	0.19	0.85	1.13	0.39	1.37	0.71	2.10	0.90	1.49	1.20	0.28	0.81	0.38	1.00	change		LU 53	QUV-1000 hrs.
2.59	-0.10	1.22	3.42	0.70	-0.46	0.21	0.28	0.32	1.20	0.92	1.27	1.02	0.80	1.07	1.19	1.02	1.09	0.67	0.94	0.62	0.75	1.00	1.16	1.00	1.46	0.73	1.49	0.76	1.17	1.16	0.54	0.67	0.41	0.77	Delta b		Delta	
-1.30	-0.21	-1.21	2.61	0.56	.0.66	1.47	1.52	1.43	1.90	1.69	2.22	1.92	1.62	1.75	2.01	1.79	1.91	1.53	1.77	1.72	1.79	1.89	1.97	1.92	2 02	1.81	2.24	1.87	2.04	1.88	1.63	1.81	1.66	1.81	change		<u>ъ</u>	

6 8 3	68	0				4	6	16	a	10	ō	₿(GL)	10	5(GL) 10 GL = Gloss Loss	5(GL)	10	Sher-cryl
10 5 9 8 10 5 10	55 9 8 10	9 6	5 9	У С		ō		10	55	10	10 0	5(GL)	5	5	4(GL)	2	enturion
8 6 10 5	5 8 6 10	5 8 6 3 10	A 5	n (5		5 5		8	3	10 ×	5	2 2	7 4	5 ~	4(GL)	12	Polylon 1900
5 9 7 110 5	5 9 7 710	5 9 7	5	5	H	10		Land Parket	2		3	2	Ž	3	2	2	087
5 10 8 10 5	5 10 8 10 9	5 10 8	5 10	5	\dashv	10			1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	2		1	, 2 Y	3	1 1 3	. 2	086
5 10 6 10 5	5 10 6 10	5 10 6	5 10	5	\dashv	ð	-	0	λ	N	3	1	. 2	2	2	2	085
5 8 7 10 5	5 8 7 10	5 8 7	5	5	\dashv	히	7	ō	2.	2	10		2	10	*	,2	084
5 10 7 10 5	5 10 7 10	5 10 7	5 10	5	+	ō	寸	ā	1.7.	2	10	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	2	ا 4 کا		. 2	083
5 9 7 10 5	5 9 7 10	5 9 7	5	5	+	히	寸	ō	 2	2	5	4	2 "	10	1	2	082
5 9 7 10 5	5 9 7 10	5 9 7	55	5	+	힉	7	ĵō,	2	THE TANK	10		ું દુ 2 *	10		21	081
5 9 7 10 5	5 9 7 10	5 9 7	ڻ.	ڻ.	1	히		6	2 2	2	6	1	2	7.	1	12mi	080
5 7 7 "10"" 5 1	5 7 7 10	5 7 7 "10	5 7	5	1	히	╗	10	Series Barrier	1 (3/2)	1. 6 left.	A. 1. S. 1	1 2 f	5	111	. 2	079
10 8 10 5	5 10 8 1.10	5 10 8	5 10	5	1	ō		1110	111	2	8	. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1.	2	4 1	(11)	, X	078
5 9 7 10 55	5 9 7 10	5 9 7	5 9	5	\dashv	ō		, OF	11 7 11 7 11 7 11 7 11 7 11 11 11 11 11			1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	2	3	1 1	N	077
	5 8 8 %/0//	5 8 8 ¹⁴ 0	ან დ	5	-	0		15.01.54	ME 12 1 1		10.	1	# A	10	1.0	2	076
5 9 7 10 5	5 9 7 10	5 9 7	5	5	-	히		10.		1 2 1	10.	图"图 1 "写	[第2]]	- 6 th	141.	2	075
5 9 7 1910 5 5 6	. 5 9 7	. 5 9 7	5	5	-	ျ		10		2	4	1 1	1.2			. 2	074
5 9 7 10 5	5 9 7 10	5 9 7	5	5	\dashv		_	10	N	2	10	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	2	2.*	1.1	2	073
5 8 7 710 5	5 8 7 710 5	5 8 7	5	5	-	힑		1011		7	The second	5	[1] 2.15	1 1	Mer 1	2	072
6 7 , 10, 10, 5, 1, 1	5 6 7 , 10 5	5 6 7	5	5		ō		10. 	12 Pd 2-1	10 Sept. 1	10.	2	13.5.2.7	4.7	w	2	071
5 9 8 710 5 10	5 9 8 (10	5 9 8	5 9	5	1	٦	5	10	N	ò	10	1	12	2	1.3	1, 1,2 it	070
5 . 9 8 . 10 . 5	5 9 8 10		5 · 9	5	\dashv		ō	10		2	. 10	1 1	1.2.	4		2	069
5 9 7 10 5	5 9 7 10	5 9 7	5	5	-	٦	5	10		1 2	. 6	2	無益 2 ≝	2	2	1. 2.1	068
5 8 7 10 1	5 8 7 10 1	5 8 7	5	5	\dashv	٦	10	101	1.1.70	2 1	5	1.1	27		14.	1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1	067
7 P. 1	5 5 6	5 6	5	5	+	٩			3		1 3.	1.1.2			3.	, Z	055
O	5 9 7 TENONE	5 9 7	5	5		ō			2	2	3.3		2.		liferole average		054
5 10 8 210 37 37 5	5 10 8	5 10 8	5 10	5	\dashv	9	_		: E 3.	2.1	, 2	1 2	2:	1 1 1 1 1	3.	1. 4. 4. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1.	053
5 10 8 10 5	5 10 8 10	5 10 8	5 10	5		٦	ō		100 Co.	6	2.	3.	6		5.1	10	052
5 9 8 10 5	5 9 8 10	5 9 8	5s 60	5		이		M.S.	10000000000000000000000000000000000000	1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1	. 2	2			. 3	7	051
10 5 8 7 10 5 10	5 8 7 10	5 8 7	5 8	· 5		0		118,00 p. 11.			2	3	2.1	1 1 1	31	2	050
10 5 9 6 110 18 10 18 10 10 10 10 10 10 10 10 10 10 10 10 10	5 9 6 10.18	5 9 6	5 9	5		ō			12	. P. A. A. S.	3.	2	4	1.14	3	10 A	049
5 6 7 10 %	5 6 7 10 %	5 6 7	5	5		ိ	1	733	2	4.76		,	2.	1.2		2	048
ly Rust Scribe Size	Density Rust Scribe Size	Density Rust Scribe Size	Density Rust	Density	Dens	6		- 22	_	Sixe	Rust		Size	Rust		Size	Formula
Blister Selection (5 cycle Corrosion Weath	Blister Sister Sister	Blister Sister Sister	Blief	Blief	Blief	13	2		Blister	3		_	Bliston		Blistor Blistor	Blister	
							T	10 m	7 7 7 7 7 7		Harry Bilster Resistance	/ Elister		the state of			
							1	1.5 section - 1		915 4 d ₁ ,		!	The state of the s	1	The state of the s	43.1.	

Г	· '			_	,	_	_	1	_	_			_	_			_	_	_	_	_	T-	_	_	_	_				_	_														_
	047	046	045	044	043	042	<u>Q</u>	Ş	020	020	038	037	036	035	034	033	032	031	023	022	021	020	910	218	21/	010	213	0 4	013	012	011	010	009	800	007	006	205	004	003	002	001	Eomula			
,	<u>,</u>	6	2	4	4	8	2	^	,		2	2	Ν	. 2	2	2	. 2	2	10	10	10	ē	ō	ē	ō	ō		•	10	4	10	10	10	10	10	. 4	.10	. # 6	10	2	•	Size	Blictor	- 2* -	1
	٠	3	3	2	2	3	ω	3	, -		3	27.4	N	. 3	N	ω	2	ω	Ch -	ن ت	5	5	5	5	5	0	•	2	5	4	Ot .	5	5	5	۲.	3 .	5	3.	5	3	ω	8	⊣ ւ:		
Ŀ	•	-	-	_	-	-	3	 :		,	١.	1	Ŋ	_		N	2	2	2	9	8	6	9	8	8	8	6	4	9	3.	8	. 8	9	8	9	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1		2	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1		2	121	7 -	3	
,		8	2	4	2	. 2	2	A : 1.7			3	3	2	2	2	N	4	2	10	0	6	6	4	•	10	G	4	•	10	10	10	10	70	10	5	2	4	4	2	2	2	14			
[, ,		2	3	ü	; 3	1	1	-						1	λ)	1	-	5	5	3	3	3	3	5	4	4	ω	5	6	5	O.	5		6	3	3	3	3	. 2	2	Density	┥.	~	
~	-	3	3	-	2	2"	-6	4	3	0		3	1		8	4	4	3	8	9	8	8	9	9	9	8	8	10	9	8	9	8	8	8	9	2	2	111	2	3	3 3	Rust		Resistanc	
*		.],	3	•	•		4	All A Comp.	2	N			3	3	2	2	A	2	6	4	8	4	•	. 4	6	. 6	. Y. ' 4 '	4 . 4		6	4	.6	8	2	6	6	4	ς, (Σ)	2	10	4	Sizo		•	
2	2	, ,	3	3	3	2	1	. 2		2		至	17.		1	2			3	-	3	2	1 7 9 9 9	ω	2	. 2	3,	3	3.	3	2	3	2	•	2	4	3	17.	3	5		Density	₹_	-	
3	۵			3	3	3.7	A	5.	17.7	· · · · · · · · · · · · · · · · · · ·	ē	0.01	the Carte	n (58	5	N . 34	5	В	8	7	7	70	8	8	8	9	8	. 8	9	8	00	20	5 6	20	ر د *	2	3	3	2	9 :	Rus		-	
10	6	5		5 3	5 6	5	6	8	10	10	ō	ē	5 6		5 6	3 3		5 3	5 3	5 3	5	6	8	8	ō	6	ō	5	6	5	6	0	5 6	5 6	5 6	3 3	5	5 6	5	10	10	Size	Corre		
5	5	o	, 0	, ,	<u> </u>	۸ (הכ	5	5	5	5	0	. 0	ļ	, ,	, (,	, (מ	,	ار	5	5	5	5	5	5	5	5	5	5	١,	, (, ,	, ,	, (, C	,	٦,	,	5	Size Density Rust Scribe	sion We		
7	9	۳	, «			•	<u> </u>	1	8	9	8	9		, •	٥	\$ 6		•	10	ا.	1	ا	8	8	9	<u>.</u>	8	8	8	5		» (٥	٥	» ē	3 4	٥	3	8	Rust	athering		
7	6	7	۵			٥	» ·	7	7	6 0	8	6	~	-	10	• •	-	1	1	1	1,	<u>s</u>	7	7	7	1	8	7	8	s c	»	,	, -	1	10		, 0	•	1	.	7	Scribe	(5 cycle		
10	10	10	ē	ē	2	1		5	6	6	10	8	ē	5	5 2	ē	5	5 2	0	,	i	5 6	3 6	3 3	0	0	ö	30	5	5 6	5 0	ō	5 2	ā	ā		5	5	1	1	3	Blister	Соп		
5	5	5	5	0	0			7	5,	o		ω	5	0		0	O	0		0			7 (7	J. C	,	. אנ	4	5 (n c	1	0	٥			٥	. 0	0				Blister Blister Rust Scribe	sion We	-	
9	6	9	9	9	ē	ē	ē	5 6	5	ō	ō	10	5	5	10	ō	ē	8	ō	"	٦	3	, =	5	٥			,	٥	1	5 "		, a		ō	a		ē	ē	2		Z)	athering		
8	5	7	7	6	9	•	-	1	A (8	8	7	7.	8	6	6	7	8	8	-	0				Ţ	1,	» (٥	, "	,	T	7	7	7	6	6	6	~	, ,	NA NA	2	(6 cycle		

mitial KU 96 140 94 94 99 136 108 91 91 91 95 68 88 68 68 68 68 68 68 68 69 74 68 68 68 68 68 68 68 78 68 68 68 78 68 68 78 68 78 68 78 68 68 78 78 68 78 78 78 78 78 78 78 78 77 88 88		***************************************	The state of the s	n/a	0 77			2		aelled	22	247
	n/a	e/u		n/a	9.22		gelled	1.11	•	gelled	73	046
	n/a	n/a		n/a	9.3		gelled	1.16		gelied	75	045
Initial KU Initial KU Scalange Initial KU Initial KU Scalange Initial KU Initial	n/a	n/a		n/a	9.49		gelled	1.35		gelled	85	244
	n/a	n/a		n∕a	9.5		gelled	0.7		gelled	82	043
	n/a	n/a		ν'n	9.44		gelled	0.86		gelled	85	042
Initial KLI	n/a	n⁄a		n∕a	9.39		gelled	1.79		gelled	92	24.
	πVa	n/a		n√a	9.4		gelled	0.54		gelled	86	040
	n/a	n/a		n/a	9.56		gelled	0.77		gelled	<u></u>	039
Initial KSU Inial KSU Schange Initial PH Inial PH Inia	n/a	n/a		n⁄a	9.55		gelled	1.38		gelled	88	038
Initial KU Inial KU Schange Inial KU Inia	n/a	n/a		n/a	9.23		gelled	0.85		gelled	92	037
Initial KU Marie	n/a	n/a		n/a	9.33		gelled	1.17		gelled	88	036
Initial KU Mal KU	n/a	n/a		n/a	9.44		gelled	1.95		gelled	83	035
Initial KU Inal KU 26 change Initial ICI Inal ICI Schange Initial ICI Initial	n⁄a	n/a		n/a	9.44		gelled	1.13		gelled	8	034
Initial KU Inal KU 26 change Initial ICI Inal ICI Schange Initial ICI	soft	ð	-8.88	8.21	9.01	55.11	1.40	0.9	-18.60	70	86	033
	a ⁄a	n/a		7/0	9.24		gelled	1.5		gelled	72	032
	a /a	n/a		ī√a	9.57		gelled	1.37		gelled	83	031
Initial KU Ini	n/a	π/a		n⁄a	9.48		gelled	0.88		gelled	70	023
Initial KLU Inial Klu In	n/a	n/a		n/a	9.65		gelled	0.78		gelled	8	022
	n/a	n∕a		n/a	9.53		gelled	1.19		gelled	69	021
Initial IXLU Inial IXLU I	n/a	n/a		n/a	9.64		gelled	2.34		gelled	78	020
Initial KU final KU % change initial ICI final ICI % change initial ICI final ICI % change initial ICI final ICI % change initial ICI settling amount 96 gelled 1.6 gelled 9.58 n/a n/a n/a 140 gelled 1.18 gelled 9.59 n/a n/a 94 gelled 1.88 gelled 9.59 n/a n/a 136 gelled 0.69 gelled 9.43 n/a n/a 138 gelled 0.69 gelled 9.43 n/a n/a 139 gelled 1.88 gelled 9.3 n/a n/a 91 gelled 1.88 gelled 9.48 n/a n/a 95 gelled 1.89 gelled 9.42 n/a n/a 85 gelled 9.42 n/a n/a n/a 69 gelled	n/a	n/a		n/a	9.47		gelled	1.28		gelled	63	019
Initial KU final KU % change Initial ICI final ICI % change Initial ICI final ICI % change Initial IDI final IDI % change Initial IDI final IDI % change amount % change amount 96 gelled 1.6 gelled 9.58 n/a n/a n/a 140 gelled 1.16 gelled 9.59 n/a n/a 94 gelled 1.88 gelled 9.43 n/a n/a 136 gelled 0.69 gelled 9.65 n/a n/a 108 gelled 1.88 gelled 9.61 n/a n/a 91 gelled 1.88 gelled 9.32 n/a n/a 95 gelled 1.88 gelled 9.32 n/a n/a 88 gelled 1.11 gelled 9.32 n/a n/a 89 gelled 9.42 gelled 9.09 n/a	n⁄a	n/a		7∕8	1.697		gelled	0.68		gelled	88	018
Initial KU Inial KU Schange Initial ICI Inial ICI Schange Initial ICI Inial ICI Inial ICI Schange Inial ICI Inial	n/a	R	٠	7/9	9.52		gelled	1.63		gelied	62	017
Initial KU Inial KU Sechange Initial KU Inial KU Inial KU Sechange Initial ICI Inial ICI Sechange Initial pH Sechange Initial pH Inial pH Sechange Initial pH Inial	n⁄a	n/a		n/a	9.38		geiled	1.12		gelled	&	016
Initial KU Inal KU Machange Initial ICI Inal ICI Machange Initial ICI Mala Machange Initial ICI Machange Initial ICI Mala Machange Initial ICI Initial ICI Machange Initial ICI Initial ICI	a⁄a	n/a		n√a	9.52		gelled	1.17		gelled	61	015
Initial KU Ínitial KU Á change Ínitial ICI Á change Ínitial ICI Ésettling 96 geiled 1.6 geiled 9.58 n/a Achange amount 94 geiled 1.18 geiled 9.59 n/a n/a n/a 79 geiled 1.88 geiled 9.65 n/a n/a n/a 108 geiled 0.69 geiled 9.65 n/a n/a 108 geiled 1.83 geiled 9.65 n/a n/a 91 geiled 1.83 geiled 9.3 n/a n/a 95 geiled 1.88 geiled 9.3 n/a n/a 68 geiled 1.88 geiled 9.32 n/a n/a 85 geiled 1.11 geiled 9.32 n/a n/a 80 geiled 9.42 9.09 n/a	n/a	n/a		₽/a	9.56		gelled	0.56		gelled	88	014
Initial KLU Inal KLU Sa. change Initial ICI Inal ICI Sa. change Initial ICI Initial ICI Sa. change Initial ICI Sa. change Initial ICI Initial ICI Sa. change Initial ICI Initial ICI Sa. change Initial ICI Initial	n/a	n/a		· n/a	9.32		gelled	0.77		gelled	7.4	013
Initial KU Machange Initial ICI Mal IC	n/a	n/a		7/8	9.45		gelled	0.66		gelled	8	012
Initial KU Inal KU Schange Initial ICI Inal ICI Schange Initial ICI Inal ICI Schange Initial ICI Initial ICI Schange Initial ICI I	n/a	n/a		n/a	9.14		gelled	9.42		gelled	83	011
Initial KU Inal KU Schange Initial ICI Inal ICI Schange Initial ICI Inal ICI Schange Initial ICI Inal ICI Schange Initial ICI Schange Initial ICI Initial ICI Inal ICI Schange Initial ICI Schange Initial ICI Schange Initial ICI Inal ICI Schange Initial ICI Inal ICI Schange Initial ICI Inal ICI Schange Initial ICI	n/a	n/a		n/a	9.09		gelled	0.492		gelled	æ	910
Initial KU Inal KU Schange Initial ICI Inal ICI Schange Initial ICI Inal ICI Schange Initial ICI Inal ICI Schange Initial ICI Inal ICI Schange Initial ICI Inal ICI Schange Initial ICI Initial ICI	a/2	n/a		n/a	9.42		gelled	1.11		gelled	68	909
Initial KU Inal KU Schange Initial ICI Inal ICI Schange Initial ICI	n/a	n/a		n/a	9.32		gelled	1.88		gelled	95	008
Initial KU Inal KU Schange Initial ICI Inal ICI Schange Initial ICI Inal ICI Schange Initial ICI Schange Initial ICI Initial ICI Schange Initial ICI Initial ICI	n/a	n/a		n/a	9.48		gelled	1.88		gelled	91	007
Initial KU Inal KU Schange Initial ICl Inal ICl Schange Initial ICl Schange Initial ICl Inal ICl Schange Initial ICl Initial ICl Schange Initial ICl Initial	n∕a	n/a		n/a	9.3		gelled	1.83		geiled	108	006
Initial KU Inal KU % change Initial ICl Inal ICl Schange Initial ICl Initial ICl Schange Initial ICl Schange Initial ICl Initial	n/a	n/a		₽/2	9.61		gelled	0.69		gelled	136	005
Initial KU Inal KU % change Initial KU Selled 1.18 Selled S	n/a	n√a		n/a	9.65		gelled	1.88		gelled	79	6 4
initial KU final KU % change initial ICI final ICI % change initial DH final pH % change amount 96 gelled 1.6 gelled 9.59 n/a n/a	B/u	n/a		n/a	9.43		gelled	1.16		gelled	94	003
initial KU final KU % change initial ICI final ICI % change initial pH final pH % change amount 96 gelled 1.6 gelled 9.58 n/a settling.	B/U	n/a		n∕a	9.59		gelled	1.18		gelled	140	002
initial KU final KU % change initial ICI final ICI % change initial pH final pH % change amount	n/a	4		B/B	9.58		gelled	1.6		gelled	8	81
Viscosity, settling, and pH Stability (6 weeks at 140F)	t builtes		% change	final pH	initial pH	% change	final ICI	initial ICI	% change	final KU	initial KU	Formula
				s at 140F)	lity (6 week	nd pH Stabi	settling, a	Viscosity,				

	gelled gelled 2.88 gelled gelled 2.88 gelled gelled 9.44 gelled 1.52 gelled 9.83 gelled 1.48 gelled 9.83 gelled 1.48 gelled 9.73 gelled 1.74 gelled 9.73 gelled 9.73 9.81 9.73 gelled 0.51 1.29 51.53 9.81 1637 0.51 1.29 51.53 9.81 1637 0.51 1.29 51.53 9.81 1637 0.51 1.29 51.53 9.81 104 10.59 1.55 0.67 -56.71 9.72 107 18.89 0.41 1.26 208.05 9.73 107 18.89 0.41 1.26 208.05 9.73 109 10.90 0.84 0.79 -5.71 9.87 111 15.63 0.63 0.88 40.16 9.3 93
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 87 gelled 87 gelled 77 gelled 84 70 -16.67 96 111 15.63 94 109 15.96 77 78 1.30 85 93 9.41 94 116 23.40 83 gelled 72 gelled 83 gelled 72 gelled 83 gelled 72 gelled 83 gelled 83 gelled 72 gelled 83 gelled 72 gelled	gelled 2.88 gelled 9.89 gelled 1.52 gelled 9.44 gelled 1.34 gelled 9.89 gelled 1.34 gelled 9.89 gelled 1.48 gelled 9.73 gelled 1.74 gelled 9.31 110 23.60 0.85 1.29 51.53 9.81 1637 0.51 1.22 139.41 9.71 gelled 0.51 1.22 139.41 9.72 gelled 0.73 gelled 9.73 gelled 0.52 n/a 9.72 n/a 10.59 1.55 0.67 -56.71 9.72 n/a 10.59 0.73 gelled 9.72 pelled 0.73 gelled 9.73 9.89 pelled 0.84 0.79 -5.71 9.89 pelled 0.97 0.75 -22.27 9.78 pelled 3.61
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 78 gelled 87 gelled 87 gelled 77 gelled 77 gelled 85 94 10.59 96 n/a 90 107 18.89 90 10.00 90 15.98 77 78 1.30 83 94 116 23.40 83 94 13.25 87 gelled 83 gelled 90 gelled	gelled 2.88 gelled 9.43 gelled 1.62 gelled 9.44 gelled 1.52 gelled 9.63 gelled 1.52 gelled 9.63 gelled 1.34 gelled 9.73 gelled 1.74 gelled 9.73 gelled 0.85 1.29 51.53 9.87 gelled 0.51 1.22 139.41 9.7 gelled 0.51 1.22 139.41 9.7 gelled 0.51 1.22 139.41 9.7 gelled 0.52 n./a 9.7 pelled 0.52 n./a 9.7 pelled 0.00 0.85 0.93 9.29 9.7 pelled 10.00 0.85 n./a 9.7 9.7 pelled 0.08 n./a 0.79 -5.71 9.8 107 1.567 0.84 0.79 -5.71 9.9 pelle
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 58 gelled 78 gelled 87 gelled 87 gelled 77 gelled 77 gelled 85 94 100 90 107 18.89 90 107 18.89 90 99 110 85 94 105 96 111 15.63 97 78 1.30 85 93 9.41 94 116 23.40 83 gelled 72 gelled 73 gelled 74 116 23.40 85 gelled 75 gelled 77 gelled 78 1.30 86 3.61 91 gelled 72 gelled 72 gelled 73 gelled	1 2.88 gelled 1 1.62 gelled 1 1.48 gelled 1 1.74 gelled 23.60 0.85 1.29 51.53 23.60 0.51 1.22 139.41 0.51 1.22 139.41 10.59 1.55 0.67 -56.71 10.59 0.41 1.26 208.05 10.00 0.85 0.93 9.28 11.63 0.63 0.88 n/a 15.96 0.63 0.88 40.16 1.30 1.1 0.79 -28.36 9.41 0.97 0.75 -22.27 23.40 1.06 0.58 40.16 1.30 1.1 gelled 13.25 0.74 0.98 31.76 0.84 gelled 0.78 gelled
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 78 gelled 58 gelled 64 gelled 78 gelled 78 gelled 78 gelled 79 gelled 87 gelled 77 gelled 77 gelled 77 gelled 70 18.89 90 107 18.89 90 107 18.89 90 90 107 18.89 90 90 107 18.89 90 107 78 13.63 94 109 15.98 77 78 1.30 85 93 9.41 94 116 23.40 83 86 3.61 91 gelled 72 gelled 72 gelled	1 2.88 gelled 2.88 gelled 3 1.62 gelled 4 1.48 gelled 5 1.48 gelled 6 1.74 gelled 7 23.60 0.85 1.29 51.53 7 0.51 1.22 139.41 7 0.51 gelled 7 0.52 n/a 7 0.85 0.87 -58.71 7 18.89 0.41 1.26 208.05 7 0.84 0.79 -5.71 7 15.63 0.69 1.10 59.42 7 15.96 0.63 0.88 40.16 7 0.97 0.75 -22.27 7 23.40 1.06 0.58 -45.00 7 3.61 0.71 0.29 -59.44 7 1.1 gelled 7 0.84 gelled
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 78 gelled 58 gelled 658 gelled 78 gelled 664 gelled 78 gelled 78 gelled 78 gelled 79 gelled 79 gelled 77 gelled 77 gelled 77 gelled 77 gelled 77 gelled 77 gelled 70 10.59 90 10.7 18.89 90 10.7 18.89 90 10.7 18.89 90 10.7 18.89 90 10.7 18.89 90 10.59 90 90 90 10.00 90 90 111 15.63 94 109 15.98 77 78 1.30 85 93 9.41 94 116 23.40 87 gelled 87 gelled 91 gelled 91 gelled	d 2.88 gelled 1.62 gelled 1.62 gelled 1.34 gelled 1.34 gelled 1.74 gelled 1.74 gelled 1.74 gelled 1.74 gelled 1.25 1.29 51.53 0.51 1.22 139.41 0.51 gelled 1.25 0.67 -56.71 1.89 0.41 1.26 208.05 10.00 0.85 0.93 9.29 0.8 n/a -16.67 0.84 0.79 -57.1 15.63 0.69 1.10 59.42 13.96 0.63 0.88 40.16 13.00 1.1 0.79 -28.36 9.41 0.97 0.75 -22.27 23.40 1.06 0.58 -45.00 3.61 0.71 0.29 -59.44 1.1 gelled 1.325 0.74 0.98 31.76 0.84 gelled
Initial KU Ifinal KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 87 gelled 87 gelled 89 110 23.60 87 gelled 77 gelled 77 gelled 85 94 10.59 90 107 18.89 90 107 18.89 90 90 107 18.67 96 111 15.63 94 109 15.96 77 78 1.30 85 93 9.41 94 116 23.40 83 94 13.25	1 2.88 gelled 2.88 gelled 3 1.62 gelled 4 1.34 gelled 5 1.48 gelled 6 1.74 gelled 7 23.60 0.85 1.29 51.53 7 0.51 1.22 139.41 7 0.51 gelled 7 0.73 gelled 7 0.85 0.67 -58.71 7 0.86 0.83 9.28 7 15.63 0.89 1.10 59.42 7 15.96 0.63 0.88 40.16 7 1.30 1.1 0.79 -28.36 9.41 0.97 0.75 -22.27 23.40 1.06 0.58 -45.00 3.61 0.71 0.29 -59.44 1.1 gelled 13.25 0.74 0.98 31.76
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 78 gelled 87 gelled 87 gelled 77 7 gelled 77 7 gelled 77 7 gelled 77 78 15.63 94 109 15.98 77 78 1.30 85 93 9.41 94 116 23.40 88 9elled 71 96 111 15.63 94 109 15.98 77 78 1.30 85 93 9.41	1 2.88 gelled 2.88 gelled 3 1.62 gelled 4 1.34 gelled 5 1.48 gelled 6 1.74 gelled 7 23.60 0.85 1.29 51.53 7 0.51 1.22 139.41 7 0.51 gelled 7 0.52 n/a 7 0.85 0.93 9.28 7 0.84 0.79 -59.71 7 15.63 0.69 1.10 59.42 7 15.96 0.63 0.88 40.16 7 1.30 1.1 0.79 -28.36 7 9.41 0.97 0.75 -22.27 7 23.40 1.06 0.58 -45.00 7 0.71 0.29 -59.44
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 58 gelled 78 gelled 87 gelled 87 gelled 77 7 gelled 77 7 gelled 77 7 gelled 77 78 15.63 94 109 15.96 77 78 1.30 85 93 9.41 94 116 23.40	2.88 gelled 1.62 gelled 1.134 gelled 1.148 gelled 1.74 gelled 23.60 0.85 1.29 51.53 0.51 1.22 139.41 0.51 gelled 10.59 1.55 0.67 -56.71 18.89 0.41 1.26 208.05 10.00 0.85 0.93 9.29 15.63 0.89 1.10 59.42 15.96 0.63 0.88 40.16 1.30 1.1 0.79 -28.36 9.41 0.97 0.75 -22.27 23.40 1.06 0.58 -45.00 -59.44
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 78 gelled 58 gelled 69 110 23.60 87 gelled 77 7 gelled 77 78 15.63 94 109 15.96 77 78 1.30 85 93 9.41	2.88 gelled 1.52 gelled 1.52 gelled 1.48 gelled 1.74 gelled 23.60 0.85 1.29 51.53 23.60 0.51 1.22 139.41 10.59 1.55 0.67 -58.71 18.89 0.41 1.26 208.05 10.00 0.85 0.93 9.29 15.63 0.89 1.10 59.42 15.96 0.63 0.88 40.16 1.30 1.1 0.79 -28.36 9.41 0.97 0.75 -22.27 23.40 1.06 0.58 45.00
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 78 gelled 58 gelled 687 gelled 87 gelled 77 gelled 70 18.89 90 107 18.89 90 99 110 -16.67 96 111 15.63 94 109 15.96 77 78 1.30	2.88 gelled 1.62 gelled 1.62 gelled 1.74 gelled 1.74 gelled 23.60 0.85 1.29 51.53 23.60 0.51 gelled 10.51 gelled 10.51 gelled 10.52 n/a 10.59 1.55 0.67 -56.71 10.89 0.41 1.26 208.05 10.00 0.85 0.93 9.29 15.63 0.89 1.10 59.42 15.96 0.63 0.88 40.16 1.30 1.1 0.79 -28.36
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 78 gelled 58 gelled 658 gelled 78 gelled 78 gelled 79 gelled 87 gelled 77 78 15.63 94 109 15.96	2.88 gelled 1.62 gelled 1.62 gelled 1.34 gelled 1.74 gelled 23.60 0.85 1.29 51.53 23.60 0.51 gelled 23.60 0.51 gelled 10.51 gelled 10.52 n/a 10.59 1.55 0.67 -56.71 10.60 0.85 0.93 9.29 15.63 0.88 n/a -16.67 0.84 0.79 -5.71 15.63 0.63 0.88 40.16 1.30 1.1 0.79 -28.36
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 78 gelled 58 gelled 67 gelled 77 gelled 77 gelled 77 gelled 77 gelled 78 gelled 77 gelled 70 18.89 90 107 18.89 90 90 90 90 9107 18.89 90 107 18.89 90 107 18.89 90 107 18.89 90 107 18.89	2.88 gelled 1.62 gelled 1.62 gelled 1.74 gelled 1.74 gelled 23.60 0.85 1.29 51.53 0.51 1.22 139.41 0.73 gelled 10.59 1.55 0.67 -58.71 18.89 0.41 1.26 208.05 10.00 0.85 0.93 9.29 15.63 0.69 1.10 59.42 15.96 0.63 0.88 40.16
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 78 gelled 58 gelled 658 gelled 78 gelled 78 gelled 78 gelled 70 18.89 90 107 18.89 90 107 18.89 90 107 -18.67	2.88 gelled 1.62 gelled 1.62 gelled 1.34 gelled 1.74 gelled 23.60 0.85 1.29 51.53 0.51 1.22 139.41 0.73 gelled 10.59 1.55 0.67 -58.71 18.89 0.41 1.26 208.05 10.00 0.85 0.93 9.29 1.667 0.84 0.79 -5.71 15.63 0.69 1.10 59.42
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 78 gelled 58 gelled 658 gelled 78 gelled 78 gelled 78 gelled 79 gelled 87 gelled 77 gelled 77 gelled 77 gelled 77 gelled 77 gelled 85 94 10.59 96 n/a 90 107 18.89 90 1000 90 gelled -16.67	2.88 gelled 1.62 gelled 1.62 gelled 1.34 gelled 1.74 gelled 23.60 0.85 1.29 51.53 0.51 1.22 139.41 0.51 gelled 0.73 gelled 10.59 1.55 0.67 -56.71 18.89 0.41 1.26 208.05 10.00 0.85 n/a -16.67 0.84 0.79 -571
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 78 gelled 58 gelled 69 110 23.60 87 gelled 77 gelled 85 94 10.59 96 n/a 90 gelled	2.88 gelled 1.62 gelled 1.62 gelled 1.34 gelled 1.74 gelled 1.74 gelled 23.60 0.85 1.29 51.53 0.51 1.22 139.41 0.51 gelled 10.53 gelled 10.59 1.55 0.67 -56.71 18.89 0.41 1.26 208.05 10.00 0.85 n/a 0.83 9.28
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 78 gelled 58 gelled 69 110 23.60 87 gelled 77 gelled 78 98 10.59	2.88 gelled 1.62 gelled 1.34 gelled 1.48 gelled 1.74 gelled 23.60 0.85 1.29 51.53 0.51 1.22 139.41 0.51 gelled 10.59 1.55 0.67 -56.71 18.89 0.41 1.26 208.05 10.00 0.85 0.93 9.29
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 78 gelled 58 gelled 87 gelled 87 gelled 87 gelled 77 gelled	2.88 gelled 1.62 gelled 1.34 gelled 1.48 gelled 1.74 gelled 23.60 0.85 1.29 51.53 0.51 1.22 139.41 0.51 gelled 10.59 1.55 0.67 -56.71 0.52 n/a 18.89 0.41 1.26 208.05
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 138 gelled 78 gelled 58 gelled 78 gelled 87 gelled 87 gelled 87 gelled 77 gelled	2.88 gelled 1.62 gelled 1.34 gelled 1.48 gelled 1.74 gelled 23.60 0.85 1.29 51.53 0.51 1.22 139.41 0.73 gelled 10.59 1.55 0.67 -56.71
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 58 gelled 78 gelled 87 gelled 87 gelled 89 110 23.60 77 gelled 77 gelled 77 gelled 77 gelled 77 gelled 77 gelled	2.88 gelled 1.62 gelled 1.34 gelled 1.48 gelled 1.74 gelled 23.60 0.85 1.29 51.53 0.51 1.22 139.41 0.73 gelled 10.59 1.55 0.67 -58.74
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 58 gelled 78 gelled 87 gelled 87 gelled 89 110 23.60 87 gelled 77 gelled	2.88 gelled 1.62 gelled 1.34 gelled 1.48 gelled 1.74 gelled 23.60 0.85 1.29 51.53 0.51 1.22 139.41 0.73 gelled 0.73 gelled
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 138 gelled 78 gelled 58 gelled 87 gelled 87 gelled 89 110 23.60 98 gelled	2.88 gelled 1.62 gelled 1.34 gelled 1.48 gelled 1.74 gelled 23.60 0.85 1.29 51.53 0.51 1.22 139.41
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 58 gelled 78 gelled 87 gelled 89 110 23.60	2.88 gelled 1.62 gelled 1.34 gelled 1.48 gelled 1.74 gelled 23.60 0.85 1.29 51.53 0.51 1.22 139.41
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled 58 gelled 989 110 23.60	2.88 gelled 1.62 gelled 1.34 gelled 1.48 gelled 1.74 gelled 23.60 0.85 1.29 51.53
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 138 gelled 78 gelled 58 gelled 87 gelled	2.88 gelled 1.62 gelled 1.34 gelled 1.48 gelled 1.74 gelled
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 138 gelled 78 gelled 58 gelled	2.88 gelled 1.62 gelled 1.34 gelled 1.48 gelled
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled 78 gelled	2.88 gelled 1.62 gelled
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 138 gelled	2.88 gelled
Initial KU final KU % change 80 gelled 86 gelled 68 gelled 64 gelled	2.88 gelled
Initial KU final KU % change 80 gelled 86 gelled 68 gelled	COO GENERAL
Initial KU final KU % change 80 gelled 86 gelled	0.63 Called
initial KU final KU % change	1.66 gelled
Initial KU final KU % change	1.34 gelled .
Viscosity, settling, and pH Stability (6 weeks	% change initial (C) final (C) % change
	Viscosity, settling, and pH Stability (6 v

		_	Т	Т	7	Т	_	1		_				7	_	_1	1	Т			Т					П	П	1	1	Т	┑	П	T	٦	T	П	Т	T	1		
047	046	045	044	043	042	2	040	039	038	037	036	035	034	033	032	031	023	022	021	020	019	018	017	016	015	014	013	012	011	910	009	008	007	006	005	004	003	002	001	Formula	
ω	3	3	3	3	ω	2	2	2	2	2	2	2	2	2	2	2	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	4	3	ω	3	3	3	ω	Resin	
7	8	5	1	-1	_	7	7	2	11	8	3	1	1	4	ယ	2	3	11	3	11	7	2	1	5	1	11	8	3	10	10	з	5	-	ω	11	2	7	8	2	Dispersant	
2	2	2	2	2	2			1	1	-	1	1	1	2	2	2	-	1	1	-	1	1	1	1	1	2	2	2	2	2	2	2	2	-1	_	_	_	1		Dispersant amount	
1	3	8	7	-	4	6	8	8	2	4	4	5	7	8	6	1	7	2	6	4	1	4	8	3	2	8	7	7	2	2	3	5	7	7	7	6	5	5	3	Thickener	
1.40	1.83	1.72	1.91	1.60	1.80	1.46	1.51	1.78	1.74	1.57	1.59	1.61	1.69	1.60	1.39	1.63	1.67	1.81	1.64	1.70	1.71	1.62	1.72	1.48	1.88	1.60	1.85	1.61	1.48	1.62	1.61	1.74	1.60	1.91	1.86	1.66	1.86	1.71	1.74	Eilm Build	
32.8	6.5	30.9	6.2	16.2	22.4	22.3	27.4	24.3	42.8	14.2	15.5	12.7	22.9	11.8	39.3	20.9	29.9	22.6	31.4	28.5	7.8	23.9	12.6	30.5	21.8	26.0	6.8	14.4	3.8	6.8	23.5	25.5	26.1	13.1	19.3	6.5	35.3	18.5	4.2	20	Gloss
66.5	31.3	64.9	33.9	51.4	59.2	58.9	62.8	59.7	71.5	47.2	49.3	46.4	60.3	44.6	68.4	55.9	65.4	59.5	63.0	60.6	36.9	62.0	47.1	63.2	59.2	56.7	34.1	45.3	23.6	34.4	59.4	62.4	61.5	50.1	63.1	33.8	68.3	56.7	23.3	<u>60</u>	SS
4	O1	4	2	3.5	4	3	4	3.5	4	4.5	4	4	4	4	4	3	3	4	3.5	4	5	3	4.5	4	3.5	3.5	3	3	نئ	3	5	4.5	4	3	4	5	4	4	cu	Coppertone	
2	3	2	2	3.5	2	4	3	3	2	3	3	3	3	3	5	3	•	4	5	5	5	3	3	3.5	3	5	ST.	4	3	ω	3	G,	O1	•	2	5	2	3	3	Toluene	
3	5	3	4	5	4	5	4	5	5	4.5	4.5	G	5	3.5	5	5	a	5	4.5	4	4	5	4	5	3	5	5	4	4	5	5	5	5	o	5	4.5	3.5	5	5	IPA	Ω
2	3	2	3	3	3	3	3	4	4	4	u	ú	3.5	3	5	4		5	5	3	5	ű	3	3	3	5	4	G	**	4	Ö	5	Ν	-	3	4	ü	-	ü	MEK	Chemical Resistance
3.5	3.5	3	3	ယ	3.5	3	3	3.5	ü	ű	, 4	, .	3.5	2	3.5	_	2	3	2.5	2	3.5	2	2	2	2	3.5	2	2	2	2	3,5	3.5	3	2,6	သ	2.5	3	u	ú	DWG	esistance
5	5	2	5	5	5	5	5	0	o	o	. 0	0	0	5	5	5	0	4	on on	o	5	~	5	3	3	5	5	L C	3	2	5	2	o	0	5	5	5	3	3	Sulf	1
4	5	3	5	4.5	5	5	3	o	3		, 0	, 0	, 0	5	5	5	3	0	5	3	3 3		5	, ,	4.0	o	5			4.5	o	5	3		5	o	4	o		NaOH	
2	4	2	3	3	2	2	G	, 0	, 0	3 0	3 0	s	ی د	6	2	~	a	O	4.5	0	4	٥	4.5	•	4	4	. 0	4.0	0	5	0	G	o	. 0	K			٥	, 0	F409	

Table 9 OVEN BAKE

Table 9 (Cont.)
OVEN BAKE

				KA 1700T	KA 1400	880	087	086	280	084	083	082	081	080	079	820	770	076	075	074	073	072	071	070	069	890	067	055	054	053	052	. 051	050	049	048	Eormula		
						2	2	2	2	1	-1	-1	-1	-1		-1	1	1	1	1	1	1	1		1	1	1	သ	2	ယ	3	ယ	ယ	ပ	3	Resin		
						8	5	5	1	3	9	10	7	3	2	9	9	9	5	2	7	11	3	3	8	1	5	8	8	9	6	5	3	8	11	Dispersant		
					,	2	2	2	2	1	1	1	1	1	1	1	1	1	1	2	2	2	2	2	2	2	2	2	1	_	1	1	2	2	2	Dispersant amount		
						4	7	7	3	6	5	1	3	8	1	4	5	1	2	5	6	5	2	2	2	6	3	4	4	2	1	4	5	6	3	Thickener		
				1.49	1.28	2.05	1.54	1.40	1.48	1.80	1.57	1.94	1.70	2.32	2.70	1.91	1.57	2.13	1.97	1.52	1.69	1.65	1.50	1.60	1.63	1.72	1.66	1.33	1.67	1.56	1.54	1.71	1.87	1.36	1.83	Film Build		
				4.1	77.8	18.0	36.6	26.4	32.5	32.8	29.4	28.0	32.1	32.8	24.6	30.3	28.7	24.8	28.9	27.9	32.9	40.9	28.7	30.1	31.8	33.3	25.5	7.5	10.0	21.7	24.4	23.9	13.0	26.8	27.7	20	ପ୍ର	CATTA
				25.4	96.7	51.4	68.6	61.4	65.3	67.0	67.0	63.6	65.7	66.5	61.7	65.7	65.4	61.0	66.6	66.3	67.4	71.0	65.2	67.7	68.8	68.5	63.3	34.3	45.2	57.2	60.1	63.2	46.7	65.2	63.4	60	Gloss	ייניאיניי
				4	4.5	4	ω	4	3	3	4	4	4	3.5	4	4	4	4	4	3.5	4	3	3.5	4	3	3	. 4	5	3	4.5	3	4	4	4	4	Coppertone		
				3	4	4	2.5	3	3	3	3	3	5	3	3	3.5	သ	3	3	3.5	2	3	3	3	3	3	3	2	2	3	5	5	3	3	2	Toluene		
				5	6	5	4	4	4	4	5	3	5	5	3	4	4	4	3.5	5	4	4.5	3	4	4	4.5	4	5	5	5	5	თ	3	5	ယ	IPA	5	
				4	2	5	2	3	3	3	4	2.5	3	ဒ	4.5	သ	ယ	ω	ယ	3.5	N	3.5	ပ	ယ	3	4	ဒ	3.5	3	ω	3	5	2.5	3	2	MEK	emical R	
				4	0	3.5	3.5	3.5	3.5	3	2	2	ပ	သ	သ	အ	2	2	2.5	2	N	2	2.5	2	2	3	N	2.5	3.5	2.5	3.5	3.5	ω	ω	3	DWO	Chemical Resistance	
				2	O	5	5	5	5	cn	3	5	4.5	4	5	5	4.5	Ch	5	5	3	5	2	3	5	2	2	3	5	3	O1	4.5	3.5	4	S.	Sulf		
				9	0	5	ω	5	5	5	3	5	4.5	3	5	4	4	5	5	G	5	3	5	3	5	3	5	3	5	3	51	3	3	4	5	NaOH		
				3	O	3	u	ω	u	4.5	4	4	4.5	4	4.5	4	55	5	5	5	u	4	4	3	4	5	5	4	3	3	5	3	3	3.5	2	F409		

30 O W	1	מ	CE 410/	3						
n «		o	42.17%	18.1	20	10	1	8	6	046
	-	, a	-73.81%	17	yes	10	1	8	6	045
		8	-40.71%	20.1	ПО	10	1	8	6	044
0		6	-67.32%	16.8	yes	10	1	8	6	043
8		10	-73.99%	15.4	yes	7	1	6	6	042
7		8	-62.48%	22.1	yes	9	1	8	6	041
6		8	-57.64%	26.6	yes	6	1	6	5	040
	F	6	-72.70%	16.3	no	10	1	8	4	039
7	3	6	-68.95%	22.2	yes	9	1	8	6	038
7		8	-100.00%						6	037
9	-	8	-68.15%	15.7	yes	10	1	8	6	036
7		6	-61.42%	17.9	yes	6	1	8	6	035
10		10	-59.20%	24.6	yes	7	1	4	6	034
7	-	8	-66.37%	15	yes	8	1	8	6	033
000	\mid	8	-62.43%	25.7	yes	7	1	8	6	032
9	F	6	-61.72%	21.4	yes	5	1	8	6	031
6	l	8	-81.80%	11.9	8	7	1	4	6	023
7		6	-86.72%	7.9	yes	10	1	4	6	022
9	-	10	-85.56%	9.1	yes	10	1	4	5	021
6		6	-86.63%	8.1	no	9	1	4	6	020
5		6	-88.08%	4.4	yes	10	1	4	9	019
7		6	-84.19%	9.8	no	9	1	2	6	018
7		6	-86.62%	6.3	yes	9	1	4	6	017
9		8	-88.29%	7.4	no	10	1	4	6	016
7		8	-88.68%	6.7	no	9	-1	2	6	015
8		8	-82.54%	9.9	yes	10	1	6	6	014
8		8	-75.66%	8.3	yes	9	1	6	6	013
7	<u> </u>	6	-87.42%	5.7	yes	8	1	4	6	012
6	3	8	-80.08%	4.7	yes	10	-1	6	6	011
8		6	-83.43%	5.7	yes	9	-1	6	6	010
8		8	-90.40%	5.7	yes	10		4	6	009
9		6	-88.14%	7.4	yes	8	1	O	7	008
8		6	-88.13%	7.3	yes	9	1	6	8	007
9	3	8	-68.86%	15.6	Yes	10	1	8	6	006
8		8	-73.53%	16.7	yes	10	1	6	6	005
8		8	-55.92%	14.9	no	10	1	8	6	004
9		8	-78.62%	14.6	yes	8	1	8	O	003
-	4	6	-70.02%	17	yes	10	1	8	ō	002
H	-	6	-46.35%	12.5	no	10	1	8	6	001
ensity Rust Scribe	e Blister density	Blister size	% change 60. gloss	Gloss 60	Flash rust-Y or N	Rust	Blister. density	Blister size	Hardness	Formula
Salt Spray-100 HOURS	Salt S				Humidity-200 hours	Humid			Pencil	
				OVEN BAKE						

			,	KA 1700T	KA 1400	388	087	980	085	084	083	082	081	080	079	078	077	076	075	074	073	072	071	070	069	890	067	055	054	253	052	051	.050		048	Formula		
				9	4	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	6	o	6	6	6	0	6	6	6	6	6	6	6	6	6	Hardness	Pencil	
				none	none	8	8	8	8	8	8	8	8	8	8	8	8	8	none	8	8	none	8	8	8	none	8	8	8	8	8	8	8	8	8	Blister size		
						1	-1	1	1	1	1	1	1	-1	1	4	1	1		1	-1		1	~	1		1	1	-1	1	1	mb	1	-1	-1	Blister_ density		
				10	10	9	7	8	7	10	10	10	10	9	9	10	9	9	6	10	10	10	8	8	7	10	8	10	10	10	10	10	10	9	10	Rust	Humi	
				70	8	yes	yes	yes	yes	yes	no	ПO	yes	yes	yes	no	yes	yes	ye s	yes	no	yes	yes	yes	yes	yes	no	no	yes	yes	yes	yes	yes	yes	yes	Flash rust-Y or N	Humidity-200 hours	
				19.4	96.5	16.8	20.9	16.8	17.6	21.7	14.3	12.9	16.8	14.7	17.2	23.8	15.7	13.3	14.5	15.9	16.4	19.6	19.4	19.5	18.4	19	13.1	15	15	15.7	12.9	13.7	14.9	25.7	16.8	Gloss.60		
						-67.32%	-69.53%	-72.64%	-73.05%	-67.61%	-78.66%	-79.72%	-74.43%	-77.89%	-72.12%	-63.77%	-75.99%	-78,20%	-78.23%	-76.02%	-75.67%	-72.39%	-70.25%	-71.20%	-73.26%	-72.26%	-79.30%	#REF!	#REF!	-72.55%	-78.54%	-78.32%	-68.09%	-60.58%	-73.50%	% change 60. gloss		
				4	8	10	8	8	6	8	10	8	8	8	6	8	8	8	8	æ	8	8	8	10	8	10	8	6	8	8	8	6	8	8	6	Blister size		
				2	4	5	4	4	4	4	5	4	4	4	4	4	4	4	4	4	4	ပ	4	5	4	5	4	3	4	4	3	3	4	4	4	Blister density	Salt Spray	
				4	10	00	8	8	6	9	9	9	8	9	8	9	8	8	8	8	9	8	7	10	8	8	4	4	8	9	9	9	8	8	9		Salt Spray-100 HOURS	
				,	2	4	3	w	3	2	2	2	2	2	2	u	2	2	2	2	2	-	2	2	2	2	2	ω	4	4	4	4	4	4	4	Scribe		

Table 9 (Cont.) OVEN BAKE

.047	046	045	044	043	042	041	040	039	038	037	036	035	034	033	032	031	023	022	021	920	019	018	017	016	015	014	013	012	21	010	909	800	007	၁06	005	400	003	002	001	Formula			
6	6	8	8	o	10	8	8	6	G	8	8	o	ō	8	8	o	8	6	ð	0	6	.0	6	0	8	8	8	6	8	6	8	6	6	8	8	8	8	G.	ō	Blister size			
3	4	4	3	4	5	4	3	4	3	4	4	4	5	4	4	3	4	4	IJ.	4	ຜ ≟	4	4	4, , ; ; ;	4	4	4	4	3	3 ::	4	4	٨	3	4	4	4	4	4	Blister density	Salt Spray-200 HOURS		
7	6	9	9	6	8	7		6	7	7	9	7	10	7	8	9	. 4	7	9	Ø	5	6	7		. 7	8	. 8	7	On	8	8	9	8	မွ	8	œ	9	8	8	Rust	MOURS		
3	4	ž W		3	3	*	3	•		16. A	3	() () () () () () () () () ()	4	3	. 3	. 2	2	3	. 3	, 1915 , 2	0	Light of 11 lift was a	ing "genig and different of	1.2		;': ' 3 ';'';'.	3.	2	2	25,82	:: 0 :: 0	2	3	5	4	4	4	4	(J)	Scribe			
24	20	24	24	24	24	20	20	20	20	200	20	3 2	20	20	20	20	24	24	28	28	24	24	24	24	28	32	24	28	24	24	28	28	20	24	20	24	24	24	24	Eonward	Impact		
^4	^4	^4	4	^4	4	^4	^4	^4	4	1	4	1	4	4	^4	^4	<4	<4	<4	<4	4	<4	<4	<4	4	<4	8	<4	<4	<4	<4	٨4	4.4	< 4	< 4	<4	^4	^4	^4	Reverse	act		Table 9
400	100	850	120	2	61	5	20	6	200	306	300	100	160	8	150	250	1000	1000	950	1000	800	450	1000	250	1000	450	650	1000	1000	800	1000	1000	700	200	250	150	500	150	100	MEK Rubs			(Cont.) BAKE
4	4	J	n O	7	. 4		3 0	3 8	3 (4		A (3 0	4	4	3	3	4	3	3	3	3	4	4	5	4	4	3	4	3	3	4	3	4	ω	4	5	4	aluminum	Adnesion	Adhanian	
	ē	5 8	5 6		5 6	i		5 6		5 6	5 6	10 0	5 6	5 6	10	10	4	8	6	4	4	8	6	6	10	4	10	6	10	ō	4	4	4	10	ō	ō	10	10	đ	Blister size			
,	n o	7	אר	A	ח	7 0	T C	5	٦ (5	5 0	5 (5 (, 0	0	0	3	4	. 3	3	3	2	3	2	J	ü	O	2	9	5	3	N	3	5	(Jr	5	0	O	5	density	Bliefer	48 H	
-	3 3	+	و م	100	100	100	100	10	9	9	10	10	100	500	, 0	5 6	6	10		ī	*		9	100	100	5	5 6	0	, 5	ō	10	ō	8	ō	16	-	P	3 6	5 3	Rust	40 Fil. YVatel Ovan	Water Soak	
-	,,	ارد	5	5.	55	4	4	4	4	4	5	5	5	55 (n c	. 4	4		4	3	3 6	ه د			3 0		, 4	٥	n 4	3	-	-	2	U	4	4		n c		Adhesion			

088 KA 1400 KA 1700T	083 084 085 086	079 080 081 082	074 075 076 077 077	069 070 071 072 073	052 053 054 055 067	048 049 050 051	Formula
♣ 8 10	8 8 6 8 6	œ œ œ თ	CO CO CO CO CO	a ca ca ca ca ca	10 8 8 8	o o o	Blister size
2 4 0	0 4 4 4 4	444	4444	4 6 4 8 4 4	ω 4 4 ω 4 α	3 4 4 4	Salt Spray-200 HOURS Blister density Rust
7 10	ထ ထ တ	ဖ ထ ဖ ထ	w	8 7 7 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8	0 0 0 4 4 0	9 8 9	200 HOURS
7 2	ယ် ယ ယ လ ယ	N N N N	M N N W	אמבאא	4 4 4 6	0 4 4 4	Scribe
20 > 168 88	24 20 20 20	24	24 24 2	24 24 24 24	20 20 24 24 24	28 24 20 20	Impact Forward B
< 4 > 168	4444	4 4 4 4	4444	4 4 4 4 4 4	4 4 4 4 4 4	4 4 4	everse
50 650 1000	50 50	1000 1000	50 800 1000 900	600 1000 500 650	650 50 200 400 750	150 150 450 550	MEK Rubs
4 (7) 170	ω 4 ω	4040	0000	0 - 0 3	A 0 0 0 - W	4 4 70 4	Adhesion treated aluminum
1000	10000	D & & O	a a a 10 a	10 8 9	a 10 0 10 10 10 10 10 10 10 10 10 10 10 1	5 6 6 6	Blistersize
G G G	10 4 10 10 m	4 4 2	4 D U U 4	& N 03 N N 3	N 01 N 01 01 01	თ თ თ თ	48 Hi Blister density
1 10 10	10 10 10	9 10 10	10 10	0 0 0 0	10 10	10 0 0	48 Hr. Water Soak 91. Bust
4 70 G	1041044	4 4 70 4	4 2 4 2	4 4 0 0 0	n n a 4 4 n	4 4 10 10	Adhesion

047	046	045	044	043	042	041	040	039	038	037	036	035	034	033	032	031	023	022	021	020	019	018	017	016	015	014	013	012	011	010	900	800	007	006	005	20	003	002	001	Formula		
66.9	36.1	65.6	35.3	53.6	59.3	58.1	64.7	60.6	67.6	48.5	50.0	48.1	62.1	47.7	72.0	59.2	73.5	64.8	68.5	68.3	36.7	67.5	49.5	70.3	62.4	63.7	36.0	49.8	25.2	37.7	57.7	2.4	63.0	50.2	63.7	46.9	68.5	MIS	29.1	60° Gloss		
0.30	0.42	0.41	0.43	0.55	0.24	0.32	0.61	1.23	1.63	0.59	0.18	0.82	0.94	0.39	0.37	0.51	4.95	5.02	4.58	4.31	5.34	4.79	4.90	4.08	4.32	3.30	4.74	3.85	4.12	3.83	3.01	3.53	3.72	0.25	1.47	1.65	0.31	MISSING PANEL	0.96	Delta E	QUV-Initial	
-0.08	-0.11	-0.41	-0.08	-0.53	-0.19	-0.15	-0.42	0.28	1.22	0.06	-0.09	-0.25	0.21	-0.02	-0.35	0.05	3.92	3.96	3.71	3.48	4.20	3.74	3.87	3.30	3,42	2.50	3.73	3.03	3.01	3.00	2.45	2.87	3.03	-0.11	0.44	-0.58	-0.21	IEL	-0.21	Delta YB		
58.8	28.3	58.1	25.3	41.6	41.2	42.9	49.1	49.4	59.1	34.9	33.8	32.3	49.1	33.3	59.7	50.4	34.6	16.3	24.9	30.3	11.4	26.1	16.3	29.1	23.0	17.9	12.8	14.1	6.2	8.5	18.4	21.6	19.9	33.9	42.7	25.1	53.1		18.7	60° Gloss		
1.93	2.63	2.16	2.47	1.95	2.38	1.58	1.25	2.08	2.02	2.25	1.52	1.52	1.82	1.05	0.88	1.23	4.28	4.84	4.52	4.64	5.16	4.50	5.10	4.07	4.49	3.91	5.51	3.96	5.34	4.99	3.13	3.62	3.89	2.99	3.41	2.59	2.03		2.85	Delta E		
0.99	1:31	1.19	1.25	0.91	1.23	0.75	0.44	1.14	1.26	1.22	0.60	0.62	1.07	1.11	0.33	0.69	2,72	2.94	2,76	2.98	3.37	2.85	3.21	2.54	2.75	2.36	3.34	2.40	3.01	2.93	1.87	2,29	2.40	1.60	1.98	0.65	0.92	MISSING PANEL	1.24	Delta YB	QUV-5	H
-12.11%	-21.61%	-11.43%	-28.33%	-22.39%	-30.52%	-26.16%	-24.11%	-18.48%	-12.57%	-28.04%	-32.40%	-32.85%	-20.93%	-30.19%	-17.08%	-14.86%	-62.93%	-74.85%	-63.65%	-55.64%	-68.94%	-61.33%	-67.07%	-58.61%	-63.14%	-71.90%	-64.44%	-71.69%	-75.40%	-77.45%	-68.11%	-66,46%	-68.41%	-32.47%	-32.97%	-46.48%	-22.48%	PANEL	0	% Loss of	QUV-500-HOUR	OVEN
1.63	2.21	1.75	2.04	1.40	2.14	1.26	0.64	0.85	0.39	1.66	1.34	0.70	0.88	99.0	0.51	0.72	0.67	0.18	0.06	0.33	0.18	0.29	0.20	0.01	0.17	19'0	0.77	0.11	1.22	1.16	0.12	0.09	0.17	2.74	1.94	0.94	1.72		1.89	Change ir delta E		BAKE
1.07	1.42	1.60	1.33	1.44	1.42	0.90	0.86	0.86	0.04	1.16	0.69	0.87	0.86	1.13	0.68	0.64	-1.20	-1.02	-0.95	-0.50	-0.83	-0,89	-0.66	-0.76	-0.67	-0.14	-0.39	-0.63	0.00	-0.07	0.58	-0.58	-0.63	1.71	1.54	1.23	1,13		1.45	₽		
61.7	31.2	59.7	29.6	44.6	44.5	48.8	53.7	51.0	59.8	41.5	37.4	36.1	53.4	38.8	63.2	51.5	24.7	12.1	20.7	20.9	8.3	15.5	11.9	24.6	16.8	15.7	11.9	10.6	5.7	8.9	16.8	16.9	17.2	32.5	47.4	22.9	54.9			66		
2.01	2.63	2.44	2.33	2.05	2.04	1.60	0.81	2.06	2.16	2.13	1.23	1.60	2.10	1.71	1.33	1.45	3.89	4.35	4.16	3.76	4,44	3.87	5.07	3,69	3.84	3.05	5.09	3,99	4,54	4.47	2.62	3.15	3.49	2.78	3.32	2.12	1.55		2.00	Delta E		
0.77	1.19	1.09	0.98	0.75	0.89	0.69	-0.01	0.94	1.15	1.08	0.30	0.60	1.10	0.88	0.47	0.71	2.13	2.43	2.30	2.03	2.51	2.10	2.83	2.05	2.15	1.44	2.87	2.16	2.31	2.37	1.39	1.72	1.98	1.26	1.67	-0.05	0.49	MISSING	0.55	Delta YB	QUV-1	
-7.77%	-13.57%	-8.99%	-16.15%	-16.79%	-24.96%	-16.01%	-17.00%	-15.84%	-11.54%	-14.43%	-25.20%	-24.95%	-14.01%	-18.66%	-12.22%	-13.01%	-66.39%	-81.33%	-69.78%	-69.40%	-77.38%	-77.04%	-75.96%	-65.01%	-73.08%	-75.35%	-86.94%	-78.71%	-77.38%	-76,39%	-70.88%	-73,76%	-72,70%	-35.26%	-25.59%	-51.17%	-19.85%	MISSING PANEL	-36.43%	% Loss of 60 gloss	QUV-1000-HOUR	
1.71	2.21	2.03	1.90	Γ	Γ	1.28	0.20	0.83	0.53	1.54	1.05	Г		1.32	0.96	0.94	1.06	0.67	0.42	0.55	0.90	0.92	0.17	0.39	0.48	0.25	0.35	0.14	0.42	0.64	0.39	0.38	0.23	2.53	1.85	0.47	1.24		1.04	Change in delta E		
0.85	1.30	1.50	1.06	1.28	1.08	0.84	0.41	0.66	-0.07	1.02	0.39	0.85	0.89	0.90	0.82	0.66	-1.79	-1.53	1.41	-1.45	-1.69	<u>-</u> 2	<u>:</u>	-1.25	-1.27	÷1.86	-b.86	-0.87	-0.70	-0.63	- <u>1</u> .8	-1.15	-1.05	1.37	1.23	0.53	0.70		0.76	l 15		

П	Т	Т	न	Į	<u> </u>	φĮ	۲	<u>ک</u>				1	٦	7	_1	Т	Ţ	П	٦	٦	٦	1	Т	T	Т	Т	T		T	Т	T	Τ	Τ	Τ	Τ	T	Τ	Ţ,	m	\prod
			700T	HS+	enturion	Sher-crvl	KA 1700T	KA 1400	288	087	086	085	084	083	082	081	88	079	078	077	076	075	074	073	072	071	070	069	068	987 87	200	200	202	200	050	949	2 6	DAR	Formula	
			22.0	7	1	1	26.5	97.0	54.4	68.8	62.7	67.9	68.7	69.3	63.5	67.8	67.9	63.3	67.3	67.2	61.2	67.9	68.6	68.2	69.8	66.7	68.5	69.8	68.2	200	35.5	20.0	02.7	3 2	46.8	97.4	200	RA O	60° Gloss	
			2.48	7.95	10.50	7.97	4.14	2.86	0.22	0.31	0.46	0.50	0.86	0.55	0.49	0.50	0.53	0.93	0.62	0.60	0.63	0.43	0.54	1.03	0.79	0.61	0.83	0.78	0.50	0.56	0.97	100	0.40	9 5	0.84		0.57	0.57	Delta E	QUV-Initial
			1.88	6.40	1.92	4.05	0.42	-0.24	6.11	-0.25	-0.26	-0.38	-0.23	-0.35	-0.47	-0.35	-0.33	0.01	-0.24	-0.26	-0.41	-0.32	-0.34	-0.88	-0.67	-0.57	-b.66	-0.53	0.40	-0.55	000	5 5	0.00	3 6) di	3 5	0.57	-0 43	Delta YB	
			15.3	78.0	32.9	74.3	25.0	92.1	45.2	56.5	48.7	57.4	46.4	49.9	44.2	41.0	44.4	41.8	43.0	37.8	37.6	38.0	39.9	40.6	49.5	47.5	50.6	53.5	50.2	45.6	22.3	30.3	47.4	48 6	KO 3	35.0	53.9	5 <u>4</u> 8	60° Gloss	
			0.84	3.58	11.32	6.26	4.14	3.75	1.46	1.05	1.13	1.13	1.68	1.32	1.62	1.20	1.20	1.55	1.52	1.62	1.55	1.39	0.99	0.91	0.72	1.03	0.98	0.93	1.28	0.96	2.79	248	340	291	240	3 23	1 95	2.41	Delta E	
			-0.25	2.46	4.46	1.07	-0.08	1.86	0.75	0.38	0.41	0.47	0.84	0.71	0.85	0.58	0.63	0.86	0.85	0.87	0.83	0.71	0.49	0.16	0.21	0.25	0.42	0.40	0.61	0.39	1.36	0.91	1 19	1 32	1.13	0 03	0.47	 8	Delta YB	QUV-5
			-30.45%	-2.50%	-35.11%	-7.13%	-5.66%	-5.05%	-16.91%	-17.88%	-22.33%	-15.46%	-32.46%	-27.99%	-30.39%	-39.53%	-34.61%	-33.97%	-36.11%	43.75%	-38.56%	44.04%	41.84%	-40.47%	-29.08%	-28.79%	-26.13%	-23.35%	-26.39%	-29.41%	-36.65%	34.42%	-18.97%	-22 49%	-19.17%	-23 29%	-20.03%	-14.38%	% Loss of 60 gloss	QUV-500-HOUR
			1.64	4.37	0.82	1.71	0.00	0.89	2.24		0.0	0.63	0.82	0.77	1.13	0.70	0.67	0.62	0.92	1.02	0.92	0.96	0.45	0.12	0.07	0.42	0.35	0.15	0.78	0.40	2.52	1.40	2.03	2.43	2.23	1.48	1.18	<u>2</u>	Change in delta E	
			-2.13	-3.94	2.54	-2.98	-0.50	2 5	2.00	0.00	0.07	0.85	70.1	1.5	1.32	0.93	0.96	0.85	1.09	1.13	1.24	1.03	0.83	1.02	0.88	0.82	1.02	0.93	1.01	0.94	1.38	1.12	1.12	1.35	1.29	1.26	<u>ب</u>	1.51	Change In Y.B.	
			12.5	75.5	25.0	60.6	23.0	3 0	2 2	30.	50.7	00.0	20.0	38.2	41.5	34.6	3/.9	33.8	35.2	36.3	43.1	32.8	32.3	38.9	50.1	36.8	39.8	48.2	38.6	40.1	26.1	32.8	52.3	55.4	54.8	33.9	54.0	55.9	60° Gloss	
			0.57	3.40	11.07	9.8	4.0	3 8	A	1 45	2 6	1 2 2	2.5	3 -0-	1.02	3 .3	2.52	2.14	2.19	30.02	3 3	1.00		1.13	1.37	1.75	1.33	1.76	1.98	1.63	2.24	2.00	2.35	2.54	2.14	1.99	1.43	1.97	Delta E	
		1	-0.17	2.53	3.84	2 2	2 2 3		191	0.71	200	0.32	2 2	0.00	2 5	9 6	200	1.12	3 8	100	2 6	2.20	0.00	0.20	0.51	0.78	0.53	0.80	0.97	0.83	0.90	0.48	1.00	1.07	0.86	0.65	0.16	0.67	100	QUV-10
		†	43.18%	-5.53%	-50.05%	/003 C3	34350	1321%	-16.29%	-13 60%	_11 77%	-18 50%	19 260	43.05%	14 99%	34 069/ 70	40.070/	10.00%	18.00%	47 70%	45 000/	20.00%	7002 F3	40.90%	7020.CV	44.83%	41.8U%	-30.95%	43.40%	-37.93%	-25.85%	-29.00%	-10.60%	-11.64%	-15.30%	-27.56%	-19.88%	-12.66%		QUV-1000-HOUR
			1.8.1	4.93	0.07	25.5	30.5	0.07	2.8	1.23	1 02	0.82		1 2 2	3	2 5	23 6	1 10	2 5	1 57	3 5	131	0.00	2 5	0.00	7.14	0./0	0.90	1.48	1.07	1.97	0.92	1.98	2.06	1.97	1.15	0.66	8	delta E YB	Change in
			7.00	300	3 87	3 5	331	0.23	2.15	0.82	0.64	0.71	0.70	1 20	15	38	121	138	1	144	100	1.36	103	0 97	1110	1.00	1 32	3 2	1.3/	1.38	0.92	0.69	0.93	1.10	1.02	0.98	0.73	Ē	B X	Thenge in

Table 9 (Cont.)
OVEN BAKE

₹a	n/a		줊	9.22		gelled	1.11		gelled	73	046
η√a	n/a	-	n/a	9.3		Selled	1.16	23.1	gelied	L	045
n/a	n/a		n/a	9.49	^	gelled	1,35	- X	gelled	85	044 4
√a	η		n/a	9.5		gelled	0.7	,	gelled	L	043
n/a	7∕2		20	9,44	:	Gelled	0.86	2	gelled		042
n/a	n/a		D/B	9.39		gelled	1.79	4	gelled	L	2
₹8	TV a		n/a	9.4		gelled	0.54		gelled	8	24 6
B/U	n/a		n/a	9.56		gelled	0.77	Nice deaths game of	gelled	L	039
n/a	n/a		13/8	9.55	المستعددات	gelled	1.38		gelled	L	038
e/u	n/a	A PLATFORM PL	n/a	9.23	, , , , , , , , , , , , , , , , , , ,	gelled	0.85	_	gelied	L	037
B/U	n/a	· ATTENDED	n⁄a :	9.33		gelled	1.17		gelled	88	036
e/u	n/a		n/a	9.44		gelied	1.95		gelled	L	035
в⁄п	n/a	, and the	· n/a	9.44		gelled	1.13		gelled	L	034
soft	ō	-8.88	8.21	9.01	55.11	1:40	0.9	-18,60	70	8	033
n/a	R/Ω		n⁄a	9.24		gelled	1.5		gelled	72	032
7∕8	n/a		₹.	9,57		gelled	1.37		gelied	93	031
n⁄a	n/a		z⁄α	9.48		gelled	0.88		gelled	70	023
Z⁄a	n/a	-	3	9.05		gelled	0.78		gelled	80	022
잝	n/a		7/0	9.53		Golled	1.19	36	gelled	69	021
₹a	n/a		200	200	The West of S	gelled (a)	2.34		gelled	78	020
n/a	. n/a	i i	n/a	9.47		Sollog	1.28	are the first own with "	gelled	63	019
n/a	B/U	,	670	1.69?	200	gelled	0:68	- Huddhim	gelled	58	018
n√a	BAL	T-12	T.	9.52	The state of the s	golled	1.63	is in the same	gelled	61	017
. n∕a	ı√a		3	9.38		gelled	1.12	es d'amounts de	gelied	8	016
₩.	ηVa		n/a	9.52		gelled	1.17	TD axc.a.c.	gelled	61	015
∵ Va	n/a	Tarres de la companya	, a /r	9.56		gelled	0.56	, ,	gelled	88	014
√a	π/a		n/a	9.32		gelled	0.77	121.2	gelled	74	013
Z _a	π/a	× sur	Na	9.45		gelled	0.68		gelled	69	012
n√a	n/a	~	n/a	9.14		gelled	9,42	gh n m	gelled	83	011
ī√a.	n/a	***	πVa	9.09		gelled	0.492		geiled	85	010
₽¥a	π⁄a	J	D/a	9.42		gelled	1.11		gelled	68	900
롱	2	-	2	9.32		gelled	1.88		gelled	95	008
2	⊋(a		Zά	9.48		Çelled	1.88		gelled	91	007
衣	n/a		n/a	9,3		gelled	1.83		gelied	108	006
ı√a	n/a		νa	9.61	11.00	gelled	0.69	-	gelled	136	005
n/a	e/u	, E	n/a	9.65		gelled	1.88	1	gelled	79	Q4
n/a	e/u	, ,,	n/a	9.43	Acres 14	gelled	1.16	, .	gelled	22	003
n/a	n/a	-	, e/u	9:59	k Lampira (2. %)	gelled	1.18	7	gelled	140	002
		Physical Colombia (Co.)	n/a	9.58	ASSESSMENT OF	gelled	1.6	V (5.0.11.2	gelled	8	81
settling type	settling amount	<u>%</u> change	final pH	initial PH	%_ change	final ICI	initial. ICI	%_ change	final KU	initial KU	Formula
		_				-					

Table 9 (Cont.) OVEN BAKE

						1					
	ŗ										
				1,7		-					
			Č	4		1					
				,		,					
				- 1							
-			-	1 V			-				
		ARMB	lly falling	STE O/A S	tadheres	settling is the relative ht on stirring stick that achieres w/o easily failing away	on stirrin	dative ht c	is the re	% settling	
geiked	gelled		gelled	8.18	the state of the	gelled	0.95		gelled	8	088
gelled	gelled		gelled	9.35	1.5 1.776	gelled	0.78		gelled	83	087
gelled	gelled		gelled	9.33		gelled	1.05		gelled	72	086
gelled	gelled	1	gelled	9.01		gelled	0.84		gelled	87	085
medium	60		. n/a	9:78	31.76	0.98	0.74	13.25	92	8	084
gelled	gelled	15.	gelled	9.82	,	gelled	==		geiled	91	083
soft	20	-9.00	8.8	9,67	-59.44	0.29	0.71	3.61	88	83	082
soft	4	-6.53	9.16	9.8	45,00	0.58	1.06	23.40	116	\$	081
medium	ž.,	-8.28	8.97	9.78	-22.27	0.75	0.97	9.41	93	85	080
medium	20	-5.5 4	9.37	9,92	-28.36	0.79	1.1	1.30	78	77	079
soft	50	-7.68	9.14	9.9	40.16	0.88	0.63	15.96	109	£	078
soft	70	-7.98	9.11	9.9	59.42	1,10	0.69	15.63	111	86	077
soft	20	-7.65	8.93	9.67	-5.71	0.79	0.84	-16.67	70	%	076
medium	£,"		gelled	9.73		e/u	0.8		gelled	8	075
80R	8	-7.97	9.12	9.91	9.29	0.93	0.85	10.00	99	80	074
soft	50	-6,68	9,08	9.73	208.05	1.26	0.41	18.89	107	8	073
n/a		, 5	n/a	3,⊱9,8		. 8∕⊔	0.52		n/a	8	072
medlum		-7.38	9.04	9.76	-58.71	0.67	1,55	10.59	94	85	071
ed-hard	56	-	geiled	9.75	12.1.00	gelled	0.73		gelled	77	070
 ed-hard	8	h h	gelled	9.71	C +8939	gelled	0.51		geiled	98	069
ed-hard	2	-8.35	. 8.89	8.7	139.41	.1.22	0.51	, 07 8 0	1637	87	068
mėdium		-7.75	9.05	18.6	51.53	1.29	0.85	23.60	110	89	067
a/a	n/a		a∕n⁄a	9,32	7 's	gelled	1.74		gelled	87	055
B/U	n/a		D∕a	9,72	, was 2, 2 mm.	gelled	1.48		gelled	58	054
medium			n/a į	9,65		gelled	1.34		gelled	78	053
n/a	n/a	1 10 10 10	n/a	9,65	121	gelled	1.62		gelled	138	052
, n∕a	n/a	ore set it a	n/a	9.43		gelled	2.88		gelled	64	-051
n/a	n/a	, , ,	n/a	9.4		gelled	0.63		gelled	68	050
, n∕a	n/a	* ***	IJ.	9.07		geiled	1.66		-	86	049
			n/a	9,53		gelled	1.34		gelled		048
	amount Junean	Zh. Change	final pH	모	change	finalici		change	final KU	initial KU	Formula
Milma	- Millian			1	2	Control of the contro	1-111-1	2			
			aks at 14	17 6 W		Hing, and	08IV. 80	Visc		_	

Table 9 (Cont.)
OVEN BAKE
Viscosity, settling, and pH Stabilly (6 weeks at 140F)

```
(Key for Tables 7, 8 and 9)
         Resin 1 = Binder resin C2
         Resin 2 = Binder resin B28
         Resin 3 = Binder resin B27
  5
         Resin 4 = Binder resin B29
         Dispersant Amount:
                Dispersant used in pigment grind as in Example G.
         1 =
                Dispersant used in pigment grind and in final mix as in Example H.
         2 =
 10
         Pencil Hardness Ratings:
         0
                 <3B
         1
                 3B
         2
                 2B
 15
         3
                 В
         4
                 HB
         5
                 F
6
                 Η
         7
                 2H
         8
                 3H
         9
                 4H
         Blister Density:
                Dense
         1
[.a
<sub>=</sub>25
                Medium dense
         2
į..<u>i</u>.
         3
                 Medium
         4
                 Few
         5
                 No Blister
```

[::£

While this invention has been described by a specific number of embodiments, other variations and modifications may be made without departing from the spirit and scope of the invention as set forth in the appended claims.

The entire disclosure of all applications, patents and publications cited herein are hereby incorporated by reference.

5

The invention claimed is:

An aqueous coating composition comprising:

- (a) a binder polymer comprising one or more copolymerizable monoethylenically unsaturated monomers, wherein at least one of said monoethylenically unsaturated monomers contains latent crosslinking functionality; and
- (b) a second polymer comprising a monoethylenically unsaturated monomer containing latent crosslinking functionality.
- 2. The coating composition of claim 1 wherein said monoethylenically unsaturated monomer having latent crosslinking functionality comprises a carbonyl-containing monomer selected from the group consisting of acrolein, methacrolein, diacetone acrylamide, diacetone methacrylamide and vinylaceto acetate.
- 3. The coating composition of claim 1 wherein the binder polymer further comprises a macromonomer represented by the formula:

$$R^{1}$$
- $(OR^{2})_{z}$ - R^{3} - C = $CR^{5}R^{6}$

wherein:

 R^1 is a monovalent residue of a substituted or unsubstituted hydrophobe compound; each R^2 is the same or different and is a substituted or unsubstituted divalent hydrocarbon residue;

R³ is a substituted or unsubstituted divalent hydrocarbon residue;

 R^4 , R^5 , R^6 are the same or different and are hydrogen or a substituted or unsubstituted monovalent hydrocarbon residue; and z is a value of 0 to 150.

- 5 4. The coating composition of claim 1 wherein said second polymer is a dispersant polymer.
 - 5. The coating composition of claim 1 wherein said second polymer is a thickener polymer.
 - 6. The coating composition of claim 1 wherein the binder polymer comprises:
 - (a) 40-60% by weight of a fatty acid vinyl ester;
 - (b) 30-50% by weight of methylmethacrylate;
 - (c) 0.5-10% by weight of diacetone acrylamide; and
 - (d) 0.5%-5% by weight of methacrylic acid, based on the total weight of the binder polymer.
 - 7. The coating composition of claim 1 wherein the monomer having latent crosslinking functionality comprises diacetone acrylamide.



An aqueous coating composition comprising:

(a) a binder polymer comprising one or more copolymerizable monoethylenically unsaturated monomers, wherein at least one of said monoethylenically unsaturated monomers contains latent crosslinking functionality; and

- (b) at least one polymer comprising the reaction product of:
 - (i) an unsaturated carboxylic acid monomer,
 - (ii) a monoethylenically unsaturated monomer different from the carboxylic acid monomer,
 - (iii) a macromonomer comprising a hydrophobic portion and an alkoxylated portion, and
 - (iv) a monoethylenically unsaturated monomer containing latent crosslinking functionality.
- 9. The coating composition of claim 8 wherein said monoethylenically unsaturated monomer having latent crosslinking functionality comprises a carbonyl-containing monomer selected from the group consisting of acrolein, methacrolein, diacetone acrylamide, diacetone methacrylamide and vinylaceto acetate.
- 10. The coating composition of claim 8 wherein said macromonomer is represented by the formula:

$$R^{1}$$
- $(OR^{2})_{z}$ - R^{3} - C = $CR^{5}R^{6}$

wherein:

4 t 14

 R^1 is a monovalent residue of a substituted or unsubstituted hydrophobe compound; each R^2 is the same or different and is a substituted or unsubstituted divalent hydrocarbon residue;

R³ is a substituted or unsubstituted divalent hydrocarbon residue;

R⁴, R⁵, R⁶ are the same or different and are hydrogen or a substituted or unsubstituted monovalent hydrocarbon residue;

and z is a value of 0 to 150.

11. The coating composition of claim 8 wherein the binder polymer further comprises a macromonomer represented by the formula:

$$R^{1}$$
- $(OR^{2})_{z}$ - R^{3} - C = $CR^{5}R^{6}$

wherein:

 R^1 is a monovalent residue of a substituted or unsubstituted hydrophobe compound; each R^2 is the same or different and is a substituted or unsubstituted divalent hydrocarbon residue;

R³ is a substituted or unsubstituted divalent hydrocarbon residue;

R⁴, R⁵, R⁶ are the same or different and are hydrogen or a substituted or unsubstituted monovalent hydrocarbon residue;

and z is a value of 0 to 150.

- 20 12. The coating composition of claim 8 wherein the binder polymer comprises:
 - (a) 40-60% by weight of a fatty acid vinyl ester;
 - (b) 30-50% by weight of methylmethacrylate;
 - (c) 0.5-10% by weight of diacetone acrylamide; and

- (d) 0.5%-5% by weight of methacrylic acid, based on the total weight of the binder polymer.
- 13. The coating composition of claim 8 wherein the monomer having latent crosslinking functionality comprises diacetone acrylamide.
- 14. The coating composition of claim 8 further comprising a second polymer comprising the reaction product of:
 - (i) an unsaturated carboxylic acid monomer,
 - (ii) a monoethylenically unsaturated monomer different from the carboxylic acid monomer,
 - (iii) a macromonomer comprising a hydrophobic portion and an alkoxylated portion, and
 - (iv) a monoethylenically unsaturated monomer containing latent crosslinking functionality.

ABSTRACT

A waterborne coating having improved chemical resistance produced from a composition containing a binder resin having post crosslinking groups, an associative thickener having post crosslinking groups and an associative dispersant having post crosslinking groups.

the specification of which

-	
11 11	"" "" LH EN
	H. 11
1011111	ź
•	, š
111111	-£
1	4
	11.11
	H.T.H
	ETH E
	77

Docket No.	
 5661	

Declaration and Power of Attorney For Patent Application

English Language Declaration

As a below named inventor, I hereby declare that:

My residence, post office address and citizenship are as stated below next to my name,

I believe I am the original, first and sole inventor (if only one name is listed below) or an original, first and joint inventor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled

WATERBORNE COATING HAVING IMPROVED CHEMICAL RESISTANCE

(check one)	•		
is attached here	to.		
□ was filed on		as United States Application No.	or PCT International
Application Num	iber		
and was amend	ed on		
		(if applicable)	
-		derstand the contents of the above imendment referred to above.	identified specification,
		United States Patent and Trademar lity as defined in Title 37, Code of	
Section 365(b) of a any PCT Internation listed below and ha	iny foreign application(nal application which de ve also identified below or PCT International a	nder Title 35, United States Code, s) for patent or inventor's certificate signated at least one country other to, by checking the box, any foreign application having a filing date before	e, or Section 365(a) of han the United States, pplication for patent or
Prior Foreign Applic	ation(s)		Priority Not Claimed
	_		
(Number)	(Country)	(Day/Month/Year Filed)	_
(Number)	(Country)	(Day (Marsh) (Vary Filed)	
(Number)	(Country)	(Day/Month/Year Filed)	
(Number)	(Country)	(Day/Month/Year Filed)	_
PTO-SB-01 (9-95) (Modified)		P02/REV02 Patent and Trademark (Office-U.S. DEPARTMENT OF COMM

60/138,086	June 8, 1999	
(Application Serial No.)	(Filing Date)	
(Application Serial No.)	(Filing Date)	
(Application Serial No.)	(Filing Date)	
Section 365(c) of any PCT Internance Section 365(c) of any PCT International Jiscourse States or PCT International Jiscourse Jiscourse Jiscourse Section 112, I acknowledg	ational application designating each of the claims of this app all application in the manner p are the duty to disclose to the	the United States, listed below and olication is not disclosed in the prio provided by the first paragraph of 35 United States Patent and Trademark
Section 365(c) of any PCT Internance of the subject matter of elementary of the States or PCT International J.S.C. Section 112, I acknowledgo office all information known to metal section 112.	tional application designating each of the claims of this application in the manner part the duty to disclose to the tie to be material to patentable between the filing date of	any United States application(s), of the United States, listed below and olication is not disclosed in the prior provided by the first paragraph of 35 United States Patent and Trademark ility as defined in Title 37, C. F. R. the prior application and the national (Status) (patented, pending, abandoned)
Section 365(c) of any PCT Internations of a section 365(c) of any PCT International J.S.C. Section 112, I acknowledgo Dffice all information known to mesection 1.56 which became available PCT International filing date of the section 1.56 which became available of the PCT International filing date of the section 1.56 which became available of the PCT International filing date of the section 1.56 which became available of the PCT International filing date of the section 1.56 which became available of the PCT International filing date of the section 2.50 which became available of the PCT International filing date of the section 2.50 which became available of the PCT International filing date of the section 2.50 which is a section 2.50 which is	ational application designating teach of the claims of this application in the manner plus the duty to disclose to the lite to be material to patentability between the filing date of his application:	the United States, listed below an olication is not disclosed in the priprovided by the first paragraph of 3 United States Patent and Tradema ility as defined in Title 37, C. F. F the prior application and the nation (Status)

I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

(patented, pending, abandoned)

POWER OF ATTORNEY: As a named inventor, I hereby appoint the following attorney(s) and/or agent(s) to prosecute this application and transact all business in the Patent and Trademark Office connected therewith. (list name and registration number)

Heidi A. Boehlefeld, Reg. No. 34, 296 Robert E. McDonald, Reg. No. 29,193 Vivien Y. Tsang, Reg. No. 40,209

Send Correspondence to: Heidi A. Boehlefeld, Esq.

The Sherwin-Williams Company - Legal Dept.

101 Prospect Avenue, N.W. Cleveland, Ohio 44115

Direct Telephone Calls to: (name and telephone number)

(216) 566-3650

Full name of sole or first inventor John M. Krajnik	
Sole or first inventor's signature	* October 27, 1999
Residence Shaker Heights, Ohio	J
Citizenship USA	
Post Office Address 3703 Normandy Road	
Shaker Heights, Ohio 44120	

Full name of second inventor, if any Keith R. Olesen	
Second inventor's signature	September 15, 1999
Residence Morrisville, North Carolina	
Citizenship -USA - Canadian	
Post Office Address 300 Carpenter Town Lane	
Morrisville, North Carolina 27560	

Full name of third inventor, if any Gerald A. Vandezande	
Third inventor's alguarture	9/15/1999
Residence Cary, North Carolina	
Citizenship USA Canadian	
Post Office Address 1221 Shincliffe Court	
Cary, North Carolina 27511	
Full name of fourth inventor, if any	
Fourth inventor's signature	Date
Residence	
Citizenship	
Post Office Address	
Full name of fifth inventor, if any	
Full name of fifth inventor, if any Fifth inventor's signature	Date
	Date
Fifth inventor's signature	Date
Fifth inventor's signature Residence	Date
Fifth inventor's signature Residence Citizenship	Date
Fifth inventor's signature Residence Citizenship	Date
Fifth inventor's signature Residence Citizenship Post Office Address	Date
Fifth inventor's signature Residence Citizenship Post Office Address Full name of sixth inventor, if any	
Fifth inventor's signature Residence Citizenship Post Office Address Full name of sixth inventor, if any Sixth inventor's signature	